

NISTIR 7052

**The NIST 3 Megawatt Quantitative
Heat Release Rate Facility –
Description and Procedures**

Rodney A. Bryant
Thomas J. Ohlemiller
Erik L. Johnsson
Anthony Hamins
Brian S. Grove
William F. Guthrie
Alexander Maranghides
George W. Mulholland

NIST

National Institute of Standards and Technology
Technology Administration, U.S. Department of Commerce

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Anthony Hamins

Alexander Maranghides

George W. Mulholland

Building and Fire Research Laboratory

William F. Guthrie

Information Technology Laboratory

Brian S. Grove

Department of Justice

Alcohol, Tobacco and Firearms Fire Research Laboratory

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Donald L. Evans, Secretary

TECHNOLOGY ADMINISTRATION

Phillip J. Bond, Under Secretary of Commerce for Technology

NATIONAL INSTITUTE OF STANDARDS AND TECHNOLOGY

Arden L. Bement, Jr., Director

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EXECUTIVE SUMMARY

The 3 Megawatt Heat Release Rate Facility (3MWHRRF) was developed at the National Institute of Standards and Technology (NIST) as a first step toward having broad capabilities for making quantitative large scale fire measurements. Such capabilities will be used at NIST to validate fire models and to develop sub-grid models. It will also serve to provide a data base for studying a broader range of fire phenomena, and to address issues related to material acceptance and fire codes. An equally important objective is to provide templates for use by other laboratories including commercial testing facilities to improve the quality of their data.

Heat release is the result of the combustion of a fuel with the oxygen in air. The fuels of primary interest are those found in constructed facilities and include wood, plastics, foam materials used in furnishings (such as polyurethane), wire insulation (such as polyvinyl chloride), and carpet materials (such as nylon).

The rate at which heat is released is the single most important quantity in terms of fire safety. Thus it is important that this measurement be made in a quantitative manner. It is a key predictor of the hazard of a fire, directly related to the rate at which heat and toxic gases build up in a compartment or the rate at which they are driven into more remote spaces. Heat release rates on the order of 1 MW to 3 MW are typical in a room that is flashed over or from a single large object such as a bed or sofa.

It is important that heat release rate measurements be made accurately because fire regulations are frequently based on peak rates of heat release. Testing laboratories must be confident that the objects tested pass the required regulation and manufacturers need accurate information in defining the fire safety characteristics of their products. A second need for accurate heat release rate data is for the development of quantitative models for predicting heat release rate. In comparing a fire experiment and a model prediction, it is essential that the heat release rate measurement have an estimated uncertainty.

The 3MWHRRF developed at NIST meets the needs described above for objects that can be placed under the 6 m × 6 m hood, which is approximately 4 m above the floor, or for enclosures whose effluent can all be directed into the hood. It is capable of measuring heat release rates in the range of 0.10 MW to 3.0 MW including brief peaks as high as 5 MW. As documented in this publication, the expanded uncertainty (95 % confidence interval) is 11 % of the heat release rate for fire sizes larger than 400 kW. The response time of the system is such that it can accurately resolve dynamic heat release rate events of 15 seconds or more.

This document is intended to serve as a description of the NIST 3 Megawatt Heat Release Rate Facility and as an operations manual. It is also intended to serve as a general guide for implementing, operating and maintaining quality control of similar quantitative large scale heat release rate measurement facilities. The measurement system consists of a hood and duct system, a duct flow rate measurement, a gas flow sampling system, and a

gas analysis system. Key features of the design and fabrication of these systems are presented including detailed schematics and the rationale for the choices made. Transient response and gas dispersion in the sampling system, sampling from a non-uniform duct flow, and making accurate total flow measurements using bi-directional probes are dealt with in the design.

A calibration burner is essential for the operation of the 3MWHRRF and for characterizing its time response. The design of the natural gas burner including the special flow control and flow metering capabilities are presented.

The general design of the software allowing the display of nearly real-time heat release rates with corrections for sampling/instrumental delay and response times, is described. The uncertainty analysis described in the report includes the effect of the drift in the gas analyzer outputs, the correlation effects in computing the oxygen difference relative to the background value, and combining the uncertainties from over 50 variables in the heat release equation.

ACKNOWLEDGEMENTS

The success of any project of this scope and magnitude is due to more than just the work of the authors. Therefore the authors wish to thank the following NIST staff for their valuable contributions: Laurean A. DeLauter, David W. Stroup, Roy A. McLane and Gary Roadarmel for construction of the calorimeter, and William H. Twilley, Laurean A. DeLauter, and Jay A. McElroy for construction of the natural gas calibration burner.

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1 Background

Heat release rate is defined as the enthalpy change per unit time as a result of the conversion of the chemical energy of a fuel to heat in a combustion process. Most commonly the fuel is carbon-based and the combustion process is one of oxidation, usually by the oxygen in air. Heat release rate is typically reported in kilowatts (kW) or megawatts (MW). Its importance follows from the fact that it is a key predictor of the hazard of a fire, directly controlling the rate at which heat and toxic gases build up in a compartment or are buoyantly driven into more remote spaces [1]. It is, in effect, the most pertinent measure of the size of a fire [2].

Understanding the heat release rate potential of an object or an assembly of objects is essential to estimating the hazard such an object or arrangement could pose if ignited. Rational limitation and regulation of such a hazard is based on such understanding. Although substantial progress is being made, the present state of fire growth models is such that accurate prediction of heat release rate for common room contents such as chairs or beds cannot be made with full confidence. Thus measurements of heat release rate on real objects are currently essential. The measured results may be used as input for hazard calculation models such as CFAST (The Consolidated Model of Fire Growth and Smoke Transport) [3] or for product regulation. In either case, accurate heat release rate measurements are essential to meaningful results.

For a simple object made from a pure substance with a known constant heat of combustion the heat release rate measurement requires only a mass loss rate measurement on the object since the former is proportional to the latter, i.e.

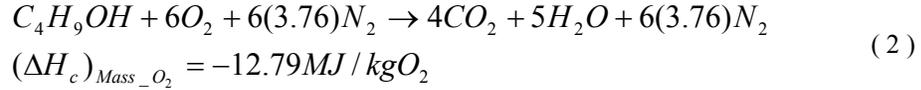
$$\dot{q} = \dot{m}\Delta H_c \quad (1)$$

where \dot{q} is the measured rate of heat release, \dot{m} is the mass loss rate (time derivative of decreasing object mass) and ΔH_c is the known heat of combustion (e.g., kJ/kg). In practice the heat of combustion of a complex object is rarely tabulated and in any case is variable for charring materials. Thus reliance on mass loss to quantify heat release is unreliable for real objects. On the other hand, mass loss is useful if the “object” is a well-defined gas or a liquid supplied at a known rate. This is, in fact, the basis for calibration of more general heat release rate calorimeters, where the calorimeter output can be compared with a precisely measured flow of a fuel whose heat of combustion is also accurately known.

Early measurements of heat release rate focused on the heat output as represented by the temperature of the product gases. Thus an array of thermocouples was positioned in a duct which captured all these gases to measure their average gas temperature [ASTM 1321 (LIFT test); ASTM 906 (OSU calorimeter)]. This approach assumes the flow is adiabatic, which is never a reality. The heat emitted from the fire as radiation, for example, can be 35 % or more of the total chemical heat release rate. More sophisticated

variants of this thermal approach, based on measuring the fuel gas flow rate required to maintain a constant product stream temperature, had the same limitation [4].

Huggett [5] first suggested a very different approach, now termed oxygen consumption calorimetry.¹ He followed up on the much earlier finding that the amount of heat evolved from most organic materials per unit mass of oxygen consumed in their complete combustion is nearly constant. For example, for butyl alcohol:



Huggett shows that for a wide variety of molecules from pure hydrocarbons, to partially oxygenated species, to partially halogenated species, and a wide variety of polymers and natural materials such as wood and coal, the heat release per unit mass of oxygen falls within a narrow range. He showed that, for most common materials containing C, H, O, and N, the average heat release per unit mass of oxygen is 13.1 MJ/kg O₂; the standard deviation of the heat release rate for materials examined by Huggett is 0.35 MJ/kg O₂. Thus the oxygen deficit in the duct flow (relative to ambient air) is a measure of the heat release rate in the flow which the duct captures.

Sensenig built the first working apparatus based on oxygen consumption calorimetry [7]. The heat release rate was inferred from the measured oxygen deficit in the flow of a hood that captured the fire plume as shown in the following equation:

$$\dot{q} = (\Delta H_c)_{Vol_{O_2}} \dot{V}_D X_{O_2}^o \theta \quad (3)$$

where

$$\theta = (X_{O_2}^o - X_{O_2}) / X_{O_2}^o \quad (4)$$

with $X_{O_2}^o$ being the oxygen volume fraction in the ambient air, X_{O_2} the oxygen volume fraction in the duct after the captured smoke plume (and any excess air) is well-mixed, \dot{V}_D is the measured volume flow rate in the hood duct, and $(\Delta H_c)_{Vol_{O_2}}$ is the heat of combustion per unit volume of oxygen consumed (e.g., MJ/m³ O₂). This simplified equation is approximate since it neglects other gases that are present such as water vapor and CO₂. The equation does convey, however, the role of the primary variables: duct flow rate and duct oxygen depletion.

Equation (3) may be rewritten on a mass basis as follows:

$$\dot{q} = (\Delta H_c)_{Mass_{O_2}} (\dot{m}_{O_2}^o - \dot{m}_{O_2}) \quad (5)$$

¹ Factory Mutual also uses a related approach in which the production of carbon dioxide and carbon monoxide, rather than the loss of oxygen, are taken as a measure of heat release [6]

where $(\Delta H_c)_{Mass_O_2}$ is the heat released per unit mass of oxygen, $\dot{m}_{O_2}^o$ is the mass flow rate of oxygen in the duct prior to the fire test, and \dot{m}_{O_2} is the mass flow rate of oxygen in the duct during the fire test.

For an open system only the exhaust flow rate, which includes the flow rate of incoming air and combustion products, is measured. It is necessary to relate the measured exhaust flow rate to the incoming air flow rate. Therefore it is useful to define the oxygen depletion factor, ϕ , as the fraction of incoming air that is depleted of its oxygen.

$$\phi = \frac{\dot{m}_{O_2}^o - \dot{m}_{O_2}}{\dot{m}_{O_2}^o} \quad (6)$$

In relating the mass flow of air into the system to the mass flow in the duct, the assumption is employed that nitrogen is not involved in the combustion process and therefore the nitrogen flow is constant. Nitrogen analysis is not performed so its volume fraction is replaced using the assumption that only N_2 , O_2 , CO_2 , CO and H_2O are present. This substitution is most accurate if all of the other gas species are measured. Accurate water analysis is difficult, so it is typically approximated on the basis of the humidity of the incoming air. Using the substitution for nitrogen, ϕ is expressed in terms of the measured volume fractions of the gas species.

$$\phi = \frac{X_{O_2}^o (1 - X_{CO_2} - X_{CO}) - X_{O_2} (1 - X_{CO_2}^o)}{(1 - X_{O_2} - X_{CO_2} - X_{CO}) X_{O_2}^o} \quad (7)$$

It is apparent in Eq. (2) that the combustion process of hydrocarbon fuels can result in a greater number of moles of products than reactants. Parker [8] defines a chemical expansion factor as follows:

$$\alpha = 1 + X_{O_2}^o (\beta - 1) \quad (8)$$

where β is the ratio of the moles of combustion products to the moles of oxygen consumed. In the case of hydrocarbon fuels the average value of α is 1.10.

The number of moles in the fraction of air depleted of its oxygen is replaced by an equal or greater number of moles of combustion products (second term of the equation below). Therefore, the mass flow rate of air into the system, \dot{m}_{air} , may be related to the measured mass flow rate in the exhaust, \dot{m}_e , by the following relation:

$$\frac{\dot{m}_e}{M_e} = \frac{\dot{m}_{air}}{M_{air}} (1 - \phi) + \frac{\dot{m}_{air}}{M_{air}} \phi \alpha \quad (9)$$

Assuming that the molecular weight of the exhaust duct gas is approximately equal to the molecular weight of the incoming air ($M_e \approx M_{air}$), the mass flow rate of the incoming oxygen is expressed as:

$$\dot{m}_{O_2}^o = \dot{m}_{air} X_{O_2,inc}^o \frac{M_{O_2}}{M_{air}} = \frac{\dot{m}_e}{1 + \phi(\alpha - 1)} X_{O_2,inc}^o \frac{M_{O_2}}{M_{air}} \quad (10)$$

Paramagnetic oxygen analyzers require the water to be removed from the sampled gas, therefore a correction must be made to the ambient oxygen volume fraction measurement.

$$X_{O_2,inc}^o = (1 - X_{H_2O}^o) X_{O_2}^o \quad (11)$$

Using Eq. (6), (10), and (11), Eq. (5) may be rewritten as follows with ϕ , as described in Eq. (7), representing the case where O_2 , CO_2 , and CO are measured while H_2O is removed from the sampled gas:

$$\dot{q} = (\Delta H_c)_{Mass_O_2} \phi \frac{\dot{m}_e}{1 + \phi(\alpha - 1)} (1 - X_{H_2O}^o) X_{O_2}^o \frac{M_{O_2}}{M_{air}} \quad (12)$$

Incomplete combustion, especially CO formation, often occurs in fires and CO formation yields only about half as much heat per unit mass of O_2 consumed as does CO_2 formation. Huggett points out that even if the CO concentration is 10 % of the CO_2 concentration, the effect on the net heat released per mass O_2 consumed is small. However, flame retardants frequently boost CO formation and oxygen-starved burning, as in flashover conditions, does so as well. Often CO formation may exceed 10 % of CO_2 formation. In general, it is recommended to measure CO and correct the heat release rate for its formation as shown in the following equation:

$$\dot{q} = [(\Delta H_c)_{Mass_O_2}^{HC} \phi - ((\Delta H_c)_{Mass_O_2}^{CO} - (\Delta H_c)_{Mass_O_2}^{HC}) \frac{1 - \phi}{2} \frac{X_{CO}}{X_{O_2}}] \frac{\dot{m}_e}{1 + \phi(\alpha - 1)} (1 - X_{H_2O}^o) X_{O_2}^o \frac{M_{O_2}}{M_{air}} \quad (13)$$

where

$(\Delta H_c)_{Mass_O_2}^{HC}$ = heat of combustion of hydrocarbon fuel, MJ/kg O_2

$(\Delta H_c)_{Mass_O_2}^{CO}$ = heat of combustion of carbon monoxide, MJ/kg O_2

ϕ = oxygen depletion factor

\dot{m}_e = mass flow rate in exhaust duct, kg/s

α = combustion products expansion factor

M_i = molecular weight of gas i , kg/kmole

X_i = volume fraction of exhaust gas i

X_i^o = volume fraction ambient gas i

The algebraic complexity of Eq. (13), compared to Eq. (3) or (5), arises essentially from a more thorough treatment of the mass balances (and atom balances) on the species between the fire, where they are generated, and the instruments, where they are measured. Parker [8] and Parker and Janssens [9] discuss the details of the heat release rate calculation based on the extent to which the duct gas flow is characterized, i.e., whether one measures only oxygen or also includes CO, CO₂ and water. The NIST calorimeter system measures oxygen, CO and CO₂; a correction is made for ambient humidity as an estimate of the water concentration in incoming air. The heat release rate is not corrected for the soot yield². Details concerning the input measurement quantities for Eq. (13) are discussed in Sec. 4, Assessment of Uncertainty.

It is important to realize that the oxygen deficit in the duct flow, even in large fires, is typically rather small. This is a consequence of the need to prevent overheating of the exhaust duct and to allow completion of the combustion reactions before the fire plume enters the duct. Thus the best one can do with regard to capturing the plume is draw it and no other diluting air into the duct inlet at the top of the hood [10]. However, fire plumes are typically already quite diluted at the flame tips [11] and, as a result, one can expect an oxygen reduction only from 21 % by volume to about 19 %. Rarely is it actually possible to capture the plume in this manner, so additional plume dilution is the norm. An implication of this is that the oxygen meter needs to have high resolution if the inferred heat release rate is to be precise. Suffice it to say that oxygen measurement and duct flow rate are the two measurements in need of greatest attention.

2 Description of System

The 3 MW Heat Release Rate Facility is located in the Large Fire Research Facility and became operational in August, 2001. It employs oxygen consumption calorimetry in the standard manner to measure the total heat output of a fire. The description of the facility may be segmented according to three major functions: calorimetry, data acquisition, and operational validation. Each of these functions is shown as boxes in Figure 1. Within each box are the subsystems that combine to complete the function. To summarize the functions, calorimetry consists of collecting all of the gases produced by the fire, measuring the rate of flow of the gases, sampling a small and well mixed portion of the gases, and measuring the volume fractions of specific gas species (especially oxygen volume fraction). Data acquisition consists of sampling the electrical output of each calorimetry instrument as it responds to the physical conditions that it monitors, converting the electrical output to a digital signal, recording a time history of the digital signal and converting the record to a value of scientific significance and displaying it in near real-time. The data acquisition system also provides a user interface to control the

² A first order thermodynamic analysis indicates that for highly sooting toluene flames the effect on the heat of combustion is less than the uncertainty in the heat of combustion per kg O₂ for an unknown fuel.

output of the calibration burner and record the subsequent response of its instruments. Operational validation consists of putting a controlled flow of chemically released heat into the system and measuring the heat flow independent of the calorimeter measurement. The calorimeter and data acquisition systems are essential for measuring the heat released from a burning item. The calibration burner is essential for confirming the measurement. Detailed descriptions of each system and selected subsystems are presented in the sections that follow.

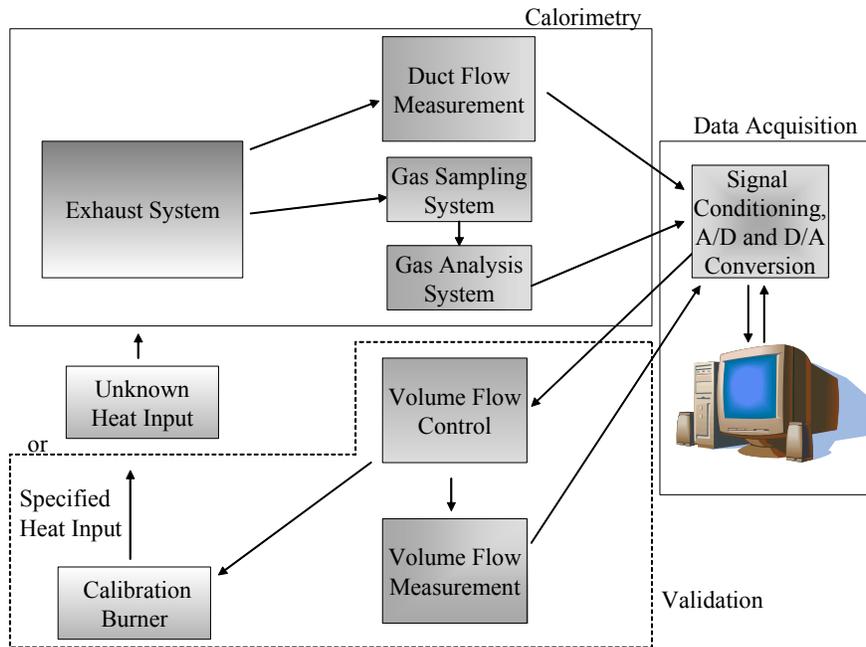


Figure 1 Schematic overview of the 3 MW Heat Release Rate Facility.

The system is nominally rated at 3 MW total heat release rate but fires with brief peaks as high as 5 MW have been successfully measured. (The hood skirt provides a temporary buffer capacity, as discussed below.) Calorimeter capacity may be limited either by the ability of the hood to capture fire plumes (i.e., by the total volumetric flow capacity of the hood) or by the height of the flame tips. The user must have a reasonable idea beforehand whether either of these factors will make this hood suitable for a specific fire situation. The literature and/or experience is the only guide as to probable maximum fire size. Flame tip height can be calculated from the available pool fire correlations [11] (and some results of this type are included below) but the user should be aware that not all fires behave like simple pool fires. The vertical extent of a burning object can affect flame tip height and plume entrainment, as can a tendency for wide objects to burn with more than one fire plume. (Multiple plumes may entrain more air than a single plume involving the same total heat release rate.) Reference [11] also includes formulas for the calculation of plume entrainment and thus the total volumetric or mass flow which a hood must swallow; again these are based on pool fires.

Fires as small as 50 kW can be measured in the 3 MW calorimeter, if a degraded signal to noise behavior is acceptable. Objects giving peak heat release rates this small are best measured in a smaller calorimeter hood.

2.1 Calorimeter

2.1.1 Hood and Duct System

Side and top view diagrams of the 9 m x 12 m and 6 m x 6 m hoods and duct systems are shown in Figure 2. The test area beneath the 6 m x 6 m hood is open on three sides. The fourth side is relatively close to one wall of the building; this could impact air inflow symmetry, especially for fires larger than 2 MW, though no problems have been noted to date. The base of the hood is located 4.57 m above the laboratory floor. The effective height of the hood inlet has been lowered to 3.0 m by the addition of a vermiculite glass fiber skirt (rated for a maximum temperature of 923 K)³. The skirt (in addition to the 1.80 m depth of the hood itself) offers a buffer volume for plume accumulation in the event of a transient peak in fire behavior that yields a plume flow too great for the hood to swallow. It can also serve to limit plume entrainment for fires that persist in exceeding the rated capacity of the hood. Both roles come at a price, as discussed below in the Design Considerations section.⁴ The effectively lowered hood inlet also helps assure that a weakly buoyant plume from a small fire is fully captured before it can drift out from under the hood.

The interior surface of the hood is coated with a fibrous cement mix to provide thermal insulation of the steel structure. This is an essential function, particularly to accommodate large fires that persist tens of minutes. However, for large and sustained fires, heating of the insulation material (and of the hood skirt) could cause it to become a source of re-radiation back to the burning object, accelerating the rate of burning.

A 1.52 m inside diameter steel duct emerges from the top of the hood and immediately turns to become horizontal, running under the high bay roof (Figure 2). Immediately downstream of this are inlets for ducts from smaller calorimeter hoods. These are normally sealed off to preclude dilution of the captured plume gases from the six-meter hood.⁵ The duct then makes a right angle turn upward, passes through the roof and makes a second right angle turn to run along the top of the roof. The entire length of the duct is thermally insulated to minimize condensation of plume moisture.

³ Above the fiber cloth is a lighter layer of fiberglass material used to seal the gap between the fiber cloth (hanging from a cable) and the interior surface of the hood. This seal is necessary to prevent significant escape of smoke in some circumstances.

⁴ In general it is much better to use a skirt than to risk losing part of the fire plume. When part of the plume is lost, the oxygen deficit generated by the fire is underestimated and thus so also is the heat release rate. Quantifying this is very difficult since one cannot judge the fraction of a plume that is being lost unless it is very obviously negligible.

⁵ Small inward leaks of air at this point in the duct system should not be problematical since they would have time to mix over the duct cross section before the gases are sampled for calorimetry. Such leaks are analogous to fire plume dilution, however, and the larger they are the more they lower the oxygen deficit in the duct and thus the system sensitivity to heat release rate.

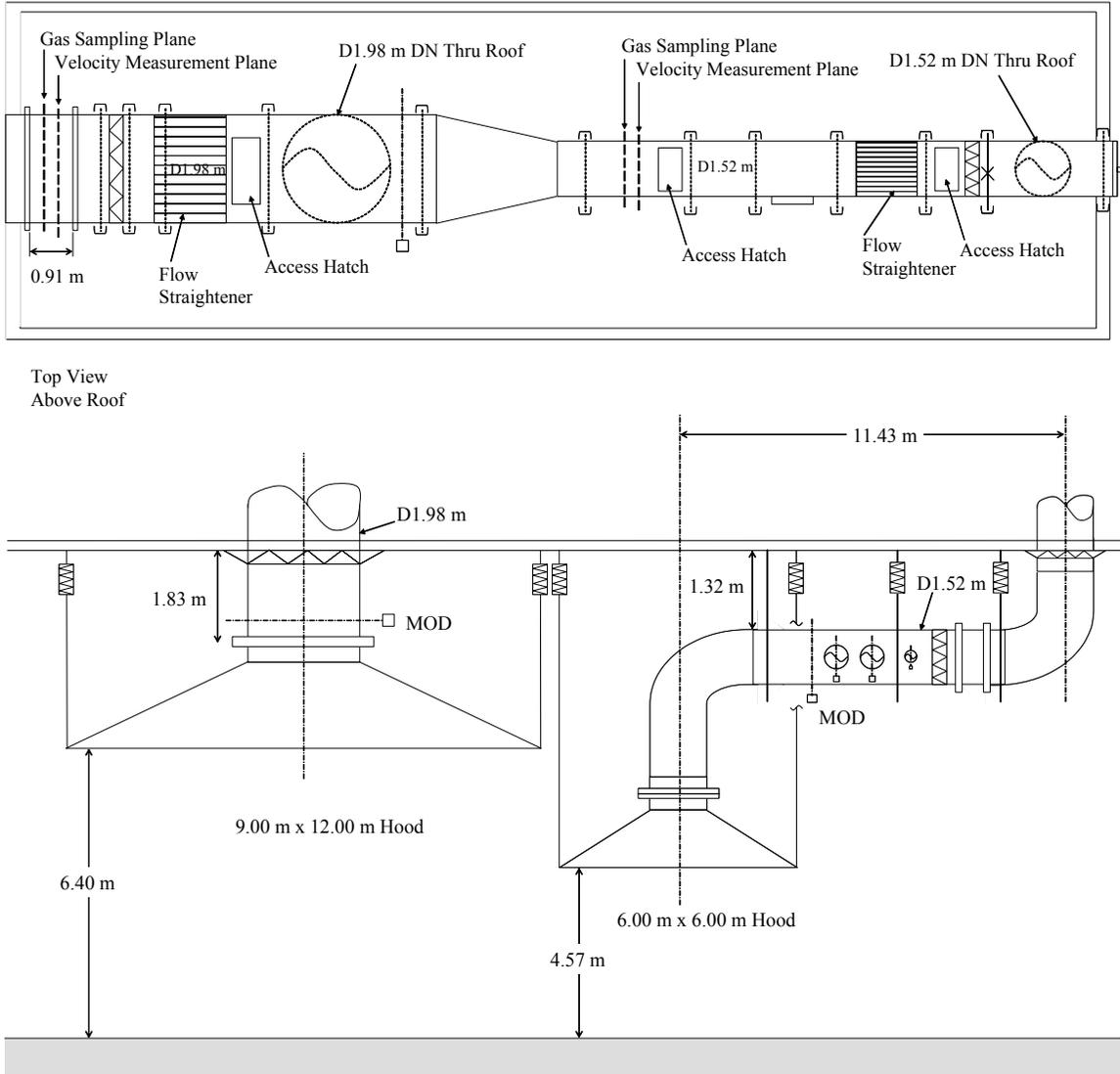


Figure 2 Large Fire Research Facility exhaust hoods and duct system.

The last turn includes a dead end duct section (with an access hatch) that has been sealed off with a flat bulkhead having small holes to assure pressure equilibration. Dead volumes in the flow system such as this, not cleanly swept by flow, are sources of dispersion or spread of the time history of the heat release rate information carried in the plume flow and should be avoided throughout the duct system and the entire gas sampling system. They provide pockets of gas that are re-distributed into the duct flow at times later than the time at which they originally reached the pocket location. This tends to smear out heat release rate peaks and slow the system response time. There are dispersive processes of this nature occurring at various locations in any real flow and gas analysis system and minimization of these must be factored in to the system design. A more extensive discussion of those pertinent to this system is given below in Sec. 2.4.3.

The three turns plus turbulence in the duct serve to mix the flow reasonably well. The mixedness of the flow was checked with helium injected at the hood duct inlet, sampled downstream and measured with a helium detector. These results indicated a uniform concentration over the sampled cross-section to within $\pm 5\%$. The sampled section of the duct was the same section as that used for normal heat release rate measurements.

The turns in the duct leave the time-averaged velocity profile skewed toward the top of the duct⁶. There is not sufficient duct length available on the roof to guarantee a fully-developed turbulent flow profile after the last turn in the duct. A flow straightening section was added between the last turn and the gas velocity measurement section to reduce the eddy size and remove any swirl. The flow straightener is of a simple tube bundle design [12]; it consists primarily of 10 cm diameter thin wall steel pipe sections, 1.5 m long. These are stacked in the section indicated in Figure 2 so as to fill the entire duct cross section. While the pressure head loss it induces is insufficient to fully flatten the velocity profile, measurements of the velocity at six locations across the duct cross section are sufficient to determine the total flow, as described in the next section.

Approximately 2.3 m downstream of the gas flow characterization section, the duct expands asymmetrically to an approximate 1.98 m inside diameter, just prior to joining with the duct from the 9 m by 12 m hood. To minimize any effect of this asymmetry, the gas velocity measurement plane in the 1.52 m diameter section was kept $1\frac{1}{2}$ diameters upstream of the duct expansion section.

Water condensation in the duct is a possibility in cold weather when humid lab air, or even more so, smoke, contacts the duct surfaces in the area atop the roof. If the duct walls are below freezing (there is no heating system in the duct), condensed water will freeze. Ice on the duct walls is probably of little concern. Ultimately the warm air will heat up the duct walls to the point that any ice melts and the water will then re-evaporate. Thermocouples on the duct wall allow monitoring of its temperature.

2.1.2 Duct Flow Rate Measurement

The velocity is measured approximately 4.2 duct diameters downstream of the outlet of the first flow straightener (located in the 1.52 m diameter section of the duct). Six bi-directional pressure probes of conventional design [13] are used. They are arrayed vertically on a duct diameter⁷ (in one plane) and placed at the Tchebyachev locations recommended in Ref. [14] (see Figure 3). The six velocity measurements are equally weighted in calculating the total flow rate in the duct. The temperature near each velocity probe location is measured with a 1.6 mm diameter sheathed chromel/alumel thermocouple (one thermocouple per velocity probe). The velocity probes are held in place by a rigid, 13 mm wide, vertical steel support spaced about 15 cm away from the

⁶This skewing was predicted by LES modeling of the flow and was confirmed by actual mapping with a probe inserted from the top of the duct at the normal velocity measurement cross section.

⁷The implicit assumption of bi-lateral flow symmetry appears justified by the lack of left/right asymmetry in the system before this plane and by the probing of the flow in this region.

probes to minimize any impact its cross section may have on the local velocity around the probes. The thermocouples are wound around the lead tubes of the bi-directional probes.

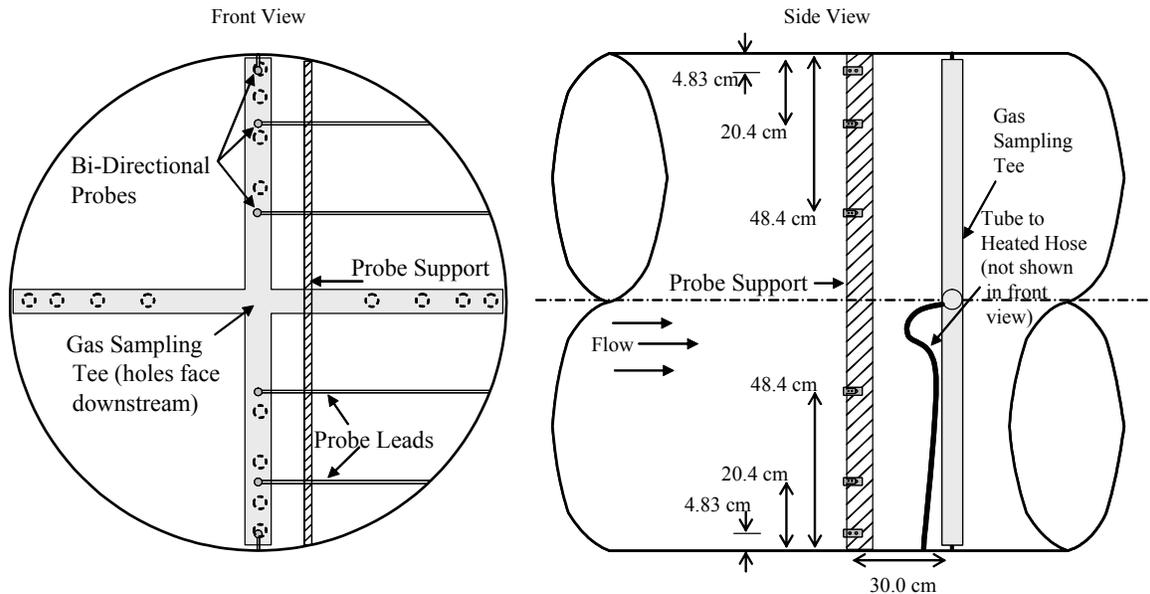


Figure 3 Schematic of velocity probes and gas sampling tee mounted in the exhaust duct. The size of the gas sampling tee is exaggerated in order to clarify the location of the sampling holes.

External to the duct and shown in Figure 4, the bi-directional probe lead tubes are bundled together and insulated with polyurethane foam pipe insulation (covered with aluminum tape for weathering) to minimize any temperature differential in the lead pairs from any given probe, since this can cause a zero offset and/or zero drift via differing gas column densities in the vertical portions of the probe leads⁸.

The bi-directional probe leads and their associated thermocouple leads go directly into an air-conditioned enclosure (see Figure 4) sitting on the building roof, next to the gas characterization section of the duct. Temperature control is necessary to minimize drift in the output of the six pressure transducers (MKS Baratron 220; range 0 to 133 Pa) that read the pressure differentials across the six bi-directional probes.

The six pressure transducers used here have all been calibrated using a Dwyer Model 1430 point gage manometer. This is a simple device that allows accurate imposition of the very low pressures seen in the duct flow velocity range that is pertinent here (less than 100 pascals). The calibration results confirmed the factory-supplied data.

⁸ This is potentially a significant source of zero drift in the pressure signal as the sun moves across the sky; thus the thermal shielding is necessary.

At a volumetric flow of $10.8 \text{ m}^3/\text{s}$, the velocities range from about 4 m/s to about 8 m/s. The local velocity values have fluctuations of roughly $\pm (2 \text{ to } 5) \%$ for this case, presumably due to turbulence in the duct.



Figure 4 Exhaust duct velocity measurement and gas sampling station.

2.1.3 Gas Flow Sampling System

The gas in the duct is sampled approximately 30 cm downstream of the plane of the bi-directional probes. The sampler is a four-armed cross that spans the duct diameter vertically and horizontally, as shown in Figure 3. The ends of the arms are anchored to the duct wall. The arms are 25.4 mm OD tubing, each having four 6 mm diameter holes spaced at equal duct area points along the arm span. The holes face downstream to lessen the chances of their being plugged by soot or ash drawn onto the hood, and they are located on equal annular area radii. The gas is pulled through the center of the cross and then goes into a lead tube that passes out the bottom of the duct. The line from the exit of the duct to the pump enclosure is a 12.7 mm ID Teflon-lined heated hose, typically operated at 363 K.

Suction is provided by an Air Dimensions Inc. Model 19320 TM heated double-head diaphragm pump that delivers 36 L/min at 35 kPa above atmospheric pressure when run at room temperature. When run at 373 K, it is expected to deliver about 20 % less volumetric flow (at NTP conditions), since it is a constant volume flow device. This

pump is mounted in a separate enclosure beneath the enclosure containing the pressure transducers. The pump is protected from soot deposition with a filter on the inlet side.

The flow rate of the gas sample is much more than is needed by the analytical instruments; together they require less than 5 L/min at one atmosphere. The reason for the excess gas flow is to shorten the time for getting the sample to the control room. The time to go from the gas sample tee to the control room is roughly 3 s.

Condensation of water (especially) and any other volatiles in the sampled gas is a concern, especially in cold weather. The heads on the gas sampling pump are heated to minimize condensation. The pump enclosure is also heated. The line leading from the pump enclosure to the control room is 9.5 mm ID by 19.5 m long, Teflon-lined, heated tube. The line is typically run at a set point temperature of 348 K.

Both the pump enclosure and the pressure transducer enclosure are mounted with wire rope vibration isolators (Enidine, Inc., Orchard Park, NY) between the enclosures and the adjacent supports. The principal reason for this is the sensitivity of the pressure transducers to any form of vibration. Both the gas sampling pump and the burners in the pollution control system can be significant sources of vibration of relatively low frequency (below about 30 hertz). The wire rope isolators offer better low frequency isolation than do rubber mounts.

2.1.4 Gas Analysis System

Figure 5 is a photograph of the flow control panel for the gas analysis system and Figure 6 shows a complete diagram of the gas analysis system located in the control room. As soon as the gas arrives at the analysis system, much of the excess flow is dumped to an exhaust line.⁹ The excess flow that is being dumped at the system inlet can be read with the large flowmeter. The flow normally bypasses this meter to minimize deposition of soot that may have passed through the pump filter. When the valves are switched so as to send the dump flow temporarily through the flowmeter one can check that the roof pump is behaving normally. The meter should read full scale (42.5 SLM) when the roof pump and the heated transfer lines are at their normal operating temperatures.

The pressure in the region where the flow from the roof enters the gas analysis system is normally kept at 500 Pa above atmospheric pressure to assure positive flow out through the exhaust line.

A pair of disposable flat disk filters is used to remove any particulates from the sample flow. The pressure drop across the filters is monitored by a Dwyer pressure gage attached to the flow line through 1.6 mm OD (1/16 in) stainless steel tubing. This small tubing minimizes any dead volume in these side lines.

⁹ The reason for dumping much of the flow before the instruments are reached is the need to dry and filter the instrument flows. The water traps or the filters would tend to clog rapidly if presented with the full flow.

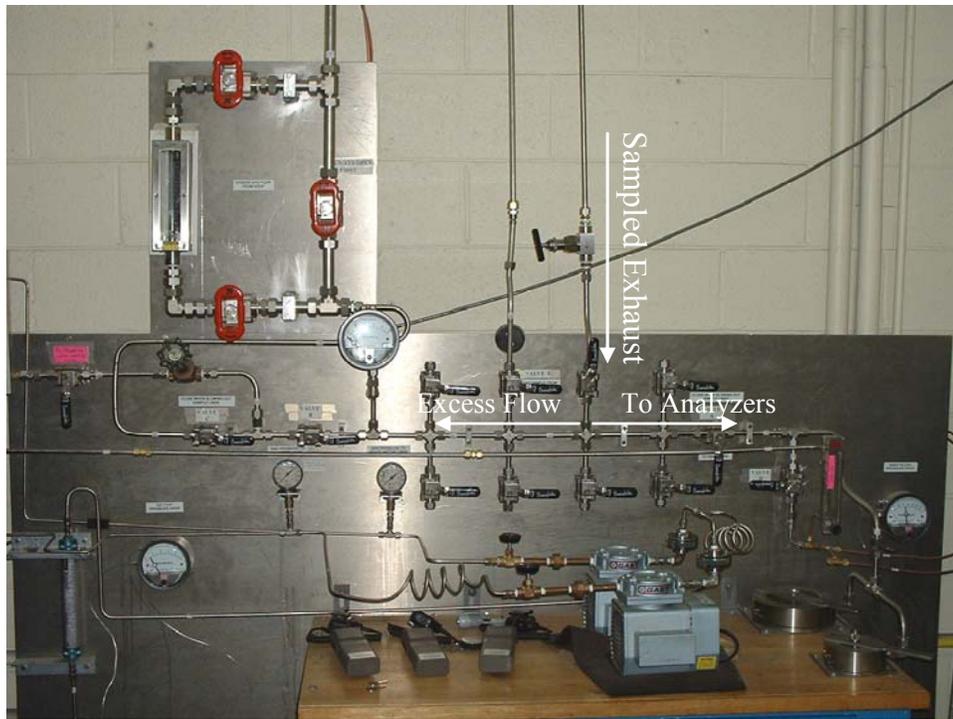


Figure 5 Gas sampling system flow control panel.

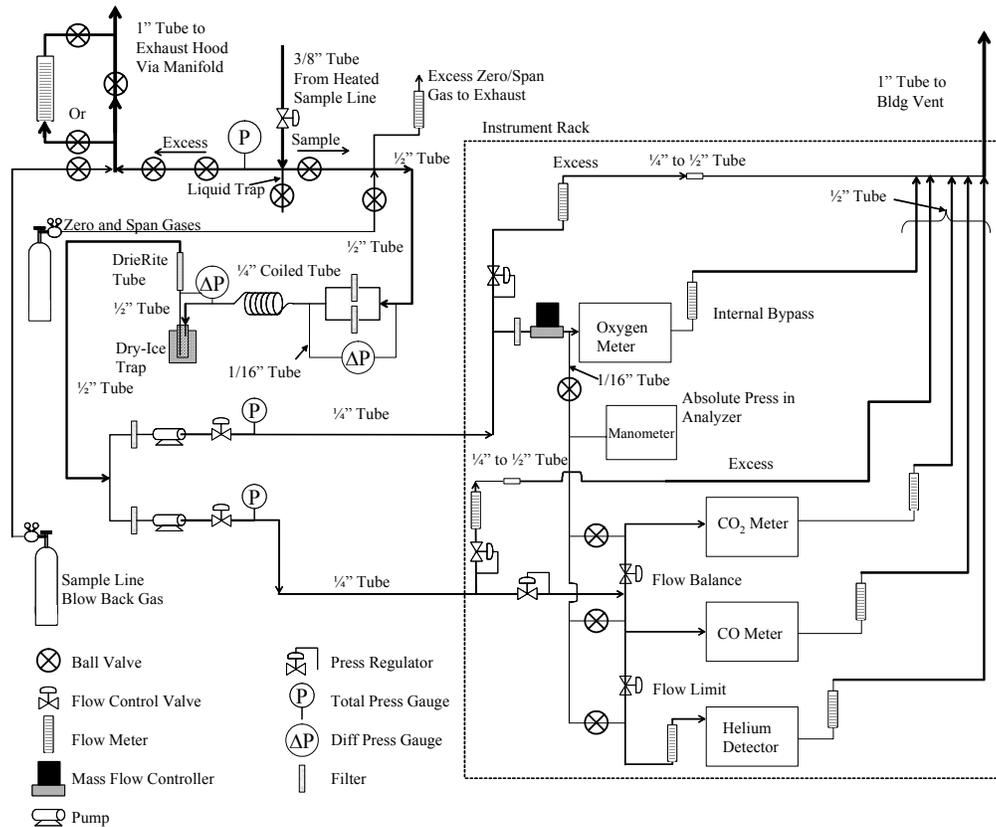


Figure 6 Diagram of the gas analysis system for the 3 MW HRR Facility.

The flow runs through a dry ice trap for moisture removal. The trap is filled with glass beads to improve heat and mass transfer, thus assuring that most of the water is removed. The trap is designed to easily handle a 30 min fire test without clogging. The pressure drop across the trap is monitored by a Dwyer pressure gage. The dry ice trap is backed up by a Drierite dessiccant trap since a water aerosol (that may form at the trap inlet) could pass through the ice trap¹⁰. The flow emerging from the Drierite tube is filtered once again before going into the control room diaphragm pumps (GAST Model DOA-P109-FB, rated at 54 L/min) to remove any Drierite dust.

Flow from one of the control room pumps goes to the Servomex 540a oxygen analyzer; the flow from the other pump goes to the Siemens Ultramat 5e CO and CO₂ analyzers. Each line has a manual valve, immediately downstream of the pump, to control the flow. The pressure gage in each outlet line helps monitor normal behavior; a faltering pump will be reflected in drift of its output pressure.

All of the gas analyzers measure the partial pressure of the gas being sensed; thus they are all sensitive to total pressure variations in the instruments. Of particular importance is the need to keep the pressure in the instrument the same during a test as it was during the instrument calibration preceding the test. Since the oxygen measurement is the most critical, it is given extra attention in this regard.

On the oxygen meter side of the pump, the flow is split just before a portion of it goes to the meter; the remaining flow is dumped to the exhaust line. The dumped flow passes through a pressure regulator (Porter Instrument Co., Model 8286) intended to help keep the flow in this path constant despite any upstream pressure variations. The flow rate is indicated by a Dwyer flowmeter downstream of the regulator. The flow to the oxygen meter is set by the controls on the oxygen meter itself.

The Servomex 540a oxygen analyzer is a paramagnetic device that takes advantage of the strong magnetic susceptibility of oxygen molecules. The current output of the device is a direct measure of the oxygen partial pressure. Since the device measures partial pressure, it is sensitive to temperature as well as pressure. The sample cell is in a specially thermostatted enclosure to keep its temperature constant. The pressure in the sample cell depends on total ambient pressure and on the flow rate to the cell. As indicated above, special efforts are taken to hold the flow constant. The total cell pressure is actively measured (see below), and any change (from the level during the span gas measurement) is compensated in the data acquisition program.

To assure further stability in the oxygen signal, an absolute pressure transducer (MKS Baratron Model 628, 0 to 133 kPa) is used to monitor the measurement cell pressure and to actively correct (in the data acquisition system) for any variations (with the value during calibration as the reference). A fitting internal to the oxygen meter, just upstream of the measurement cell, was modified to include a small diameter tube leading to this pressure transducer.

¹⁰ The oxygen meter is sensitive to moisture in the gas sample. Past experience has shown that if about half of the Drierite tube length is showing a color change from blue to pink, the oxygen signal can begin to drift.

The Siemens Ultramat 5e CO and CO₂ analyzers both utilize a non-dispersive infrared absorption principle. Light from a broadband infrared source is split into two beams, one going through the sample cell and the other through a nitrogen-filled reference cell. A pair of double-layer detector cells is placed at the ends of both sample and reference cells. The four detector cells all contain a fixed percentage of the gas to be analyzed (CO or CO₂). A chopper wheel causes a pulsating signal whose amplitude is proportional to the amount of CO or CO₂ in the sample cell.

The pump flow going to the CO and CO₂ meters is in excess of instrument requirements so as to decrease the transit time and the excess is dumped as it enters the instrument rack area. The dump flow and the combined instrument flows are each controlled by a pressure regulator (Porter Instruments Model 8286). The flow to the two instruments is set using their built-in controls and flowmeters.

2.2 Data Acquisition System

2.2.1 Signal Input and Output

The signals from the various measurement devices used for oxygen-depletion calorimetry determination of heat release rate are collected using the NIST Large Fire Research Facility data acquisition system (DAQ). The DAQ is currently configured to collect data both from instruments for calorimetry calculations and from other instruments or sensors being utilized for the experiment.

The DAQ hardware components (manufactured by National Instruments) are stored in an instrument rack in the instrument control room of the Large Fire Research Facility. The DAQ components are separate from the computer and transfer of data between the DAQ and computer is via a PCI (Peripheral Component Interconnect) bus computer interface. The primary DAQ board has 16 analog input channels at 16 bit digital resolution and is capable of a sampling rate of 333 kHz. A total of 40 analog input signals are required for the calorimetry computation. Seven signal conditioning and multiplexing modules are employed and each module has a capacity for 32 input channels. The channels are scanned at a rate of 200 Hz and the signals are dumped to a single channel on the primary DAQ board. Each multiplexed channel is electronically averaged for 1 s and the digital value is stored to the computer. The signal conditioning features of the modules include an electronic filter (200 Hz low pass) and gains (up to 100 times). The gains are typically applied to low voltage signals such as those produced by thermocouples. Each module is connected to a shielded terminal block which collects signals up to 10 V amplitude and provides cold junction compensation for thermocouples voltages.

2.2.2 Real Time Display

The user interface for the DAQ is written in a LabView program to compute the heat release rate and display user-specified data and computations. The program is run on a Windows workstation with dual 733 MHz processors and is located in the instrument

control room of the Large Fire Research Laboratory. The output is displayed on the workstation monitor and updated as the fire test occurs.

During a fire test, all measurement channels are available for display. Calorimetry instrument readings, velocities, and heat release rate (both from the oxygen calorimetry calculations and the calibration burner) are displayed graphically with up to 6 min of history (see Figure 7). Additional plots of instrument raw voltages are available to assist with the zeroing and spanning processes. In addition, plots of other important, but non-calorimetry-related measurements are displayed when specified.

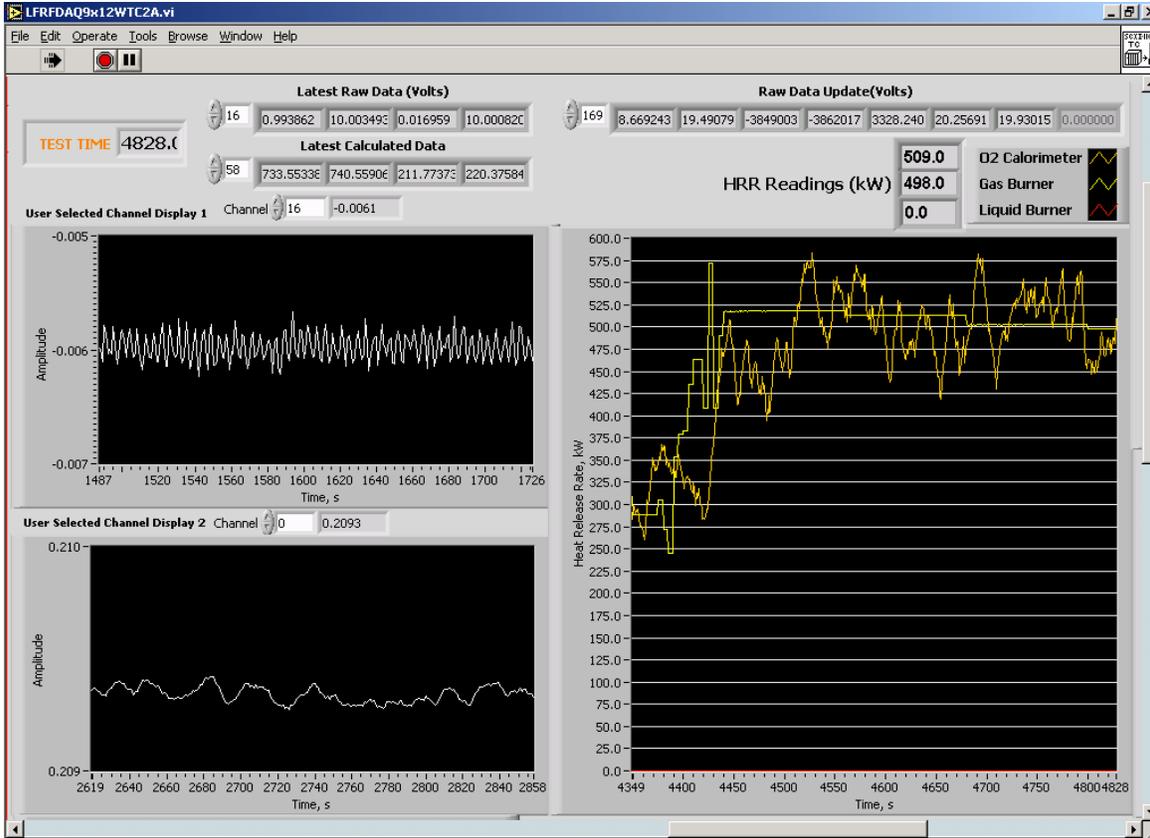


Figure 7 Real time display of oxygen sensor cell pressure ratio (upper left), oxygen volume fraction (lower left) and heat release rate (right).

Two marker channels are available and are used to keep track of specific events during a fire test. These markers are initiated with pushbuttons which are prominent on the display screen. Event marking puts simulated voltage spikes from 0 to 5 V and 10 to 15 V for one second in the channels set up for the markers. Plotting the data in these channels along with a basic measurement or calculated value enables relating the events to the response of the calorimetry system or a particular component of it. Such events include the beginning of zeroing, spanning, and background averaging periods, ignition and extinguishment of the fire, and step increases and decreases that are of importance for delay and system smoothing characterization.

2.2.3 Computation Algorithm

Most data are stored as voltages without modification. (The exception is the temperature measurements, which are converted in real time to degrees Celsius.) A second data file is created simultaneously in which the raw voltages are converted to CO, CO₂, and O₂ dry volume fractions, pressures, etc. These are in turn combined to generate flow velocities, duct volume flow, duct mass flow, and heat release rate. For heat release calorimetry testing, data are combined after estimating the relative delays for each instrument (described below) and synchronizing the data generated by a given moment of the fire.

Each channel of raw or computed data has an associated delay time. The delay time is the period between when a fire event occurs under the hood and when the particular sensor begins to respond to the change associated with the fire event. There are two main categories of delay. The first is for those sensors located at the sampling section of the duct which include pressure transducers and thermocouples. These sensors respond in less than a second to changes in their environment, but the input from an event under the hood is delayed in reaching the sensors by the flow time for the gas at the flame tip to enter the hood and progress through the duct to the sampling section. The second category of delay is for the gas analyzers located in the experiment control room. These instruments experience the duct flow delay as well as a sampling line flow delay and their own inherent sample processing delays (response times). These delays, which vary with the exhaust flow, are determined from specific tests that investigate instrument response to step changes under the hood.

The data acquisition and analysis program uses the delays to combine the outputs of sensors and instruments in such a way that the responses to particular phenomena under the hood are synchronized. In other words, output from fast responding sensors is stored in memory to be combined with output from the more slowly responding sensors at the appropriate time. Thus the faster sensor outputs are actually delayed in their combinations and calculations while the slowest outputs are utilized instantly.

The concept of storing varying histories of sensors with different response times is straightforward. The maximum delay time experienced by any sensor in the whole set of sensors defines how much history is stored for all sensors in the "history array". A delay time for each sensor is converted to an integer number of seconds. This also represents the position in the array that corresponds to the appropriate age of the data relative to that of the slowest sensor (the age and position correspond directly due to the 1 Hz sampling rate).

As the fire test proceeds, the calculations are grouped in several sets. Each set builds on variables calculated in the previous sets. The algorithm flowchart in Figure 8 displays these calculation steps. Additional detail of the algorithm is presented in Appendix D.3.

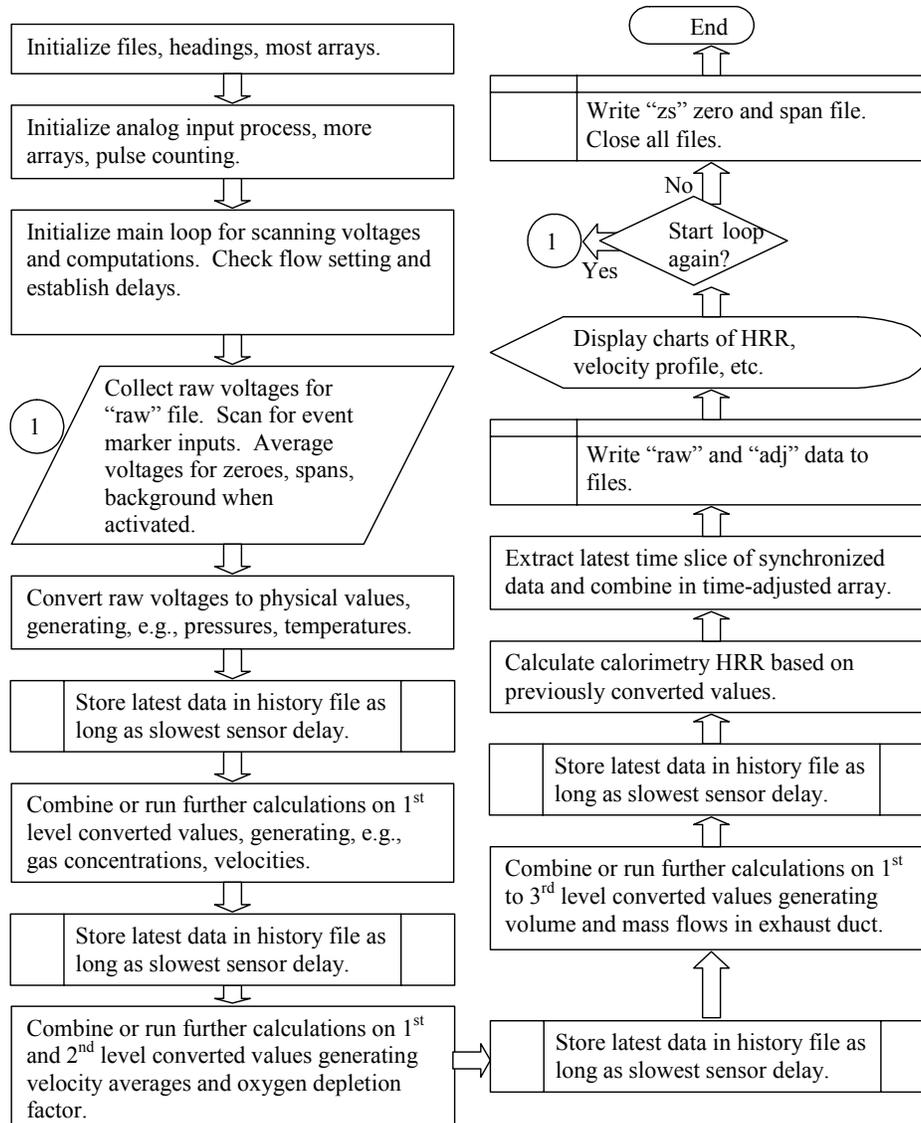


Figure 8 Heat release rate computation algorithm.

In the first set, the calculations include all temperatures, basic O₂ volume fraction, CO and CO₂ range factors, pressures, and mass losses. The second set of calculations includes those for oxygen volume fraction pressure correction, CO and CO₂ volume fractions, bi-directional probe velocities, water vapor volume fraction at ambient temperature, and average duct gas temperature near the sampling section (and the uncorrected natural gas flow and pressure for calibration burns). The third set of calculations includes the average duct velocity, and the oxygen depletion factor, ϕ (and the heat release rate of the natural gas for calibration burns). The fourth set consists of calculations of the volumetric duct flow and the mass flow in the duct. The last step calculates the heat release rate based on the duct mass flow, ϕ , and the O₂, CO, CO₂, and H₂O volume fractions.

2.2.4 Data Storage

Three files are generated during a fire test with suffixes “raw,” “adj,” and “ZS:” The “raw” file records the raw voltage values, thermocouple temperature values, and the two event marker channel values.

The “adj” file records the simple one-step conversions applied to the raw voltages to give values in terms of scientific significance such as species volume fraction and pressure. In addition the results of calculations for velocity, mass flow rate, and oxygen depletion factor are stored. Finally, the computation of the heat release rate is stored. The “raw” and “adj” files are updated each second with each sample of the data acquisition system and the associated time stamps are stored.

The “ZS” file lists the voltages generated by the zeroing and spanning processes for the gas analyzers as well as the calibration signals for the response of pressure transducers, load cells, etc. For some of the instruments, such as the gas analyzers, the calibration curve is linear and interpolation between two calibration points enables assignment of volume fractions to the recorded voltages. Other instruments, such as the pressure transducers and load cells, are generally non-linear or nearly linear and have been pre-calibrated over the necessary range. These calibration equations require a single point each to enable conversions from voltage to, e.g., Pa or kg.

2.3 Calibration Burner System

Because the calculation of heat release rate requires a large number of individual measurements, it is essential to have an independent confirmation of measurement accuracy. This is accomplished by burning an accurately measured flow of natural gas having a well-defined heat of combustion.



Figure 9 Photo of 3 MW fire from the natural gas burner.

The natural gas burner, shown in Figure 9, has been designed, fabricated and tested for this purpose. The burner can produce flows that correspond to a wide range of heat release rates, from 50 kW to over 6 MW in any increments specified by the user. The burner and flow system are configured to use natural gas as supplied by the local gas company. The energy content of the gas supply is measured by a natural gas calorimeter (COSA CW95) located in the instrument control room. Operation of the burner is automated with control and monitoring executed from the DAQ system. Details of the algorithm for the burner control and monitoring are presented in Appendix D.4.

2.3.1 Burner

The natural gas burner has a height of 96 cm (measured from floor to exit holes) and plan view dimensions of 112 cm x 150 cm (width x length). It is capable of producing controlled fires up to 6 MW using natural gas as fuel. The natural gas is delivered to the combustion zone above the burner through eleven primary rows of tubes. Two pilot tubes are located below and perpendicular to the primary tubes. The eleven primary tubes are grouped into four separate banks, which are independently opened and closed using solenoid valves. Operation of the four primary banks is dependent upon the amount of energy released in order to regulate flame-height, maximize efficiency and minimize the risk of flame blow-off. Each bank consists of three tubes except for Bank 1 which consists of two tubes. Each primary tube is split in half and capped at the end to allow for thermal expansion, thereby minimizing stress on the burner. Each tube has 56, 3 mm diameter holes drilled every 2.54 cm. Flow is initiated to the pilot tubes by a solenoid valve and the pilots are ignited using a 10,000 V spark igniter. Figure 10 is a photograph of the burner.

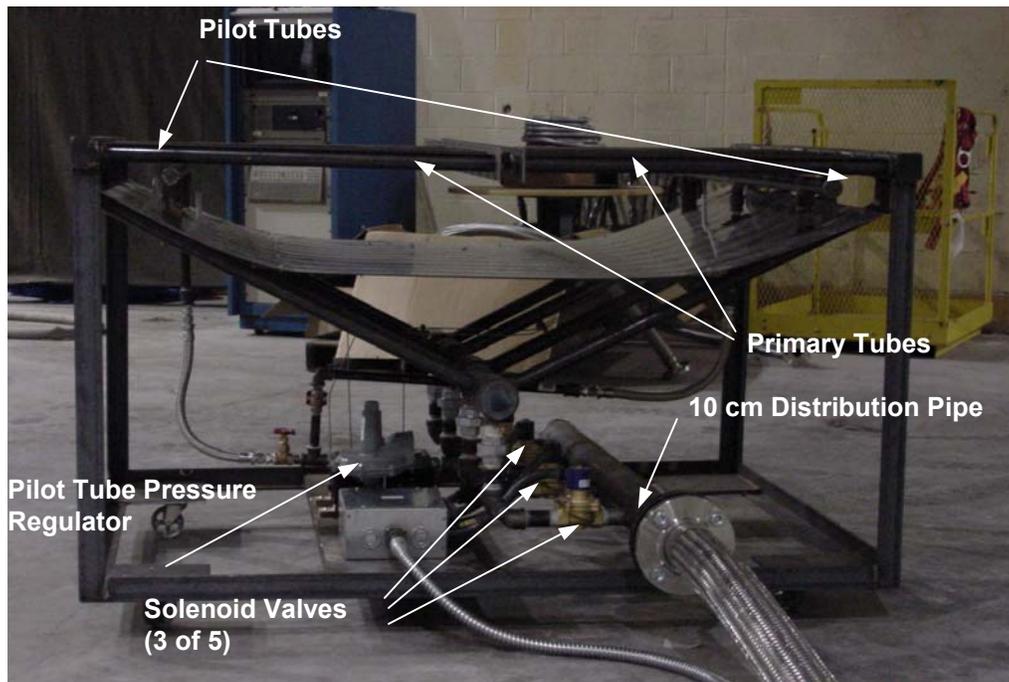


Figure 10 Calibration burner.

The burner is supplied with natural gas by a 7.5 cm diameter (i.d.) flexible stainless steel wound hose line, which feeds into the burner through a 10 cm diameter (i.d.) main distribution pipe. The main distribution pipe feeds both the two pilot lines and the 11 primary tubes. An electronic photoelectric sensor monitors the pilot flame and is linked to a shutoff valve to assure that a flame is burning when the gaseous fuel is flowing.

2.3.2 Flow Control and Flow Measurement

The burner is supplied with natural gas through an overhead gas train, which controls and measures the amount of gas supplied to the burner. Gas pressure is regulated to approximately 100 kPa above atmospheric pressure prior to reaching the overhead train. The gas train consists of a filter, a flow control valve, a volumetric gas flow meter, and a safety shut-off valve. The flow control valve is a pneumatically driven, programmable, high precision valve that is controlled by current provided by the data acquisition system. The volumetric flow meter is a rotary displacement meter that provides an amplified pulse output that is detected by the data acquisition system. A thermocouple and a pressure transducer are located in the volumetric flow meter so that mass flow may be deduced from the volumetric flow measurement. Figure 11 is a photograph of the gas train installed overhead in the Large Fire Research Laboratory.

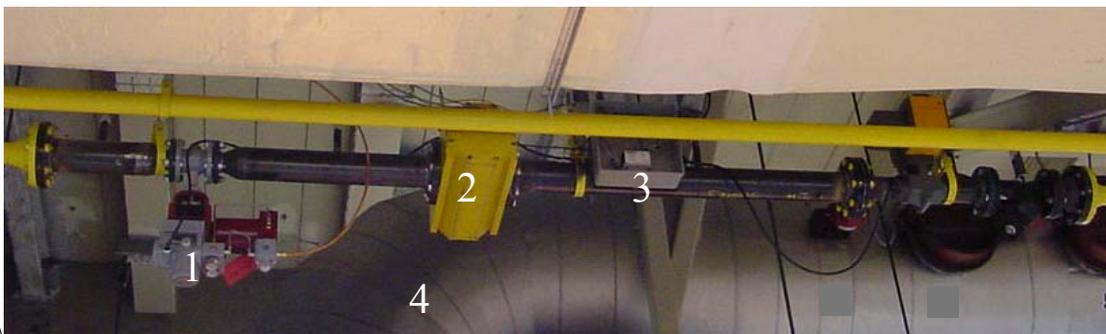


Figure 11 Overhead gas train including the (1) control valve, (2) rotary displacement meter, and (3) emergency shut-off valve. The exhaust duct (4) is also shown.

Figure 12 is a schematic diagram of the burner and the systems used to measure and control the flow of gas. The automated safety system is also shown on the diagram and includes a photoelectric sensor (FireEye), the Safety Panel, and Emergency Cut-Off switches. The input and outputs to the Safety Control panel are shown schematically in Figure 12. The panel is used to initiate the gas flow and to cut-off the gas flow in the event of an emergency. The manual cut-off closes the emergency shut-off valve labeled as item (3) in Figure 11. For emergencies, manual cut-offs are also positioned at doors on the east and west sides of the Large Fire Research Laboratory.

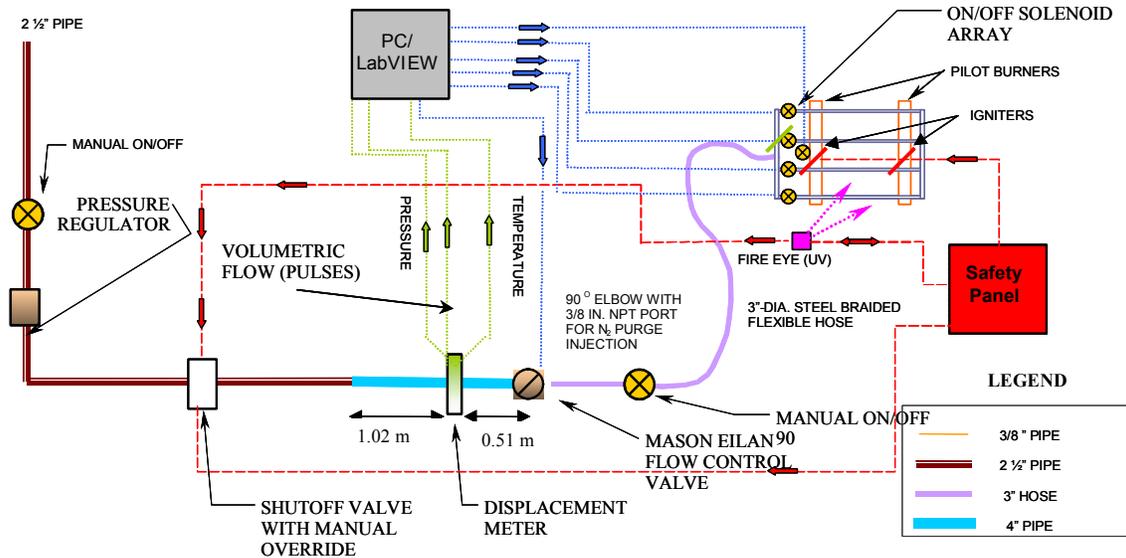


Figure 12 Schematic diagram of the natural gas burner system.

2.4 Design Considerations

2.4.1 System Time Delays and Time Response

The computed heat release rate is displayed on the computer monitor during a test; however, the numbers lag behind the actual fire output. There are several components to the overall transient response of the system to an instantaneous event in the fire being measured. Initially there will be no response since the information about a change has not reached the analyzers whose data go into the heat release rate calculation. So the first component of transient response is the gas travel time from the flame tips to the location in the duct where the gases are sampled; this varies with the hood flow rate. Next there is the gas travel time from the gas sampler on the roof to the inlet of the instruments in the control room (which includes the travel time through the plumbing in the control room). These are independent of hood flow rate but depend on the pumping speed of the system and the use of bypassed flows. Finally there is the response time of the instruments themselves. This is fixed when the flow rate to each instrument is set at its manufacturer-recommended value. Along the entire path, the gas does not travel as a rigid slug; rather it tends to undergo mixing with gases originating later as a result of various turbulent mixing processes. This process, called dispersion, also affects time response of the overall system to a change in the fire behavior. Careful design helps minimize this effect.

In general one needs to measure the lag time (total sample flow time) from the fire to the instrument inlet. This has a differing value for the oxygen meter and the CO/CO₂ meters since they involve differing flow paths (and flow rates) in the control room. Lag time is used to synchronize the measurements that go into the heat release rate calculation. One also needs to measure and take note of the system response times for the individual gases. These are to be kept within a certain range since they affect how closely the system will

follow a given time-varying heat release rate process from the fire being measured. In particular, system response times affect accurate measurement of brief heat release rate peaks (see section on transient effects below).

As a first approximation, a few of these times break out as follows:

- Duct flow time (fire to sampling point at $9.9 \text{ m}^3/\text{s}$) $\approx 7 \text{ s}$
- Gas sample flow time from roof to control room $\approx 2 \text{ s}$ to 3 s
- Instrument response times at nominal flow rates $\approx 5 \text{ s}$ to 10 s

The total system delays are somewhat longer than the sum of these numbers, however; for example, the total delay is 25 s for a particular experiment discussed below.

Precise values of the lag time for each instrument are needed since they must be incorporated into the data handling that results in a correct calculation of heat release rate. Measurement of these times is facilitated by a heat source that can be changed abruptly in magnitude (up and down). This capability is achieved via the data acquisition computer which commands the degree of opening of the gas flow control valve in the line to the multi-tube calibration burner; this system itself has an approximately one second lag time in response to computer commands.

The first time interval, the flow delay to reach the gas sampling plane in the duct on the roof, is measured by putting an event mark in the test file when the gas flow to the burner is turned on and then by finding the time at which any¹¹ of the thermocouples on the bi-directional probes begins to register a gas temperature increase. Reference [15] recommends a specific value of a temperature increase of 3 K ¹² and that is what is used for the NIST system. Again, this time interval varies with the hood flow rate.

The second component of the lag time for a given instrument, the time to go from the gas sampler on the roof to the inlet of the instrument, is a constant if the speeds of the roof and control room pumps are constant and the fraction of the excess sample flow dumped at the first flow split is unchanged. However, as noted, it can vary between the oxygen meter and the CO/CO_2 meters, because the flow paths differ from the laboratory pump(s) onward. This component of the lag time is found by noting the time between the above thermocouple response and the first instrument response to the fire-altered gases. Reference [15] recommends taking the time when the oxygen meter reading shows an increment of 0.05% and the CO_2 meter an increment of 0.02% ; these are also adopted for the NIST system. Note that the CO level from a gas burner can be difficult to read. One can safely assume that the lag time component for it is the same as for the CO_2 meter since they are effectively in the same flow system.

¹¹ The duct flow has been found to be well-mixed at flow rates of $9.4 \text{ m}^3/\text{s}$ and above. It is prudent to check more than one thermocouple at lower flow rates.

¹² To get a sharply readable increase of this size may require a fire of several hundred kW. Larger hood flows require a larger fire. Too small a fire will give erratic results.

The system response time is defined in Ref. [15] as the time for the oxygen meter¹³ to go from 10 % to 90 % of the change induced by a step change in fire size. Again, any and all dispersion in the system, from the fire plume tip all the way to the gas analysis instrument, contributes to the time it takes for this signal to change from 10 % to 90 %. This dispersion smears the original time sequence of events in the fire. In particular, it decreases the reading of any heat release rate peak that occurs on a time scale comparable to or shorter than this 10 % to 90 % response time of the system. This raises an issue that is discussed further in the next section.

2.4.2 Transient Effects on Peak Heat Release Rate

Fire regulations are frequently based on maximum allowed rates of heat release. Different calorimeter facilities have differing time responses and thus differing tendencies to smooth out a brief peak. Some facilities use an open hood while others use a compartment which allows smoke to build up prior to spilling into the hood, thus adding a delay in measurement of heat release rate.

Messerschmidt and Van Hees [15] discuss this transient response issue in the context of the European Community's Single Burning Item Test, which is based on heat release rate measurement. It is shown that different laboratories could end up rating a product differently in this test solely as a result of the differing transient behavior characteristics of their measurement systems. They recommend that the oxygen meter's apparent response time (defined as above) fall within a window of 9 s to 12 s, in order to minimize the tendency of differing labs to rate a product differently in the Single Burning Item test.

Another aspect of transient system response is related to noise in the calculated heat release rate. System noise (a result of the random variations in all of the variables entering into the heat release rate calculation) can affect the apparent magnitude of a heat release peak, and thus its uncertainty. The effect depends on the root mean square noise level and its frequency characteristics relative to the peak duration. An approach that is sometimes used is to judge a tested product's performance on the basis of a heat release rate curve subjected to a running time averaging process. The longer the time interval used for averaging, the more the noise is filtered out but also the more real, rapid heat release rate changes are damped. This raises the question as to how rapid a heat release rate fluctuation matters when an object is burning in some context such as a compartment fire. There may not be a unique answer to this and it is a subject of planned research at NIST. For now one can estimate that in a compartment fire context, upper layer gas temperature changes and second object ignition processes begin to respond significantly to heat release rate alterations in a time of the order of 5 s to 15 s, suggesting this range as the appropriate upper limit for time smoothing of the data. In practice, it is easy to use graphing software to examine the effect of varied time smoothing intervals on the heat release rate peak of a test object. For mattress fires it was found that 20 s smoothing reduced the apparent peak values by a couple of percent. In Ref. [15], a 30 s interval was

¹³ The CO and CO₂ meters' response times (inherent to the instruments, not the overall system) tend to be a little faster than the oxygen meter and thus do not limit the system response. In any event, they tend to be secondary in importance to HRR calculation.

used without any discussion. The smoothing interval, if any, should be reported along with the heat release rate data.

Determining the Role of Transient Effects on Measured Peak Heat Release Rate and Energy Conservation

As part of the present work, a series of experiments was performed to characterize the response of the 3 MW heat release rate calorimeter to square-wave pulses in terms of peak heat release rate, the width of the peak, and the conservation of energy. The results of these experiments were used to establish a criterion for assessing whether the peak heat release rate for an experiment is being underestimated because of the time response of the system.

In principle this is a problem which can be treated as a deconvolution of the actual heat release rate vs time from the measured heat release and the system response characteristics [16,17]. Thus one solves an integral equation relating observed heat release rate to the time integral of actual heat release rate modulated by the measurement system response. Differing mathematical techniques have been demonstrated in the noted references. The inferred correction to the apparent heat release rate history is sometimes large ($O(100\%)$), particularly for cases in which the heat release rate peak width is comparable to the time response of the measurement system. However, it is pointed out in Ref. [18] that the deconvolution process is quite sensitive to noise in the data and to the errors in the system response function. Thus it is of unclear value here where both of these issues are significant. Rather than proceed in this manner, we focus on characterizing the time response domain in which the 3 MW hood system gives accurate results. Deconvolution remains an area for further exploration.

The basic approach to assessing system time response was to produce a square-wave pulse heat release rate using the natural gas calibration burner described in Sec. 2.3. The peak heat release rate was set at nominal values of 0.5 MW, 1.0 MW, and 2.5 MW using a flow control valve. A signal was manually initiated from the computer control panel to open the flow control valve to a preset value and a second signal was sent to reset the flow to the pilot level. The loop time of the program for controlling/acquiring data is 1 s.

The heat release rate of the burner is computed from the heating value of the natural gas, its pressure, and the flow rate. As discussed in Sec. 2.3.2, the flow meter is a rotary device which displaces a fixed volume of gas four times per revolution. Digital pulses are produced at a rate of about 1 pulse per 2 L of gas. A heat release rate of 1.0 MW corresponds to about 7 pulses per second and 2.5 MW to about 18 pulses per second. The relatively low number of pulses per second limits the resolution for 1 Hz measurements such as needed in this study, but it does allow an accurate estimate of the average heat release rate.

A Schmidt-Boelter type radiometer with a time constant of 0.1 s to 0.2 s was used to provide a more rapid response to the actual peak heat release rate. The radiometer was set up a distance of 4 m from the burner with the view including the entire flame volume. The corrected burner peak heat release was obtained by multiplying the radiometer output

times a calibration factor determined for each of the three heat release rates. To determine this calibration factor, the heat release rate computed from the calibration burner volume flow measurement and radiometer output were averaged over a 20 s period during the steady burning for each of the three heat release rates. The calibration factor is computed as the ratio of the average heat release rate to the average radiometer voltage. The ratios have a dependence on fire size with values decreasing by 30 % for a five-fold increase in the heat release rate (2.62 GW/V at 0.5 MW, 2.20 GW/V at 1 MW, and 1.85 GW/V at 2.5 MW).

Figure 13 provides a detailed comparison for the burner heat release rate based on the flow meter and the output from the radiometer. Qualitatively the pulse shapes are similar as measured by both devices. The limited signal resolution of the flow meter is apparent from the discrete change in heat release rate around 4955 s and again around 4970 s. There appears to be a one to two second delay in the processing of the pulse counting relative to the radiometer measurement. This delay was observed in all the tests. The inflection point of the radiometer output near the end of the pulse is thought to result from continued flow through the burner after the valve for the flow controller has been reset to the baseline level. The gas continues to drain as pressure in the gas line to the burner equilibrates to the lower baseline level.

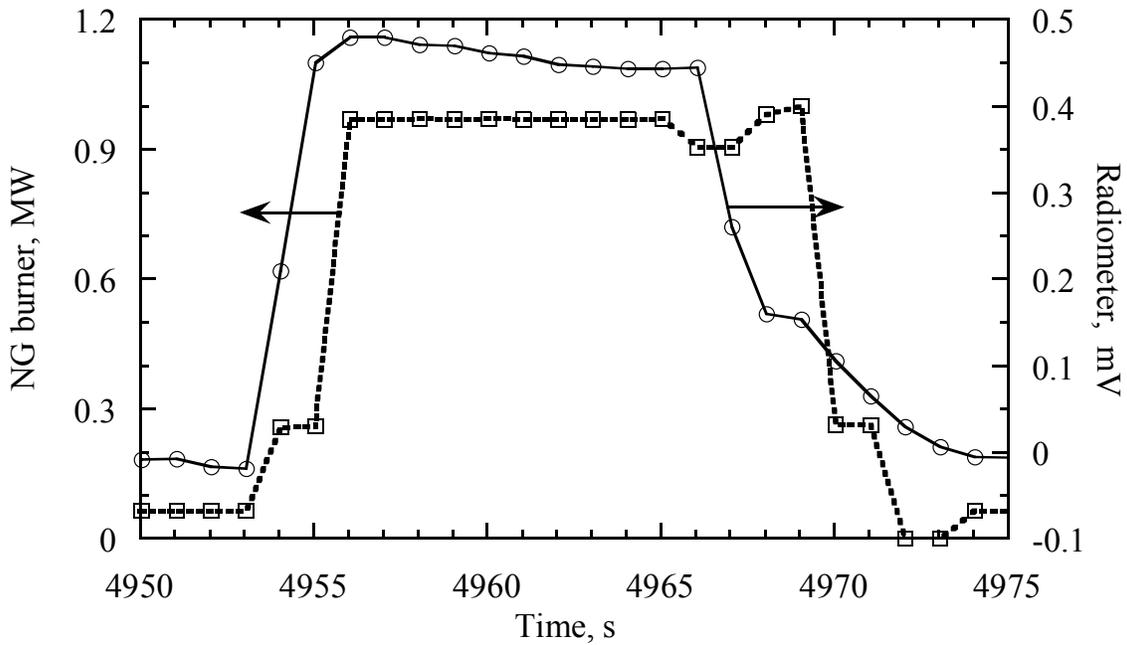


Figure 13 The square-wave pulse from a 15 s release of natural gas for a 1 MW heat release rate as measured by a radiometer and the burner flow meter.

The measurement sequence began by setting the calibration burner at a heat release rate of 0.10 MW. This pilot level of heating is needed to efficiently ignite the rapidly increasing gas flow. The mass flow controller was set for a flow corresponding to 1 MW heat release rate and then a switch was activated which in turn opened the mass flow

controller valve. After a fixed time, the sequence was reversed and the heat release set back at 0.1 MW. After the calorimeter reached a steady heat release at this low value, a repeat run would be made following the same procedure as above. Typically three runs were made for each of four pulse times: 30 s, 15 s, 10 s, and 5 s. At least one measurement was also made for a 60 s pulse. This sequence was then repeated for heat release rates of 0.5 MW and 2.5 MW.

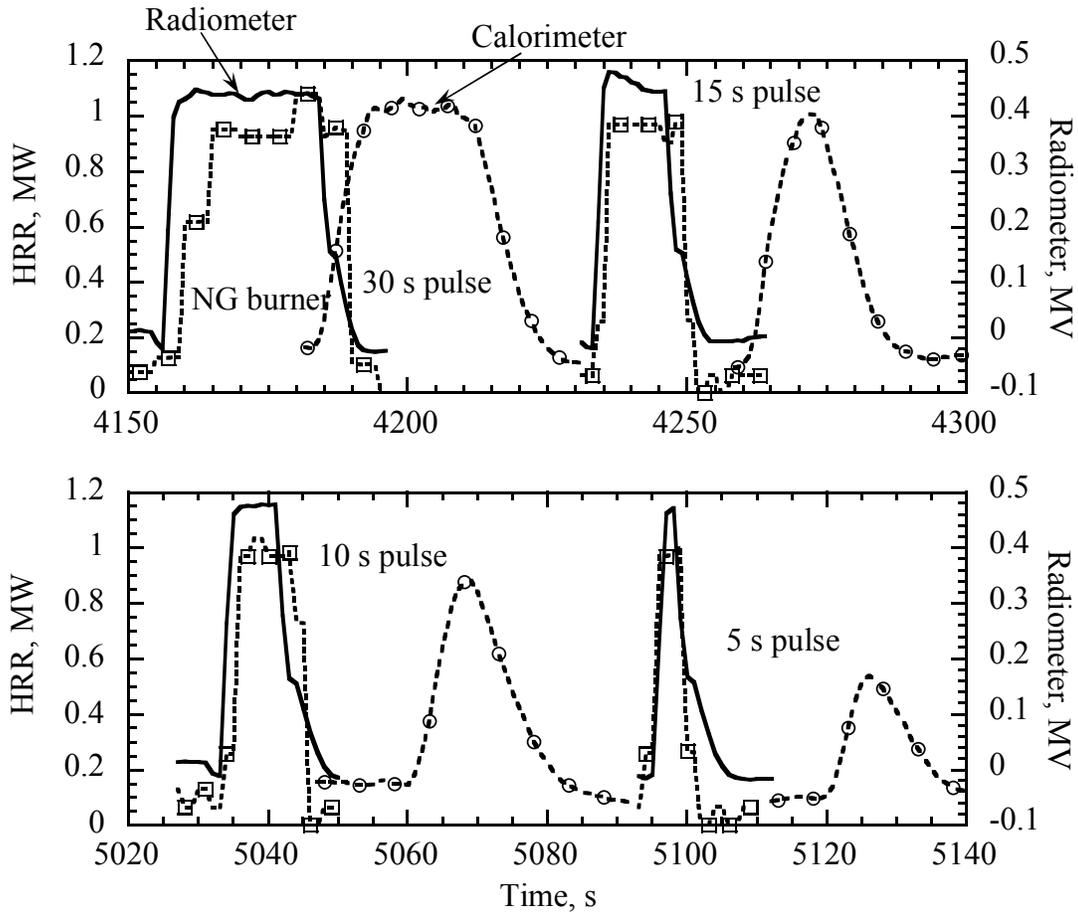


Figure 14 The measured output versus time for the NG burner (\square), calorimeter (\circ), and radiometer (solid line) resulting from 1 MW square-wave pulses of 30 s, 15 s, 10 s, and 5 s.

Figure 14 illustrates the characteristics of the square-wave pulse shapes for the 1 MW fire for the four different pulse widths. The 25 s time delay for the calorimeter is a result of the gas sampling time together with the nominal 9 s response time of the oxygen analyzer. The relatively low resolution of the natural gas flow measurement is apparent from the step changes in the heat release rate. The radiometer provides a better representation of the heat release pulse shape since it responds to the flame intensity, and it has a higher resolution (and faster response time) than the gas flow meter. For the 30 s and 15 s pulses, the peak in the calorimeter output is close to that of the burner and the

full time widths at the half peak height (FWHH) are similar though the curve shape produced by the calorimeter is rounded rather than square. The calorimeter peak is slightly reduced for the 10 s pulse and is reduced by about a factor of two for the 5 s pulse. In these two cases the FWHH values are also increased relative to the radiometer output.

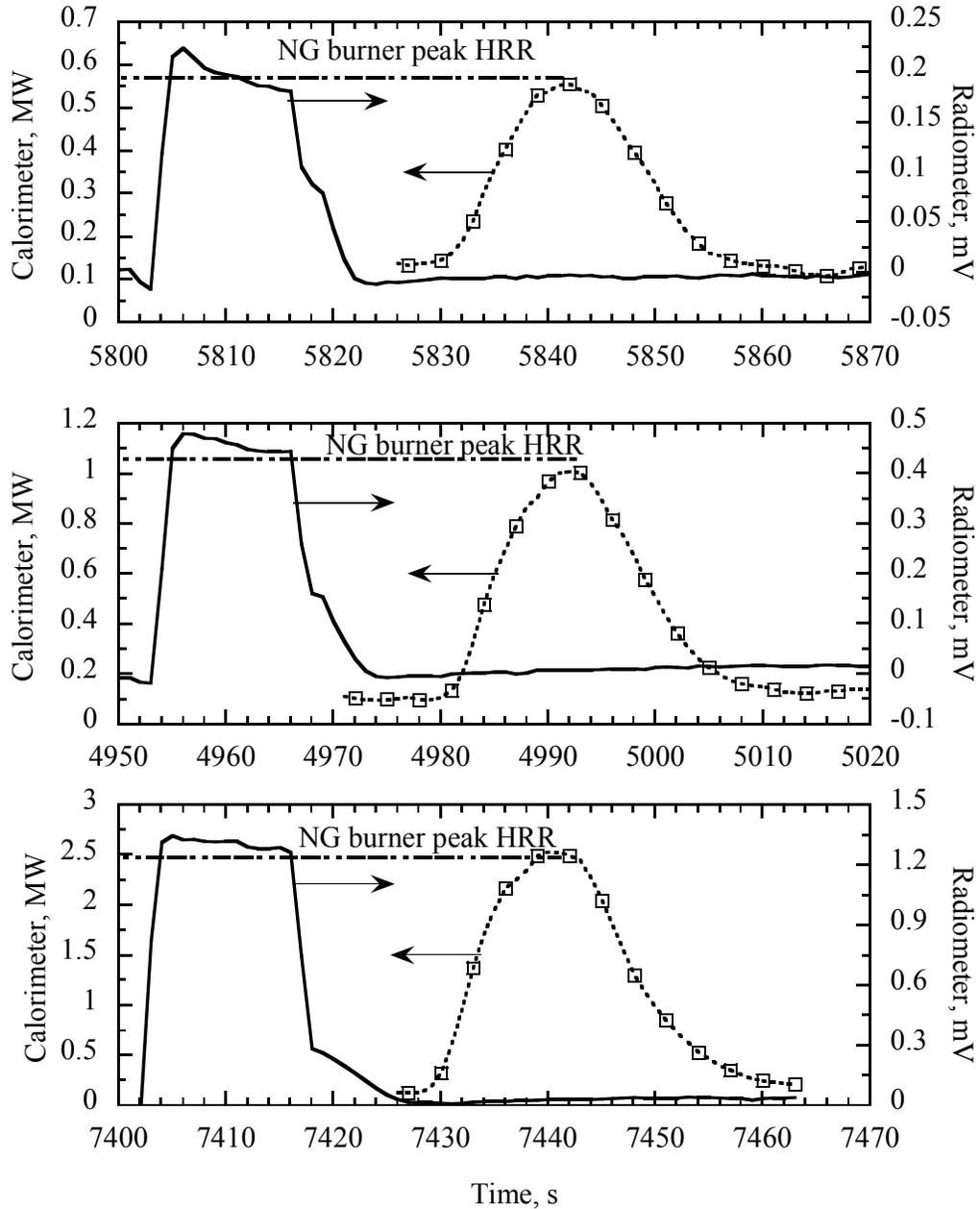


Figure 15 The heat release rate and the radiometer output as plotted versus time for 15 s pulses for HRR of 0.5 MW, 1 MW, and 2.5 MW

The pulse experiments for the other two heat release rates provided similar results. It is seen in Figure 15 for the 15 s square-wave pulses for the three heat release rates that the peak heights are similar to those of the NG burner, the FWHH are similar to those from the radiometer, and that the scaled shapes of all three calorimeter-generated curves are similar. There are slight differences in the radiometer-generated pulse shapes such as a flatter top section and a more abrupt decrease in the HRR at the end of the pulse for the larger heat release rates. These subtle changes do not seem to be reflected in the calorimeter-generated curves.

The total heat released by the pulse is equal to the area under the burner output curve. For energy conservation for the calorimeter system, the area under the calorimeter curve should equal the area under the burner curve. In Figure 14 the two areas appear to approximately match for the longer two pulses, but it is difficult to determine if this is the case for the shortest two pulses. A quantitative assessment of energy conservation was made by determining the total integrated heat released computed based on the burner flow and on the calorimeter output. The integrated area is that above the nominal 100 kW baseline. The baseline correction is estimated as the average of the baseline values before and after the pulse. The average ratio of the integrated calorimeter output to the integrated burner output for a fixed heat release rate is 0.98 ± 0.05 (see Table 1) and ranges from 0.89 to 1.06. The largest deviation from 1.0 occurs for the 5 s pulse at 1 MW. It is thought that the low number of pulses, about 3, counted per second is responsible for this decrease.

It was decided to again take advantage of the more rapid response time of the radiometer. A corrected total burner heat release was obtained by integrating the radiometer output and then multiplying by a calibration factor determined for each of the three heat release rates. The calibration factor was selected so that the radiometer “energy” equaled the integrated heat release rate from the gas burner for the 30 second experiment. The flow meter accuracy of the gas burner is improved about five-fold with the longer integration time. Using this approach, it was found that the average ratio of energies deviates by 6 % or less for the shortest to the longest pulse for any one burner setting. There is an increased uncertainty for the shortest pulse length. For the 5 second pulses, the range in the standard deviation is 4 % to 7 % of the mean compared to a more typical range of 1 % to 3 % of the mean for the longer pulses.

Energy conservation has been established to within the resolution of the experiment (see Table 1). This basic premise for obtaining a quantitative measurement of the total energy released regardless of how small a pulse is that the total oxygen consumed in the combustion reactions is obtained from the integrated oxygen analyzer output. This premise has been validated.

Table 1 Energy conservation results

Nominal pulse width, s	Integrated calorimeter output	Integrated calorimeter output ^a
	Integrated burner output	Integrated radiometer output
0.5 MW		
30	0.97 ± 0.01	0.97 ± 0.04
15	1.01 ± 0.03	0.98 ± 0.02
10	0.96 ± 0.01	0.92 ± 0.03
5	0.90 ± 0.06	0.92 ± 0.04
1 MW		
30	1.06 ± 0.02	1.06 ± 0.02
15	0.96 ± 0.03	1.05 ± 0.03
10	0.98 ± 0.02	1.10 ± 0.02
5	0.89 ± 0.04	1.05 ± 0.06
2.5 MW		
30	1.02 ± 0.01	1.02 ± 0.01
15	1.02 ± 0.02	1.05 ± 0.01
10	1.02 ± 0.02	1.07 ± 0.01
5	0.97 ± 0.04	1.06 ± 0.07

^a The integrated radiometer output for each of the three heat releases was multiplied by a factor to match the total burner heat release rate for the 30 s square-wave pulses.

A summary of the average peak HRR and FWHH and the associated standard deviations are given in Table 2 and Table 3 for each set of three or more repeat measurements. The FWHH is computed based on the half-height above the baseline value. The peak HRR is not adjusted for the baseline value. For pulse lengths of 15 s and longer, the calorimeter peak is within 9 % of the burner peak. The peaks correspond to the instantaneous maximum values recorded by the calorimeter, the corrected burner, or the radiometer. The five second-smoothed peaks were found to yield similar results except for the shortest pulse widths. The results indicate that the calorimeter peak is about 15 % smaller than the burner peak for the 10 s pulse and about 50 % smaller for the 5 s pulse. The results in Table 2 indicate that the calorimeter value on average is a factor of 1.03 ± 0.04 greater than the corrected burner peak for square-wave pulses having widths equal to or greater than 13 s. The calorimeter significantly underestimates the peak height for square wave pulses lasting less than 10 s.

The corrected burner peak heat release rate is not affected by the pulse width down to 5 s. The standard deviation of the burner peak heat release rate for the four pulse widths is at most 5 % of the average for any of the three HRR (see Table 3).

The FWHH time based on the calorimeter for the 1 MW fire is at most 10 % longer than the radiometer time for the 15 s and 30 s pulse experiments while it is about 25 % longer for the 10 s pulse and more than a factor of two longer for the 5 s pulse. Another observation is that the FWHH measured by the calorimeter remains relatively constant as the pulse width is reduced from 10 s to 5 s. In this limit, the calorimeter response is controlled by the time response of the oxygen analyzer so that the response approaches a constant independent of how short the square-wave pulse might be.

Table 2 Gas burner square-wave pulse results for peak HRR and FWHH

Pulse width, s	Calorimeter peak Burner peak	Radiometer FWHH, s	Calorimeter FWHH, s
0.5 MW			
60 ^a	1.03	59	58
30	0.97 ± 0.02	28.0 ± 0.2	29.3 ± 0.3
15	1.01 ± 0.06	12.6 ± 0.1	14.4 ± 0.2
10	0.89 ± 0.05	8.7 ± 0.6	11.1 ± 0.4
5	0.58 ± 0.02	3.8 ± 0.6	8.9 ± 0.7
1 MW			
60	1.06 ± 0.03	58.6 ± 0.7	59.3 ± 0.8
30	1.06 ± 0.01	29.3 ± 1.2	30.0 ± 1.7
15	0.96 ± 0.01	13.8 ± 0.5	15.2 ± 0.7
10	0.82 ± 0.06	8.1 ± 0.5	10.8 ± 0.3
5	0.52 ± 0.03	3.4 ± 0.2	8.9 ± 0.3
2.5 MW			
60 ^a	1.09	58	58
30	1.05 ± 0.03	28.2 ± 0.9	28.2 ± 0.8
15	1.04 ± 0.02	14.4 ± 0.1	14.7 ± 0.2
10	0.88 ± 0.03	8.7 ± 0.8	10.6 ± 0.1
5	0.47 ± 0.02	3.4 ± 0.2	10.3 ± 0.4

^aOnly one test performed.

The response of the calorimeter to the square-wave pulses suggests a possible method for checking whether the peak heat release rate is changing too rapidly to obtain an accurate heat release rate with the calorimeter. If the FWHH is 15 s or longer for the HRR calorimeter, then one has confidence from this study that the heat release is accurately represented by the data. However, if the FWHH is less than 11 s the peak heat release will likely be underestimated by 15 % or more. It does not appear to be possible to correct the peak heat release rate based on the FWHH, since small changes in the FWHH can result in a factor of two or more increase in the peak heat release rate, as seen in the data in Table 2. On the other hand, the square-wave pulse data may be useful in testing algorithms such as that developed by Abramowitz and Lyons [17] for deconvoluting the actual heat release rate from the measured values.

A second important issue is the effect of the random system noise on the apparent magnitude of the heat release peak and thus the uncertainty in the peak height. The random noise sources include the gas analyzers, the pressure transducers for measuring velocity, the thermocouples, real variations in the temperature, velocity, and gas levels being measured, variations in the pumps and exhaust fans, and changing ambient humidity and temperature. By looking at the peak heat release rate in repeat tests under nominally identical conditions, we can assess the effect of the calorimeter related noise sources on the measured peak. A convenient measure of repeatability is the coefficient of variation (CV), which is defined as the ratio of the standard deviation for repeat

measurements to the average value. We find that the CV for corrected peak burner heat release rate (see Table 3) is at most 0.05 for any of the 12 set of tests with at least three repeats each and is 0.02 or less for 5 of the 6 sets of tests with pulse widths of 15 s or 30 s. The CV for the calorimeter is also found to be in the range of 0.01 to 0.02 for 5 of the 6 sets of tests with pulse widths of 15 s or 30 s. The near equality of the CV's suggest that the calorimetry repeatability may be limited by the slight lack of repeatability in the square-wave pulse produced by the burner. Larger CVs up to 0.10 are obtained for heat release rate by the calorimeter for the 5 s and 10 s square-wave pulses.

Table 3 Gas burner square-wave pulse coefficient of variation (CV)

Nom. pulse width, s	Corrected burner peak, MW	Burner CV	Calorimeter peak MW	Calorimeter CV
0.5 MW				
30	0.59	0.01	0.56	0.02
15	0.56	0.04	0.56	0.03
10	0.56	0.05	0.45	0.02
5	0.54	0.04	0.34	0.10
Avg \pm σ	0.56 \pm 0.02			
1.0 MW				
30	1.00	0.02	1.06	0.02
15	1.05	0.01	1.00	0.01
10	1.05	0.03	0.85	0.06
5	1.04	0.01	0.53	0.04
Avg \pm σ	1.04 \pm 0.02			
2.5 MW				
30	2.53	0.02	2.63	0.02
15	2.47	0.01	2.57	0.01
10	2.52	0.01	2.23	0.04
5	2.46	0.02	1.14	0.02
Avg \pm σ	2.50 \pm 0.04			

It is encouraging that the contribution of the system noise to CV for the peak heat release rate for the 30 s and 15 s square-wave pulses is typically 0.01 to 0.02. However, this does not mean that the CV for repeat burns of identical furnishing items, consumer products, or building materials will be as small. The CV in HRR measurements for such materials may be far greater than 0.02 because the identical items may not really be “identical” due to material and/or construction variation or because the flame spread process occurring on real objects is very sensitive to the details of the ignition process as well as the ambient flow and temperature field. Fire growth processes on real objects of any complexity (e.g., mattresses or items of upholstered furniture) are notoriously difficult to reproduce precisely. Since these help dictate the shape of the heat release rate curve from the overall object, and its peak, one can expect appreciable variations in measured heat release rate for such items, even with an ideal calorimeter.

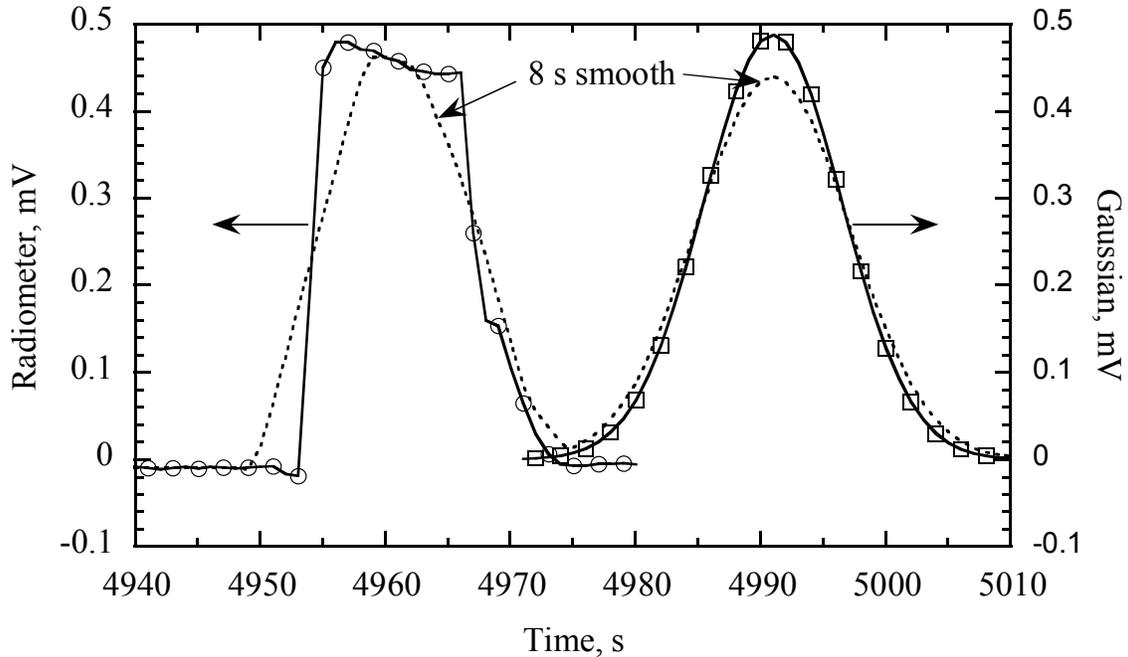


Figure 16 Comparison of the effect of 8 s smoothing on the peak height for a square-wave pulse vs. a Gaussian pulse. The peak heights for the square-wave pulse and Gaussian are 0.488 mV relative to the baseline, the FWHH is 13 s, and the standard deviation of the Gaussian is 5.52 s.

The analysis presented so far has computed measured time response characteristics for square-wave pulses. In reality it is likely that the peak will be more rounded in shape. A Gaussian peak is a useful example. In the domain where calorimeter response affects the results, one might expect the calorimeter peak heat release rate for a square-wave to be larger than for a Gaussian with the same FWHH. The estimate here is based on the 15 s square-wave pulse for the 1 MW fire plotted in Figure 13 with a FWHH of 13.0 s. A Gaussian pulse was modeled with a standard deviation of 5.44 s corresponding to the 13.0 s FWHH value. The magnitude of the Gaussian peak above the baseline was taken to be equal to the corresponding measured value. To simulate the system response of the calorimeter, an eight second smoothing was used for both the “square-wave” pulse and the Gaussian. As indicated in Figure 16, the Gaussian peak is decreased by about 10 % by including the time response of the system through smoothing while the decrease for the Square-wave peak is about 3 %. The reason for the closer approach to the peak for the square-wave is the ten-second duration at the maximum value compared to a one-second duration for the Gaussian. This effect offsets the much more rapid rise for the square-wave compared to the Gaussian. The difference in the peak heights for the two pulses will decrease for wider pulses and increase for shorter pulses.

The ability to reproducibly generate nominal square-wave heat pulses has been important to assessing the transient characteristics of the HRR calorimeter without the complicating effects of the fire spread and burning of real objects. One of the key results is the determination of the minimum pulse width needed to make an accurate measurement of

peak HRR. For fires with FWHH of 15 s or longer (as measured by the calorimeter), the calorimeter overestimates the actual peak heat release rate value by 3 % on average. However, if the FWHH measured by the calorimeter is less than 11 s, the measured peak heat release rate value underestimates the actual peak heat release rate by 15 % or more.

The burner was also key to assessing the repeatability performance of the calorimeter. The coefficient of variation, CV, for repeat measurements of the peak heat release rate (instantaneous value) of fire pulses with a duration of 15 s or greater is typically 0.02 or less for nominal 0.5 MW, 1.0 MW, and 2.5 MW fires. Such information is important in fire tests to separate calorimeter effects from the burning characteristics of real objects.

It was found that the calorimeter is able to provide a good estimate of the total heat released for square-wave pulses changing too rapidly for the peak to be resolved by the calorimeter. That is, the integrated heat release measured by the calorimeter conserves energy to within about 5 % for pulses as short as 5 s.

The fast response time of Schmidt-Boelter type radiometer was key to obtaining the most quantitative data on the gas burner output. It may be possible to combine the output of a radiometer, which has a time response of less than 1 s, with the integrated output from the calorimeter, which conserves energy, to estimate peak heat release rates for fires with FWHH as small as 3 s.

2.4.3 Factors Affecting Dispersion of the Gas Measurement Signals

As noted previously, the rise time of the O₂, CO and CO₂ signals depends not only on the inherent instrument response time¹⁴ but also on the time-wise dispersion of the gas concentration gradient due to mixing in the plume capture and gas sampling systems. Thus, the overall system response time assessed in the previous section is a product of various dispersion processes as well as instrument response characteristics.

A transient fire under the calorimeter hood results in some time-varying stream of gas concentrations emerging from the flame tips that carries information about fire size (heat release rate). As this stream of gases enters the hood, it is paralleled by (and partially mixed with) a flow of in-drawn excess air. A series of lateral, cross-sectional slices through these parallel streams, with the gases mixed laterally¹⁵, contains a perfect history of the heat release rate behavior of the fire below the hood. However, no real system is capable of mixing these incoming gas streams in a lateral direction only. Invariably there is longitudinal mixing as well and this means that the time history of the fire is being smeared out.

¹⁴ Instrument response time may be limited by the electronics and/or by the gas turnover time in the instrument's plumbing and measurement cell. The latter can be shortened by an increased sample flow rate but this is typically limited by pressure drop or other mechanical issues.

¹⁵ Lateral mixing (were it alone possible) brings with it only a lowering of the system sensitivity to heat release rate since it dilutes the fire plume gases.

There are numerous longitudinal mixing mechanisms in any real system; each causes the process referred to as dispersion. The mechanisms pertinent to the six-meter hood system can be listed as follows:

- Fire plume and duct flow turbulence
- Smoke build-up in the hood
- Flow separation in the bends of the hood duct
- Flow dispersion in the sampling line
- Mixing in the sample line filter and pumps
- Dilution from side arms on a sampling line
- Particle-induced mixing in the dry ice water trap and in the Drierite trap

If the fire is enclosed in a room below the hood, a configuration that is sometimes used with the six-meter hood, there will be an additional significant mechanism due to plume mixing in the room upper hot gas layer prior to emergence from the room. Assuming that the upper layer in such a room is well-mixed, this room-effect dispersion time is of the order of the upper layer volume divided by the plume volumetric flow rate. The upper layer volume is at least as great as the volume determined by the door soffit height and will be greater with increased heat release rate. A program such as CFAST [3] can provide a good estimate of the depth of the hot gas layer. CFAST agrees well with experimental results for the ISO 9705 room (2.4m by 3m by 2.4 m high with normal size door opening) [19]. The plume flow rate depends on heat release rate as well; Heskestad [11] provides the equations for this calculation. As an example, a 500 kW fire in an ISO 9705 room will have an estimated upper layer mixing time of 4 s to 8 s.¹⁶ This indicates that room dispersion effects can be substantial; as will be seen below, there is only one other element in the 3 MW system that normally yields comparable dispersion.¹⁷

We briefly consider the first item in the above list, which includes two dispersion mechanisms over which the experimenter has no control. The dispersion in the fire plume itself is a result of the intense turbulence typically existing there. For a 1 MW fire under the six-meter hood, one can show that the velocity-induced dispersion is of the order of ± 0.3 s in going from the top of the flames to the hood inlet. As to the second aspect, for a hood flow of $14.2 \text{ m}^3/\text{s}$, typical of that used for a large fire, the dispersion in the turbulent duct flow is of the order of ± 1 s (this dispersion mechanism is discussed further below in connection with the sampling line).

Here we elaborate further only on those mechanisms over which an experiment designer might want to try to exercise some control.

Confining the smoke build-up in the hood (including the skirted volume) might be thought of only as a safe way in which to handle a fire that temporarily becomes larger

¹⁶ An object yielding a 500 kW fire, when placed in a room will also see substantial radiative feedback from the hot smoke layer. This could significantly increase the peak HRR seen in a room versus that in an open hood, depending on the view factor the burning surfaces have toward the upper smoke layer.

¹⁷ One implication of this magnitude of room effect is that it has the potential to somewhat slow the overall system time response characteristics discussed in the above section on transient effects on HRR.

than anticipated. In fact the skirt serves precisely this purpose but it also has consequences with regard to dispersion of which one should be aware. The skirt acts only by allowing a volume in which smoke can accumulate. Once the accumulation occurs to some depth, the entrainment of excess air is decreased only because the plume begins to entrain and re-cycle the air/smoke mixture in the backed-up volume, rather than further excess air (above the smoke layer base height). Thus the mechanism by which a hood skirt works is inherently dispersive. However, simulation of this process using FDS shows that the accumulated smoke volume is not well-stirred with the incoming plume. Instead the bulk of a fire plume (if centered on the hood duct inlet axis) will pass straight through the back-up volume, unchanged. Only the outer portions of the fire plume are sheared off and subjected to this re-cycling. A consequence of this is that the dispersion process is weak, mixing only a minority of the flow, but extended in time (many seconds); therefore, the accumulated smoke volume is returned to the hood duct flow at a slow pace. The system user should try to avoid having the plume partially back up into the hood/skirt volume if precise monitoring of peak heat release rate is desired. This requires having a sufficient hood flow to swallow the diluted fire plume at its peak (see Ref. [10] for a discussion of hood flow calculations based on plume entrainment).

Flow dispersion in tube flow (both laminar and turbulent) is the subject of classic studies by G. I. Taylor [20]. Taylor shows that an instantaneous plug of fluid with a constant concentration of a gas species introduced into a fully developed turbulent flow results (after about 100 diameters of tube length) in a Gaussian distribution of that species, in time (or equivalent space). The width of the distribution is characterized by a dispersion coefficient that is a function of tube diameter and Reynolds number. Interestingly, Taylor's solutions indicate that even in the ca. 25 m sampling lines between the roof and the instruments in the control room, turbulent flow dispersion has a negligible effect (less than 0.1 s) on system dispersion, even when the added effects of flow bends are accounted for. The same reference was used for the estimate above of the more significant dispersion in the hood duct flow.

Dispersive mixing in such system elements as the sample filter upstream of the roof pump or the filters upstream of the control room pump(s) depends on the filter housing design. Such mixing would be eliminated if there are no separation zones for the flow but this tends to be incompatible with minimization of the size of the housing. Estimation of the possible mixing time constants (estimated flow separation volume over volumetric flow rate) for the existing filter housings implies that they are negligible sources of dispersion (less than 0.1 s) in the current system. The same applies to the sample pumps.

Any location in the sampling system that has a pipe tee to provide an alternate flow path (or a tee to facilitate a pressure gage)¹⁸ introduces a side arm with a dead volume. Inspection of Figure 6 indicates that there are such tees in the present system. Such a dead volume communicates with the main sample flow by a combination of diffusion and

¹⁸ Pressure gages do not need a significant flow in/out of their lead tube. Thus the lead tubes used in this system were made extremely small in diameter (1.5 mm OD tubing) in order to minimize their flow dispersive effects on the passing sample flow.

induced flow circulation. Thus the gas in such a volume mixes with the passing sample flow, altering its composition and acting, in effect, as a dispersive mechanism. Using the pure diffusion solution for a semi-infinite, stationary gas subjected at time zero to a differing gas concentration at its outer boundary [21] one can show that pure diffusion can only cause mass fluxes that would amount to a negligible source of dispersion. On the other hand, the flow past the side arm can be expected to induce a circulation eddy in the outer end of the side arm of length comparable to the side arm tube diameter. This outer induced eddy will in turn induce another eddy of comparable dimensions. Presumably this induction continues into the side arm to a depth dictated by viscous dissipation of these induced eddy motions. Successive eddies communicate by diffusion and some flow mixing thus extracting gas from the side arm at a potentially much greater rate than by pure static diffusion alone. While there is not a quantitative treatment of this process available, one can anticipate that it could become a significant source of dispersion, especially for larger diameter side arms (worst case example, the side arm on the hood flow duct seen in Figure 2). Such dispersion could manifest itself as a drift in the gas analyzer outputs or it could extend the time to zero the gas analyzers. There is one location in the gas sampling system (in the control room) where this becomes a concern and the operating procedure therefore calls for closing a valve near the tee in this sidearm to greatly shorten its effective length and to minimize this effect. This action should eliminate this source of dispersion as an area of concern in the present system.

The dry ice trap and the Drierite traps are both examples of packed beds. Flow dispersion in packed beds is a well-studied subject [22]. The complex flow of gas around the particles in a packed bed creates numerous paths of varying lengths along with minute separation zones, all of which spread the gas out in space (or time). The effect on a step function change in flow concentration as a result of axial dispersive processes in a successive set of particle beds like those used here for drying the sample flow can be reasonably well estimated. Given the particle size, gas flow rate and the length of the two drying devices, one can estimate that the combination smears an input step function in gas concentration over a time of about 4 seconds. These two drying devices are thus the most significant and routine sources of flow dispersion in the current system, though they do not add excessively to the basic system time response as set by the gas analyzer instruments themselves. If it became desirable to lessen the system response time further, it would be necessary to abandon the use of packed beds for gas flow drying. The Cone Calorimeter, for example, uses a laminar flow, thermoelectric cooling device. The sample flow is much greater here; it is not known whether an adequate device of this type is available.

The dominant response time in the gas sample analysis system is that due to the analyzers themselves. The oxygen analyzer, for example, has a nominal response time of 8 s (to 90 % of input change). The above discussion indicates that, in the absence of a room as a container for the fire being measured and also in the absence of significant smoke back-up in the hood, the dispersive elements in the system will add roughly 5 s to this, giving an overall time to response to a step change at the fire of about 12 s to 13 s (depending on the exact definition of response time one uses¹⁹ and ignoring flow lag times)²⁰. This is in

¹⁹ Most of the dispersive times are (1/e) estimates.

reasonable agreement with the results described in the preceding section on transient behavior of the heat release rate measurement system. Again it should be noted that use of a room or the existence of smoke back-up in the hood will increase the response time significantly, though the former will be more noticeable than the latter.

2.4.4 Flame Height vs. Heat Release Rate

The discussion by Heskestad [11] provides the basic equations governing the flame height from a pool fire, as a function of pool diameter. (Also included in the reference are other correlations for some other fire situations.) Since it is undesirable to allow the plume to be swallowed by the duct at the top of the hood, these flame height calculations provide one guideline for the system design, namely how far above the floor (the assumed fire location) the inlet duct needs to be in order to just capture the biggest fire for which the system is designed. The routine user of the system can also use such calculations to estimate whether the hood height will accommodate the planned fire. Since all fires do not act like simple pool fires²¹, one must use these calculations as a rough guide only and not push the upper limit without being prepared for some plume swallowing²².

Flame heights have been calculated to assist in the design of experiments and measurements using the various exhaust hoods in the Large Fire Research Facility. The primary consideration here is assuring that the visible flame tip does not enter the exhaust system. Prediction of flame height for the calibration gas burner is difficult. At low flow rates, the flame emanating from the burner can be classified as buoyant, using Delichatsios' Fire Froude Number [23]. However, with increasing gas flow the flame quickly transitions to a momentum dominated jet. Further complication of the problem results from flame merging. At low gas flow rates individual flamelets exist and then suddenly merge with increasing gas flow. It is unclear if the merging of individual flamelets occurs at the transition from a buoyant flame to a momentum driven jet.

To predict burner flame height, it was assumed that the burner flames behave in aggregate like a pool fire. The results of the pool fire calculation are also instructive in judging likely flame heights from other burning objects, as well as from the calibration gas burner. Figure 17 shows the calculated flame tip height as a function of heat release rate for pool fires with diameters of 0.5 m, 1.0 m, and 2 m. Note that heat release rate is the primary determinant of flame tip height; pool fire diameter is secondary. The flame tip height is defined as the sum of the mean flame height and one-half of the

²⁰ Also note that since all of these dispersive elements are in series, they are not strictly additive; rather the final result is the successive convolution of all preceding dispersive elements.

²¹ Anything that impedes plume entrainment, such as a wall on one side of a fire, tends to increase flame height. Anything that tends to enhance plume entrainment, such as a multi-segmented fire will shorten the flame height.

²² A small amount of plume swallowing will not likely suppress burning because the plume at its tip is over-aerated. This can be difficult to judge visually, however; a CO increase in the exhaust gases would be a better indicator. Since the gas temperature in the duct will go up rapidly if combustion continues there, there is a risk of damage to the system. Heavy swallowing of flames, especially for longer than times of the order of 10 s, is to be avoided.

intermittency flame length. The intermittency length gives the difference between the maximum and minimum visible flame height, whereas the mean flame height is defined as the mean value of the visible flame height. The mean flame height and the intermittency lengths were taken from Eq. (8) and Figure 14 in Heskestad [24]. Calculation of flame height for multiple jets that merge, using Heskestad's pool fire correlation, will over predict flame height.

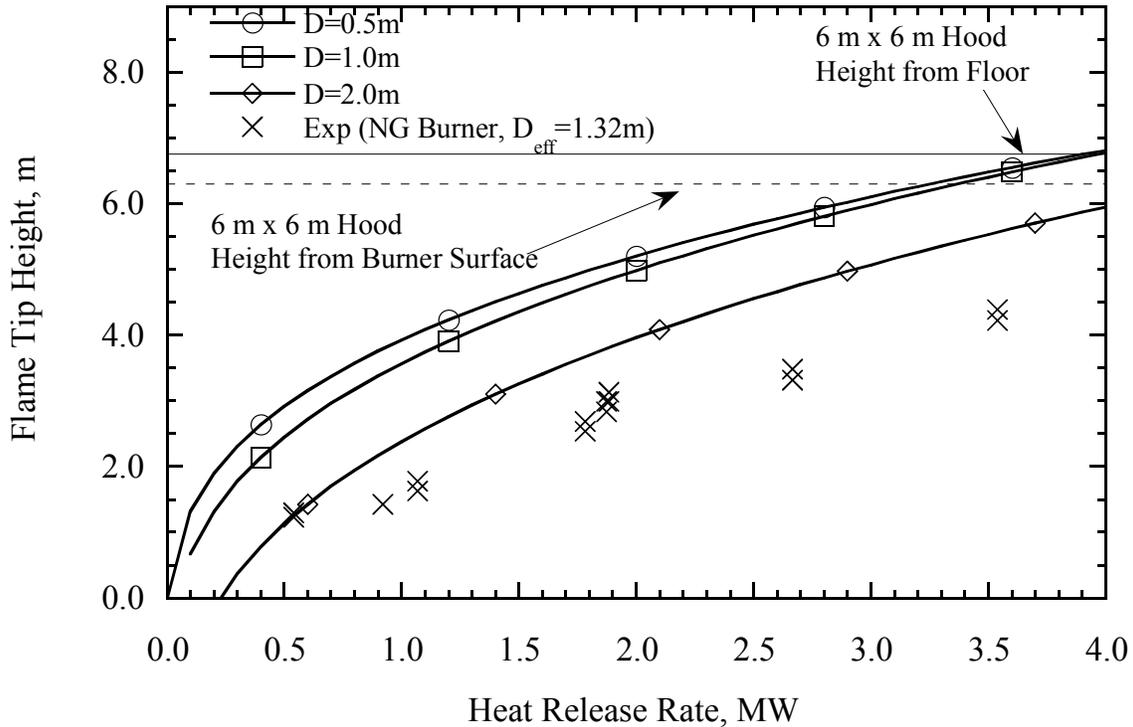


Figure 17 Calculated flame tip heights for pool fires and actual results for the natural gas calibration burner.

The average flame tip height for a 6 MW fire in a 0.5 m burner is approximately 1 m higher than the average flame length. The plot shows two horizontal lines that represent the distance above the floor (solid line) and the distance above the calibration burner to the exhaust in the 6 m x 6 m (3 MW capacity) hood. Figure 17 shows that the 6 m x 6 m hood may not accommodate a 4 MW fire unless it has a diameter of 2 m or greater. Fires of 4 MW or greater and with effective diameters of less than 2 m are better accommodated by the 9 m x 12 m hood.

Actual flame tip heights were measured when all eleven tubes were open. Flame tip height was determined using a 20 cm diameter protractor (1 degree angular resolution) to measure the angle between the line of sight to the flame tip and a horizontal reference line. The vertical position of the protractor above the floor and the horizontal location from the center of the burner was recorded. The height of the flame tip above the horizontal reference line is the tangent of the angle multiplied by the distance from the burner. Flame tip height above the floor (includes burner height) was computed by

adding the vertical position of the protractor to the previously determined height. The measured flame tip heights minus the burner height are shown in Figure 17. The scatter is due to a combination of the variability in the use of the simple tools and the difficulty in estimating the point defining the flame tip, which fluctuates strongly.

3 Operation and Safety

3.1 Calorimeter

The first steps to operating the calorimeter are to assure that the system is properly configured. This includes setting the exhaust hood flow to fit the anticipated fire size, bringing all components up to their normal operating temperatures, delivering the required flow from the sampling ports in the duct on the roof and feeding the correct flows to each of the analyzers. If any part of the gas analysis system has been opened (typically to insert clean water traps or particulate filters) it is checked for leaks. When everything is satisfactory, the data acquisition system (see Sec. 3.2 below) is initiated and calibration of the gas analyzers and zeroing of the pressure transducers on the bi-directional probes are performed. All analyzers are zeroed first using bottled nitrogen. They are then spanned with bottled calibration gases. After the system has fully recovered from the calibration process and is reading steadily once again the gas sample from the duct (with no fire), the no-fire baseline reading of the system, is recorded by the data acquisition system. When the actual test is initiated, the baseline is again followed for three to five minutes before the fire is ignited (ignition is denoted with a marker channel). After the fire has extinguished naturally (or with an extinguishing agent), the post-test, no-fire reading of the system is recorded for at least three to five minutes. These before- and after-fire readings give information used to construct the system baseline that applies during the test. If the fire is located in an enclosure, more time is allowed for smoke to clear and for the system to equilibrate.

The preceding steps involve various manipulations of the valves and switches on the control panels. Detailed and stepwise instructions are described in Appendix B.2.

3.2 Data Acquisition System

The first series of steps to running the data acquisition system is to make sure that the computer and DAQ hardware have power and that the Measurement and Automation Explorer and LabView software packages are running. The DAQ program is then opened with LabView. Once the DAQ program is loaded, adjustments to operating parameters are made (these changes are made with the program loaded, but not running). The channels to be scanned are set²³, the appropriate set of delay times for the hood flow is selected²⁴, span values (mainly gas cylinder volume fractions) are set, and calorimetry settings for the combustion products expansion factor and heat of combustion per mass of

²³ Generally, the calorimetry channels are well established and changes to the channel list would involve non-calorimetry-related measurements.

²⁴ If a hood flow other than the three offered is required, the channel delay times would have to be changed (and possibly measured first).

oxygen are entered. Particular chart history settings (the number of points retained on a chart) and the scan rate or averaging period (the default is 200/s and 1 s, respectively) must be entered before running the program. Ambient humidity and barometric pressure should be entered at this time and user-selected channels for display may also be set. These can be changed during the test as well.

At this point, the program is started, the main filename for the test is entered, and the calorimetry system is operated as described in Sec. 3.1. After the fire is ignited, the DAQ operator monitors conditions and performance and updates the humidity and barometric pressure periodically over the duration of the fire test. After the fire is extinguished, the system is allowed to return to ambient conditions to record a post-fire baseline. The DAQ operator also uses the event marker channels to mark events such as zeros, spans, ambient conditions, baseline HRR, ignition, extinguishing, and any other significant occurrences.

A detailed and stepwise description of the DAQ operating procedures is described in Appendix B.3.

3.3 Calibration Burner

It is recommended to operate the calibration burner prior to a series of fire tests for operational confirmation. Operation of the burner requires a minimum of two operators at all times, the safety officer and the DAQ operator. The safety officer is responsible for all manual tasks involved in start-up and shut-down of the burner, while the DAQ operator is responsible for all remotely controlled tasks such as specifying the burner output.

First the manual shut-off valve for the natural gas is opened and checks are made for proper operation of the igniters, the photoelectric sensor, and the solenoid valves. Once proper operation is confirmed, flow is initiated through the pilot tubes and the pilots are ignited using the DAQ burner control panel. Upon successful ignition a target heat release rate is specified at the DAQ burner control panel. The DAQ program provides a current to the natural gas control valve which has been calibrated to corresponding heat release rates, therefore giving remote control of the output of the burner. The burner and the DAQ burner control panel are monitored as the test proceeds, with all personnel being instructed to warn for unsafe conditions. The burner is shutdown by reducing the target heat release rate so that flow occurs through the pilot tubes and shutting off the flow control valve. The pilot flames eventually extinguish and the natural gas line is purged from the shut-off valve with nitrogen.

Detailed operation steps are described in Appendix B.4. It is important to follow these procedures to ensure safe operation of the calibration burner. Improper operation of the burner could produce an explosive mixture of natural gas and air within the building, possibly resulting in a catastrophic event. Emergency shut-down procedures are also described in Appendix B.4.

3.4 Safety

A fire of any size, whether controlled or un-controlled, is inherently hazardous. Therefore, when dealing with large fires, safety is a priority concern. Many active and passive safety mechanisms are in place in the Large Fire Research Laboratory. The most important of these mechanisms is allowing only adequately trained and experienced personnel to operate and participate in fire tests. Safety steps have been documented as part of the operations procedures for many of the components and tasks involved in a fire test. A fire test requires at least three personnel to comprise a test team. Each member of the testing team has a specific role and is required to update an operations checklist prior to beginning a fire test. The safety officer conducts a short meeting of the team members prior to the fire test to explain the test and reconfirm each member's responsibility. During this meeting each operations checklist is collected and reviewed by the safety officer to ensure that no safety steps are omitted. A general safety checklist is included in Appendix B.1 and should be followed as part of any fire test.

Other safety mechanisms include keeping the fire test area cleared for visual monitoring, employing communication devices to convey warning signals and event changes, having the properly sized water extinguishing system ready and, if necessary, having a trained and fully equipped firefighter on hand. There are safety systems to manage unforeseen failures of components like the natural gas burner such as manual shut-off valves and emergency shut-off buttons located near exits. Also the facility exhaust system is equipped with two exhaust trains to reduce the risk of complete failure of the system during a fire experiment. Finally, routine maintenance of the facility and its components is performed and safety procedures are reviewed annually.

3.5 Baseline Heat Release Rate

There is virtually always some drift in the gas analyzers, especially the oxygen analyzer. As a result there will be a non-zero (positive or negative) baseline measurement of heat release rate. This indicated value of heat release rate will exist before the fire test has started and after the fire (including smoldering) is fully extinguished (and the pre and post-test values will usually differ). The technique used to account for the baseline drift begins with allowing the heat release rate facility to operate for (3 to 5) min immediately prior to a fire test and (3 to 5) min immediately following full extinguishment of a fire test. The pre-test and post-test baselines are therefore determined, respectively. Figure 18 is a graphical example of a fire test performed with the calibration burner. Nominal heat release rates were 0.05 MW, 0.65 MW and 2.70 MW and a baseline drift from 0.005 to 0.020 MW was observed over the span of 54 minutes.

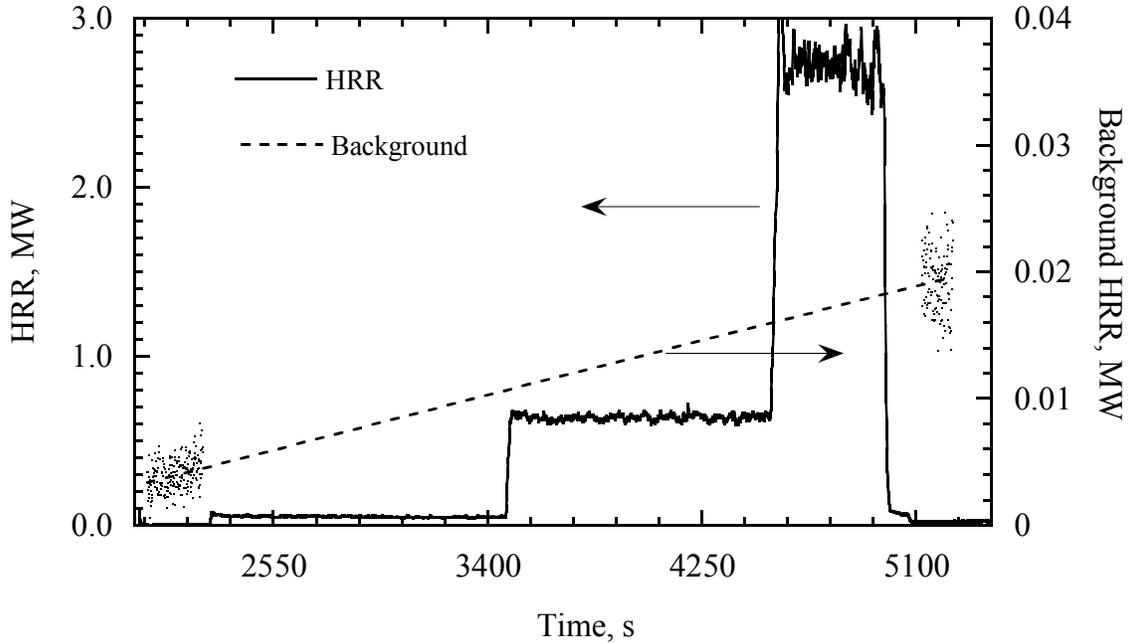


Figure 18 Time history of uncorrected heat release (left axis) and baseline heat release rate (right axis).

A time-varying relation for the baseline heat release rate, $\dot{q}_{bkgd,sys}$, relative to which all heat release rate measurements during a test were made, is determined by performing a least squares linear fit to the pre- and post-test data, Eq. (14) (see Figure 18). This relation assumes that the baseline drift of the facility is linear over the entire duration of the fire test. (30 minute drift test of the gas analyzers resulted in mostly linear positive or negative drift, therefore confirming this assumption) The estimated baseline heat release rate at time t is algebraically subtracted from the measured value of heat release rate at time t , Eq. (15). Performing this operation at each time step results in a time history of heat release rate corrected for the baseline drift of the system, $\dot{q}_{crctd,sys}$. This operation is especially important when evaluating peak heat release rate. The baseline will affect the characteristics, such as height and width, of the peak heat release rate curve.

$$\dot{q}_{bkgd,sys} = m_{sys}t + j_{sys} \quad (14)$$

$$\dot{q}_{crctd,sys} = \dot{q} - \dot{q}_{bkgd,sys} \quad (15)$$

The method outlined above measures the drift of the system as a whole. It will be referred to as Method I. The system drift is a result of the drift of the system components.

Since the raw data from each instrument is recorded for the pre- and post- test measurements, the baseline heat release rate due to the component drift also can be computed. The heat release rate is derived from the measured depletion of oxygen,

which is described mathematically (Eq. (7)) by the oxygen depletion factor, ϕ . Measurements of CO₂ and CO are also used to define ϕ . For the present report, the baseline drift of the three gas analyzers (O₂, CO₂, and CO) is used to compute a baseline drift of heat release rate from conditions at time, t=0. Least squares linear fits of the voltage outputs of each instrument, Eq. (16) to (18), are used to compute the gas species volume fraction drift. The baseline volume fractions are substituted into Eq. (13) to compute the baseline heat release rate due to the instrument drift.

Computing the baseline heat release rate due to the drift of the components will be referred to as Method II, and is represented by Eq. (19). Baseline heat release rates are computed by both methods for two series of test at random times within a series. The results are presented in Table 4 and show good agreement for the two methods of baseline HRR determination. The fractional difference, F_d , defined as (Method I - Method II)/Method I has a mean and standard deviation of 0.12 ± 0.10 . This good agreement indicates that most of the background drift can be accounted for by the drift of the gas analyzers.

$$V_{O_2,bkgd} = m_{V_{O_2}} t + j_{V_{O_2}} \quad (16)$$

$$V_{CO_2,bkgd} = m_{V_{CO_2}} t + j_{V_{CO_2}} \quad (17)$$

$$V_{CO,bkgd} = m_{V_{CO}} t + j_{V_{CO}} \quad (18)$$

$$\dot{q}_{bkgd,comp} = \dot{q}(\dots, V_{O_2,bkgd}, V_{CO_2,bkgd}, V_{CO,bkgd}, \dots) \quad (19)$$

Table 4 Baseline heat release rate comparison

Baseline heat release rate, kW		
System (Method I)	Component (Method II)	F_d
14.8	11.6	0.22
16.6	12.8	0.23
17.4	11.6	0.26
34.8	35.7	-0.03
39.5	38.8	0.02
51.9	50.2	0.03
55.8	52.1	0.07
65.1	57.1	0.12
	Avg \pm σ	0.12 \pm 0.10

4 Assessment of Uncertainty

A few studies exist which address the uncertainty of heat release rate measurements by oxygen consumption calorimetry. The studies vary in apparatus, version of the heat release rate equation, level of heat release rate, and detail of analysis. Axelsson et al. [25] estimated the heat release rate measurement uncertainty for the measurement as conducted in the Single Burning Item (prEN 13823) and the Room Corner Test (ISO 9705). The relative expanded uncertainty estimates ranged from 0.07 to 0.14, depending on the apparatus and the heat release rate. The uncertainty of the oxygen concentration measurement, followed by the heat of combustion factor and the mass flow rate measurement were identified as the major sources of uncertainty. Details on the uncertainty of the oxygen and the mass flow rate measurements were presented. The study notes that for larger oxygen deficits the combined uncertainty of the heat release rate measurement is less. Enright and Fleischmann [26] performed an analytical estimate of the heat release rate measurement uncertainty for the cone calorimeter. They estimated relative expanded uncertainty ranging from 0.10 to 0.12, depending on the heat release rate. The greatest sources of uncertainty identified were, the heat of combustion factor, the combustion expansion factor, and the oxygen measurement. Yeager [27] also performed an analytical uncertainty estimate for experiments conducted in a room compartment with a controlled supply of energy into the room and identified the volume flow rate and oxygen measurement as majors source of uncertainty. He reports a relative expanded uncertainty of 0.12 when the exhaust volume flow rate is optimized for the fire.

The oxygen depletion measurement and the exhaust mass flow rate measurement have been consistently reported as major sources of uncertainty. However, Janssens' [28] review of the results of heat release rate round robins brings attention to the uncertainty due to random effects such as material and burning variability, environmental effects, operator error, and measurement bias between laboratories. The impact of these effects is important and deserves further study. A crucial first step in such a study is a self-audit by the individual laboratories of their heat release measurement uncertainty. Such an assessment requires the use of a calibration burner with good repeatability to avoid the variability in the results from differences in the heat release rate for nominally identical solid fuel structures. The goal is to evaluate the calorimeter and one wants to avoid other sources of variability.

The self audit conducted here follows the methodology described in the ISO guidelines [29] and adopted by NIST [30]. The approach is to represent each component of uncertainty as a standard uncertainty. So called Type A uncertainties are those that can be computed based on statistics such as the standard deviation about the mean. The others, designated as Type B, require scientific judgment together with available data. A common example is knowing the maximum range of a variable and then converting this range into a standard uncertainty by dividing it by $2\sqrt{3}$ [30].

The calculation of the uncertainty in the heat release rate requires the combining of many components of uncertainty. This is apparent from the heat release rate equation, Eq. (13), which is a function of more than ten variables. There are five new aspects to the uncertainty analysis presented here as compared to previous analyses. The first concerns

the estimation of the uncertainty in the oxygen volume fraction to take into account the small noise relative to a much larger uncertainty in the calibration gas. A second is expressing all of the gas analyzer outputs in terms of their voltage to eliminate correlations induced in intermediate quantities by common measurement results. A third is subtracting a baseline drift from the gas analyzers and analyzing the uncertainty in the drift correction. The fourth is to perform the uncertainty propagation with a numerical method that is easily implemented in a spreadsheet program. And the fifth is to combine the total uncertainty based on the uncertainty propagation with the repeatability measurements to obtain a combined uncertainty and ultimately an expanded uncertainty corresponding to an approximate 95 % confidence interval. The assessment begins with estimating the uncertainty of individual Type A and B components.

4.1 Type A Uncertainty

Voltage

The standard uncertainty is estimated using the sample standard deviation of data collected during periods of operation at constant heat release rate or without any heat input into the system. This applies to all gas analyzer voltages and pressure transducer voltages. For each analyzer there are at least three voltage measurements. First, the voltage corresponding to the zero gas (nitrogen), second the voltage corresponding to the span gas, and last the voltage corresponding to the gas volume fraction at time t . For example, the voltage for the oxygen analyzer corresponding to a volume fraction of 0.2095 was approximately 0.833 V and the uncertainty in the voltage reading by the DAQ was $\pm 25 \mu\text{V}$.

Temperature

Type K thermocouples are employed for each of the temperature measurements. These thermocouples have fundamental error limits of $\pm 2.2 \text{ K}$. Assuming a rectangular distribution, the standard uncertainty is computed by dividing the limit by $\sqrt{3}$. The thermocouples are directly in the exhaust stream and are subject to fluctuations due to the turbulence in the exhaust duct. The standard deviation of 300 temperature measurements is nominally 1.0 K and is chosen to represent the noise due to turbulence. Combining the two standard deviations in quadrature results in a standard uncertainty of $\pm 1.6 \text{ K}$.

Repeatability

The mean and the standard deviation about the mean were computed for the six repeat heat release rate measurements for the nominal 0.05 MW, 0.65 MW, and the 2.70 MW natural gas burner flames.

Linear Least Squares Coefficients

The system and instrument drift data typically consist of 300 to 800 points. An Excel spreadsheet function "LINEST" is used to compute the coefficients for the linear fit. It also computes the standard deviation of the mean (or standard error) for each coefficient which is referred to here as the standard uncertainty. Before the regression analysis is run, the data are centered about the mean time, \bar{t} , which eliminates the covariance between the slope and the intercept.

4.2 Type B Uncertainty

Zero and Span Gases

The zero gas is 99.99 % nitrogen, therefore the measurements of zero O₂, CO₂, and CO volume fractions are assumed to have a standard uncertainty of ±0.0001. The O₂ span gas is breathing air that has an oxygen volume fraction of 0.2095 ±0.0005. Span gases for CO₂ and CO are purchased as a mixture of CO₂/CO/N₂. The volume fractions are specified and each bottle is delivered with a certificate of analysis specifying the actual volume fraction with a relative standard uncertainty of ±0.005.

Relative Humidity

Based on the manufacturer's technical specifications the accuracy of the humidity meter is ±2 % RH.

Ambient Pressure

The ambient pressure is read from a mercury barometer and corrected for temperature and altitude. The uncertainty in the reading is estimated to be ±0.27 kPa.

Bi-Directional Probe Constant, $C_{bdp,i}$

For flow with Reynolds number (relative to probe diameter) greater than 3800, the ratio of dynamic pressure to velocity is essentially constant and this constant value (0.0698 m³/K·kg) has been determined to be accurate to within ±5 % (±0.0035 m³/K·kg) [13]. The nominal range of Reynolds number for flows over the 2.54 cm bi-directional probes is 2000 to 16000.

Duct Diameter

The duct diameter, 1.52 m, is measured with a tape measure. Due to the duct not being a perfect circle the standard uncertainty is assumed to be ±0.01 m.

Heat Release of Fuel per kg of Oxygen Consumed, $(\Delta H_c)_{Mass_O_2}^{HC}$

The value of $(\Delta H_c)_{Mass_O_2}^{HC}$ for use if the fuel properties are not known is taken to be 13.1 MJ/kg O₂ based on the study of Huggett [5]. A slightly modified version of Table 2 of Huggett for typical synthetic polymers is used to compute the standard deviation in $(\Delta H_c)_{Mass_O_2}^{HC}$, ±0.35 MJ/kg O₂. The modifications were to delete polyoxymethylene, which is an outlier with an $(\Delta H_c)_{Mass_O_2}^{HC}$ of 14.5 MJ/kg O₂, and to add cellulose with an $(\Delta H_c)_{Mass_O_2}^{HC}$ of 13.59 MJ/kg O₂, which is representative of paper. The relative standard uncertainty is computed as ±0.027.

Natural gas, which contains typically 94% methane (as supplied by the local natural gas company) is used for calibration burns. Fuel composition is periodically determined from gas chromatograph results. The value of $(\Delta H_c)_{Mass_O_2}^{HC}$ for natural gas is 12.55 MJ/kg O₂ with an estimated standard relative uncertainty of ±0.00159 (±0.02 MJ/kg O₂). It is computed from the enthalpy balance for the complete combustion of natural gas

(major species) and oxygen to produce CO₂ and H₂O. (The complete combustion of pure methane and oxygen, which is a simpler computation of the enthalpy balance, results in $(\Delta H_c)_{Mass_O_2}^{HC} = 12.54$ MJ/kg O₂.) The NIST Chemistry WebBook lists the heat of formation for each molecule and the expanded uncertainty [31].

Heat Release of CO per kg of Oxygen Consumed, $(\Delta H_c)_{Mass_O_2}^{CO}$

The value of $(\Delta H_c)_{Mass_O_2}^{CO}$, computed from the enthalpy balance for the combustion of CO in oxygen to produce CO₂, is 17.69 MJ/kg O₂ with an estimated standard relative uncertainty of ± 0.0006 (± 0.01 MJ/kg O₂). The NIST Chemistry WebBook lists the heat of formation for each molecule and the expanded uncertainty [31].

Combustion Products Expansion Parameter, α

The expansion parameter α accounts for the volume of the combustion products exceeding that of the oxygen consumed. The quantity α can be related to the ratio of the moles of combustion products formed to the moles of oxygen consumed, which is denoted as β , via the following equation:

$$\alpha = 1 + X_{O_2}^o (\beta - 1) \quad (20)$$

where $X_{O_2}^o$ is the volume fraction of oxygen in ambient air, which is assumed to be 0.2095. As an example, the combustion of one mole of methane (CH₄) requires two moles of oxygen and produces three moles of product made up of one mole of CO₂ and two moles of water. The resulting values of β and α are 1.5 and 1.105.

The values of α for a range of common polymers found in constructed facilities are listed in Table 5. The mean value of α , 1.10, is used in the computation of the heat release rate if the properties of the fuel are unknown. In this case, the standard uncertainty for α is computed as the standard deviation of the values for the polymers listed in Table 5 with a value of ± 0.048 and a standard relative uncertainty of ± 0.044 .

Table 5 Expansion parameter α for polymers found in constructed facilities

Polymer	Formula	β	α
Polystyrene	(-C ₈ H ₈ -)	1.200	1.042
Polycarbonate	(-C ₁₆ H ₁₁ O ₃ -)	1.246	1.052
Polyethylene	(-C ₂ H ₄ -)	1.333	1.069
Polymethylmethacrylate	(-C ₅ H ₈ O ₂ -)	1.500	1.105
Polyvinylchloride	(-C ₂ H ₃ Cl-)	1.600	1.126
Polyurethane	(-C ₁₃ H ₆ O ₆ N ₂ -)	1.630	1.132
Cellulose	(-C ₆ H ₁₀ O ₅ -)	1.830	1.175
Avg $\pm \sigma$			1.100 \pm 0.048

4.3 Uncertainty Propagation

Suppose a general equation can be applied to describe a measurement process which has an output y and the output y is based on a number of input quantities, x_i .

$$y = y(x_1, x_2, x_3, \dots, x_N) \quad (21)$$

In the case that all input quantities are uncorrelated, the combined relative expanded uncertainty is given by

$$\frac{U_e(y)}{y} = k \frac{u_c(y)}{y} = k \sqrt{\sum_{i=1}^N s_i^2 \left(\frac{u(x_i)}{x_i} \right)^2} \quad (22)$$

In Eq. (22), $u(x_i)$ is the standard uncertainty for each input, $u_c(y)$ is the combined uncertainty, k is the coverage factor, and s_i is the associated dimensionless sensitivity coefficient given by

$$s_i = \frac{\partial y}{\partial x_i} \frac{x_i}{y} \quad (23)$$

4.3.1 Calibration Burner

An estimate of uncertainty for the natural gas burner heat output, $u_t(\dot{q}_{burner})$, is obtained by applying the propagation of uncertainty as described in Eq. (22). This includes the uncertainty of the three measured variables; namely pressure (P), temperature (T) and volumetric flow rate (\dot{V}) and the uncertainty of the natural gas heat of combustion ($(\Delta H_c)_{NG}$). The ideal heat output is computed from the following equation:

$$\dot{q}_{burner} = \dot{V} \frac{P}{P_{ref}} \frac{T_{ref}}{T} (\Delta H_c)_{NG} \quad (24)$$

Volumetric flow, temperature and pressure were measured and the volume flow rate was adjusted to represent the standard conditions for which the heat of combustion was determined. Since the ideal heat output is the multiplicative product of each measurement, the sensitivity coefficients reduce to 1.0 (or -1.0) and the resulting expression for the uncertainty is given in the following equation:

$$\frac{u_t(\dot{q}_{burner})}{\dot{q}_{burner}} = \sqrt{\left(\frac{u_P}{P} \right)^2 + \left(\frac{u_{\dot{V}}}{\dot{V}} \right)^2 + \left(-\frac{u_T}{T} \right)^2 + \left(\frac{u_{(\Delta H_c)_{NG}}}{(\Delta H_c)_{NG}} \right)^2} \quad (25)$$

The Type K thermocouple used to measure the natural gas temperature has error limits of ± 1.1 K, which corresponds to a standard uncertainty of ± 0.64 K when a rectangular

distribution is assumed. The uncertainty of the OmegaDyne pressure transducer is 0.10 % of the full range, which is 10.2 atm resulting in a standard uncertainty of ± 0.0102 atm. Nominal temperature and pressure are 293 K and 2.02 atm, respectively. The lower heating value of the natural gas heat of combustion was determined from gas chromatograph reports supplied by the local gas utility. The nominal value is 33,733 kJ/m³ (computed for reference conditions of 1 atm and 300 K) and the standard deviation, computed from gas chromatograph reports spanning six days, was ± 133 kJ/m³. Neither of these three variables are expected to fluctuate significantly during a test. The volumetric flow rate was the only dynamic variable in this calculation. It is determined from the ratio of the measured frequency of pulses, f , and the meter factor, K . The meter factor supplied by the manufacturer, $K=5.08 \times 10^{-4}$ pulses/cm³, is employed in the computation. This agrees with the mean meter factor taken from the results of the flow calibration as discussed in Appendix E.2. The standard deviation about the mean meter factor over the calibration range is $\pm 0.03 \times 10^{-4}$ pulses/cm³. Combined with the uncertainty in the pulse counting method, the standard relative uncertainty of the volumetric flow rate measurement is estimated at ± 0.01 . The standard relative uncertainty for the temperature, pressure and natural gas heat of combustion are, ± 0.002 , ± 0.005 , and ± 0.004 , respectively. Using Eq. (25), the total relative uncertainty for the ideal heat output of the calibration burner is calculated to be ± 0.012 .

4.3.2 Calorimetry

The relationship which applies to the measurement of heat release rate is given by Eq. (13), which is reproduced here for convenience.

$$\dot{q} = [(\Delta H_c)_{Mass_O_2}^{HC} \phi - ((\Delta H_c)_{Mass_O_2}^{CO} - (\Delta H_c)_{Mass_O_2}^{HC}) \frac{1-\phi}{2} \frac{X_{CO}}{X_{O_2}}] \frac{\dot{m}_e}{1 + \phi(\alpha - 1)} \left[\frac{(1 - X_{H_2O}^o) M_{O_2}}{M_{air}} \right] X_{O_2}^o \quad (13)$$

with

$$\phi = \frac{X_{O_2}^o (1 - X_{CO_2} - X_{CO}) - X_{O_2} (1 - X_{CO_2}^o)}{(1 - X_{O_2} - X_{CO_2} - X_{CO}) X_{O_2}^o}$$

As written the expression for \dot{q} contains parameters which are correlated or co-dependent, namely X_{O_2} and $X_{O_2}^o$, which violates the assumption leading to Eq. (22). In order to avoid such co-dependencies induced by common inputs, Eq. (13) must be reduced to the most basic measurement inputs of instrument voltages, thermocouple temperatures, and constant parameters (universal, empirical and calibration). This process is described for each of the measurement devices in text to follow.

The resulting measurement value for the project at hand is the heat release rate corrected for the baseline or zero measurement bias, the algebraic subtraction of Eq. (13) and (19).

The baseline heat release rate is determined by linear fits to the component data (Eq. (19), Method II). For the purpose of the uncertainty propagation, all data is centered about the mean time, \bar{t} (determined from the baseline data), which eliminates the covariance between the slope, m , and the intercept, j .

$$a = m(t - \bar{t}) + j \quad (26)$$

It is important to recognize that the quantity ϕ is proportional to $(X_{O_2}^o - X_{O_2})$ since the volume fraction of CO and CO₂ are small compared to that of oxygen. In addition the difference in the oxygen volume fractions is typically quite small. Some care must be taken in estimating the uncertainty in this case. An example is presented by Kragten [32] which illustrates the potential danger caused by ignoring correlations induced in intermediate measurement results by shared inputs. A similar example affecting the assessment of heat release rate is appended. The example illustrates the importance of performing an uncertainty analysis for the most basic inputs such as instrument voltage outputs and constants (empirical or universal). The relations for converting the instrument voltage outputs to units of more scientific significance follow.

Oxygen Analyzer

The oxygen analyzer produces a DC voltage [V] that is converted to the oxygen volume fraction by the following relation (includes the pressure correction):

$$X_{O_2} = \frac{V_{O_2} - V_{O_2,Zero}}{V_{O_2,Span} - V_{O_2,Zero}} (X_{O_2,Span} - X_{O_2,Zero}) \left(\frac{V_{O_2,press,Zero}}{V_{O_2,press}} \right) \quad (27)$$

where:

V_{O_2} = voltage measured by oxygen sensor at time, t

$V_{O_2,Zero}$ = voltage measured by oxygen sensor for the zero gas

$V_{O_2,Span}$ = voltage measured by oxygen sensor for the span gas

$X_{O_2,Span}$ = oxygen volume fraction of the span gas, bottled air (0.2095)

$X_{O_2,Zero}$ = oxygen volume fraction of the zero gas, nitrogen (N₂)

X_{O_2} = oxygen volume fraction computed with respect to voltage measurement at time, t

$V_{O_2,press}$ = voltage measured by absolute manometer to monitor pressure in the oxygen analyzer at time, t

$V_{O_2,press,Zero}$ = voltage measured by absolute manometer to monitor pressure in the oxygen analyzer during the zeroing of the instrument

The oxygen sensor is calibrated before each fire test to determine $V_{O_2,Span}$ and $V_{O_2,Zero}$. Absolute pressure is measured at the oxygen analyzer and the output is corrected for pressure fluctuations relative to the output when the instrument is zeroed.

Similarly, the relation converting the voltage output to the ambient oxygen volume fraction is:

$$X_{O_2}^o = \frac{V_{O_2}^o - V_{O_2,Zero}}{V_{O_2,Span} - V_{O_2,Zero}} (X_{O_2,Span} - X_{O_2,Zero}) \left(\frac{V_{O_2,press,Zero}}{V_{O_2,press}^o} \right) \quad (28)$$

The ambient oxygen measurement is conducted immediately after the spanning of the instruments. This value is then held as a constant in the computation.

Carbon Dioxide Analyzer

The carbon dioxide analyzer produces a DC voltage [V] that is converted to the carbon dioxide volume fraction by the following relation:

$$X_{CO_2} = \frac{V_{CO_2} RF_{CO_2} - V_{CO_2,Zero} RF_{CO_2,Zero}}{V_{CO_2,Span} RF_{CO_2,Span} - V_{CO_2,Zero} RF_{CO_2,Zero}} (X_{CO_2,Span} - X_{CO_2,Zero}) \quad (29)$$

where:

V_{CO_2} = voltage measured by CO₂ analyzer at time, t

$V_{CO_2,Zero}$ = voltage measured by CO₂ analyzer for the zero gas

$V_{CO_2,Span}$ = voltage measured by CO₂ analyzer for the span gas

$X_{CO_2,Span}$ = CO₂ volume fraction of the span gas, CO₂/CO/N₂ mixture

$X_{CO_2,Zero}$ = CO₂ volume fraction of the zero gas, N₂

RF_{CO_2} = range factor for the CO₂ voltage measured at time,t

$RF_{CO_2,Zero}$ = range factor for the CO₂ voltage measured when the instrument is zeroed

$RF_{CO_2,Span}$ = range factor for the CO₂ voltage measured when the instrument is spanned

The range factors are specific to the CO₂ analyzer employed. Depending on the range selected by the analyzer, a voltage is sent to the appropriate range channel of the data acquisition system. This voltage (V_{Ri}) is entered into the following relation to determine the range factor. The range factors are written to the adjusted data file.

$$RF_{CO_2} = AV_{R1} + BV_{R2} + CV_{R3} + DV_{R4} \quad (30)$$

Similarly, the voltage output converted to the ambient carbon dioxide volume fraction is:

$$X_{CO_2}^o = \frac{V_{CO_2}^o RF_{CO_2}^o - V_{CO_2,Zero} RF_{CO_2,Zero}}{V_{CO_2,Span} RF_{CO_2,Span} - V_{CO_2,Zero} RF_{CO_2,Zero}} (X_{CO_2,Span} - X_{CO_2,Zero}) \quad (31)$$

Carbon Monoxide Analyzer

The carbon monoxide analyzer produces a DC voltage [V] that is converted to the carbon monoxide volume fraction by the following relation:

$$X_{CO} = \frac{V_{CO} RF_{CO} - V_{CO,Zero} RF_{CO,Zero}}{V_{CO,Span} RF_{CO,Span} - V_{CO,Zero} RF_{CO,Zero}} (X_{CO,Span} - X_{CO,Zero}) \quad (32)$$

where:

V_{CO} = voltage measured by CO analyzer at time, t

$V_{CO,Zero}$ = voltage measured by CO analyzer for the zero gas

$V_{CO,Span}$ = voltage measured by CO analyzer for the span gas

$X_{CO,Span}$ = CO volume fraction of the span gas, CO₂/CO/N₂ mixture

$X_{CO,Zero}$ = CO volume fraction of the zero gas, N₂

RF_{CO} = range factor for the CO voltage measured at time, t.

$RF_{CO,Zero}$ = range factor for the CO voltage measured when the instrument is zeroed

$RF_{CO,Span}$ = range factor for the CO voltage measured when the instrument is spanned

The range factors will be specific to the CO analyzer employed. Depending on the range selected by the analyzer, a voltage is sent to the appropriate range channel of the data acquisition system. This voltage (V_{Ri}) is entered into the following relation to determine the range factor. The range factors are written to the adjusted data file.

$$RF_{CO} = AV_{R1} + BV_{R2} + CV_{R3} + DV_{R4} \quad (33)$$

Ambient Water Vapor

Relative humidity (RH , [%]) is read from a humidity meter located in the data acquisition control room. The ambient temperature (T_{amb} , [°C]) is measured from a thermocouple located on the data acquisition rack. The signal condition modules convert the thermocouple millivolt signal to degrees C before it is used in the HRR computation. Ambient pressure (P_{amb} , [torr]) is read from a mercury barometer located in the high bay area of the Large Fire Laboratory. The reading is corrected for altitude and temperature. The three measurements are used in the following relation [33] to infer the volume fraction of water vapor at ambient conditions.

$$X_{H_2O}^o = \frac{RH}{100} \frac{760}{P_{amb} 101.3} (5.5259 \times 10^{-7} T_{amb}^4 + 1.7195 \times 10^{-5} T_{amb}^3 + 1.5678 \times 10^{-3} T_{amb}^2 + 0.043725 T_{amb} + 0.611) \quad (34)$$

Exhaust Duct Bi-Directional Probes and Thermocouples

The bi-directional probes produce a DC voltage ($V_{bdp,i}$) that is converted to a differential pressure by the following relation:

$$\Delta P_i [Pa] = 133.322 b_i (V_{bdp,i} - V_{bdp,i,Zero}) \quad (35)$$

where b_i [torr / V] is the calibration coefficient of each probe and 133.322 [Pa / torr] is the conversion factor for torr to Pascals. The voltage measured when each probe is zeroed is $V_{bdp,i,Zero}$.

At each probe location a temperature is measured, $T_{bdp,i}$. The signal condition modules convert the thermocouple millivolt signal to degrees C. The pressure differential and temperature measurements are employed in the following relation to infer the exhaust gas velocity at each probe location.

$$U_{bdp,i} = C_{bdp} \sqrt{\Delta P_i (T_{bdp,i} + 273.15)} \quad (36)$$

where

$$C_{bdp} = \frac{1}{C} \sqrt{\frac{2R}{P_{ref} MW_{air}}} = 0.0698 \quad (37)$$

when $C=1.08 \pm 0.05$ as determined by McCaffrey and Heskestad [13].

The average velocity and average temperature for the six probes are computed to represent the velocity and temperature in the exhaust duct at the gas sampling point.

$$U_{avg} = \frac{0.0698}{6} \sum_{i=1}^6 \sqrt{133.322 b_i (V_{bdp,i} - V_{bdp,i,Zero}) (T_{bdp,i} + 273.15)} \quad (38)$$

$$T_{avg} = \frac{1}{6} \sum_{i=1}^6 (T_{bdp,i} + 273.15) \quad (39)$$

The mass flow rate ([kg/s]) of the exhaust duct is then computed by the following relation:

$$\dot{m}_e = \frac{\frac{0.0698}{6} \sum_{i=1}^6 \sqrt{133.322 b_i (V_{bdp,i} - V_{bdp,i,Zero}) (T_{bdp,i} + 273.15)}}{\frac{1}{6} \sum_{i=1}^6 (T_{bdp,i} + 273.15)} \rho_{air,ref} T_{ref} \frac{\pi D^2}{4} \quad (40)$$

where $\rho_{air,ref}$ (1.1767 kg/m³) is the density of the reference gas (dry air), T_{ref} (300 K) is the temperature of the reference gas, and D (1.52 m) is the inside diameter of the exhaust duct at the probe location.

A close inspection of all of the relations presented above will reveal the co-dependent input parameters of Eq. (13). The co-dependent pairs are $(X_{O_2}, X_{O_2}^o)$, $(X_{CO_2}, X_{CO_2}^o)$, and $(U_{bdp,i}, T_{bdp,i})$. These parameters share variables or one is dependent upon the other as in

the case of $U_{bdp,i}$ and $T_{bdp,i}$. Therefore it is recommended to break down the computation to the basic input measurements before beginning an uncertainty propagation to properly account for the co-dependence in intermediate quantities.

A major justification for the added complexity to the uncertainty propagation is specific to the heat release measurement as conducted in this laboratory and is illustrated by the appended example. The heat release measurement is based on oxygen consumption calorimetry and is therefore directly proportional to the difference between the measurements of oxygen and ambient oxygen volume fraction, $(X_{O_2}^o - X_{O_2})$. The combined uncertainty for each term of the oxygen difference is dominated by the uncertainty of the oxygen volume fraction of the span gas. This uncertainty is on the order of 3 times greater than the oxygen difference measured in small fires. By rewriting Eq. (13) in terms of the basic inputs, the uncertainty of the span gas will be correctly accounted for and will not give an erroneously large uncertainty for the oxygen difference, as would be the case if Eq. (13) were used directly.

Rewriting Eq. (13) in terms of the basic input measurements results in a final equation that consists of 64 input parameters. The parameters are listed in Table 6 and the equations, in terms of basic inputs, for each measurement instrument were presented above.

A numerical approach to Eq. (22) as described by Kragten [32] has the advantage of being easily implemented in an Excel spreadsheet. The method numerically approximates all the partial derivatives and calculates the combined standard uncertainty without the use of intermediate quantities that violate the condition of mutual independence. It is a spreadsheet-based format that offers relatively easy tracking of the contribution of uncertainty of each parameter. An example of the spreadsheet developed for this project is shown in Figure 19. The details of creating a spreadsheet uncertainty propagation are explained in Ref. [32].

The uncertainty of the heat release rate measurement varies with the operating conditions of the calorimeter and the size of the fire. A series of experiments was conducted with the natural gas calibration burner targeted at 0.50 MW, 0.65 MW, and 2.70 MW, to produce nominal values for the uncertainty analysis. The measurements were corrected for the background drift by applying Method II as described in Sec. 3.5 and the uncertainty propagation was performed on the resulting relation for the corrected heat release rate. Due to the background correction the number of parameters increases from 64 to 70.

	A	B	C	D	E	F	G	H	I	J
1										
2										
3			u(VO2)	u(VO2_Zero)	u(VO2_Span)	u(XO2_Zero)	u(XO2_Span)	u(VO2_press)	u(VO2_press_Zero)	u(VO2_amb)
4			0.00002500	0.00002500	0.00002500	0.00010000	0.00050000	0.00023000	0.00006000	0.000024
5		df	999999	999999	999999	999999	999999	999999	999999	9999
6	Measurement Equation Input	Value								
7	VO2 [V]	0.81798500	0.81801000	0.81798500	0.81798500	0.81798500	0.81798500	0.81798500	0.81798500	0.817985
8	VO2_Zero [V]	-0.00290000	-0.00290000	-0.00287500	-0.00290000	-0.00290000	-0.00290000	-0.00290000	-0.00290000	-0.002900
9	VO2_Span [V]	0.83296500	0.83296500	0.83296500	0.83299000	0.83296500	0.83296500	0.83296500	0.83296500	0.832965
10	XO2_Zero [-]	0.00000000	0.00000000	0.00000000	0.00000000	0.00010000	0.00000000	0.00000000	0.00000000	0.000000
11	XO2_Span [-]	0.20950000	0.20950000	0.20950000	0.20950000	0.20950000	0.21000000	0.20950000	0.20950000	0.209500
12	VO2_press [M]	-7.47735000	-7.47735000	-7.47735000	-7.47735000	-7.47735000	-7.47735000	-7.47712000	-7.47735000	-7.477350
13	VO2_press_Zero [M]	-7.48270000	-7.48270000	-7.48270000	-7.48270000	-7.48270000	-7.48270000	-7.48264000	-7.48270000	-7.482700
14	VO2_amb [M]	0.83278384	0.83278384	0.83278384	0.83278384	0.83278384	0.83278384	0.83278384	0.83278384	0.832807
15	VO2_press_amb [M]	-7.48030130	-7.48030130	-7.48030130	-7.48030130	-7.48030130	-7.48030130	-7.48030130	-7.48030130	-7.480301
16	VCO2 [M]	0.23657600	0.23657600	0.23657600	0.23657600	0.23657600	0.23657600	0.23657600	0.23657600	0.236576
17	VCO2_Zero [M]	-0.00440000	-0.00440000	-0.00440000	-0.00440000	-0.00440000	-0.00440000	-0.00440000	-0.00440000	-0.004400
18	VCO2_Span [M]	1.62930000	1.62930000	1.62930000	1.62930000	1.62930000	1.62930000	1.62930000	1.62930000	1.629300
19	XCO2_Zero [-]	0.00000000	0.00000000	0.00000000	0.00000000	0.00000000	0.00000000	0.00000000	0.00000000	0.000000
20	XCO2_Span [-]	0.10100000	0.10100000	0.10100000	0.10100000	0.10100000	0.10100000	0.10100000	0.10100000	0.101000
87										
88	(HRR) qdot [kW]	635.35	634.11	635.37	635.33	634.97	637.26	634.10	635.34	636.
89			-1.24	0.02	-0.02	-0.38	1.91	-1.25	-0.01	1.
90	u [kW]	36.43	1.53	0.00	0.00	0.15	3.64	1.56	0.00	1.
91	df	96861550916								
92	k	#NUM!								
93	U	#NUM!								
94										
95	rel u(qdot)	5.7%								
96										
97	VO2_drift	0.832224	0.832224	0.832224	0.832224	0.832224	0.832224	0.832224	0.832224	0.8322
98	XO2_drift	0.20946411	0.20946411	0.20946411	0.20945785	0.20936413	0.20996403	0.20947056	0.20946244	0.209464
99	VCO2_drift	0.03532327	0.03532327	0.03532327	0.03532327	0.03532327	0.03532327	0.03532327	0.03532327	0.035323
100	XCO2_drift	0.00041187	0.00041187	0.00041187	0.00041187	0.00041187	0.00041187	0.00041187	0.00041187	0.000411
101	VCO_drift	-0.00617654	-0.00617654	-0.00617654	-0.00617654	-0.00617654	-0.00617654	-0.00617654	-0.00617654	-0.006176
102	XCO_drift	-0.00001254	-0.00001254	-0.00001254	-0.00001254	-0.00001254	-0.00001254	-0.00001254	-0.00001254	-0.000012
103	phi_dte-to-drift	0.00034004	0.00034004	0.00034006	0.00034003	0.00033999	0.00034025	0.00030113	0.00034004	0.000376
104	bkgdHRR [kW]	11.63	11.63	11.63	11.62	11.62	11.66	10.34	11.63	12.
105										
106	crctdHRR [kW]	623.72	622.49	623.75	623.70	623.35	625.60	623.76	623.72	623.
107			-1.24	0.02	-0.02	-0.37	1.87	0.03	-0.01	-0.
108	u [kW]	35.73	1.53	0.00	0.00	0.14	3.51	0.00	0.00	0.
109	rel u(qcrctd)	5.7%								
110										
111	Color Key									
112	Variable measurement									
113	\HRR(qdot) \XO2 \XO2_amb \XCO2 \XCO2_amb \XCO \XH2O_amb \Ubdp,1 \Ubdp,2 \Ubdp,3 \Ubdp,4 \Ubdp,5 \Ubdp,6 \Uavg \Tav									
114	Ready									

Figure 19 Example of Kragten spreadsheet for computing HRR uncertainty.

The uncertainty for these measurements is presented in Table 6 including the total relative uncertainty, u_r . Each of the 70 input parameters is listed with its nominal value, relative standard uncertainty and its non-dimensional sensitivity coefficient. The quantities labeled as “Constant” are quantities that may or may not vary between uses of the calorimeter while those labeled “Variable” fluctuate during use of the calorimeter. Type A or B determinations are indicated by either “A” or “B” in parenthesis. By visual inspection of the table, the product of the sensitivity coefficient and the relative standard uncertainty help to quantify the contribution to the total uncertainty. Therefore parameters with absolute values of sensitivity coefficients equal to or greater than unity are expected to make a greater contribution to the total uncertainty.

Table 6 Corrected heat release rate relative uncertainty

Parameter/measurement [units] (type)	Nominal value	Relative standard uncertainty, $u(x_i) / x_i$	Sensitivity coefficient, $ s_i $		
			0.05 MW	0.65 MW	2.70 MW
$X_{O_2}, X_{O_2}^o, [-]$					
$V_{O_2}, [V]$ (variable)	0.817985	0.00003 (A)	1113	80.2	16.35
$V_{O_2,Zero}, [V]$ (constant)	-0.002900	0.00869 (A)	0.004	0.004	0.004
$V_{O_2,Span}, [V]$ (constant)	0.832965	0.00003 (A)	1.253	1.256	1.24
$X_{O_2,Zero}, [-]$ (constant)	0.0000	0.0001 (B) absolute	-	-	-
$X_{O_2,Span}, [-]$ (constant)	0.2095	0.00239 (B)	1.258	1.261	1.245
$V_{O_2,press}, [V]$ (variable)	-7.47735	0.00003 (A)	1.774	1.776	1.752
$V_{O_2,press,Zero}, [V]$ (constant)	-7.48270	0.00001 (A)	1.257	1.260	1.244
$V_{O_2}^o, [V]$ (constant)	0.832784	0.00003 (A)	0.515	0.514	0.506
$V_{O_2,press}^o, [V]$ (constant)	-7.480301	0.00001 (A)	0.517	0.516	0.508
$X_{CO_2}, X_{CO_2}^o, [-]$					
$V_{CO_2}, [V]$ (variable)	0.236576	0.01704 (A)	0.549	0.169	0.133
$V_{CO_2,Zero}, [V]$ (constant)	-0.00440	0.10400 (A)	0.000	0.000	0.000
$V_{CO_2,Span}, [V]$ (constant)	1.629300	0.00046 (A)	0.135	0.139	0.127
$X_{CO_2,Zero}, [-]$ (constant)	0.0000	0.0001 (B) absolute	-	-	-
$X_{CO_2,Span}, [-]$ (constant)	0.10100	0.00500 (B)	0.136	0.139	0.127
$RF_{CO_2}, [-]$ (variable)	1.039	0.00000 (B)	0.549	0.169	0.133
$RF_{CO_2,Zero}, [-]$ (constant)	1.039	0.00000 (B)	0.000	0.000	0.000
$RF_{CO_2,Span}, [-]$ (constant)	6.209	0.00000 (B)	0.136	0.139	0.127
$V_{CO_2}^o, [V]$ (constant)	0.033502	0.01309 (A)	0.001	0.001	0.001
$RF_{CO_2}^o, [-]$ (constant)	1.039	0.00000 (B)	0.414	0.030	0.006

Values expected to contribute significantly to the total uncertainty are in **bold**.

Table 6 Continued – Corrected heat release rate relative uncertainty

Parameter/measurement [units] (type)	Nominal value	Relative standard uncertainty, $u(x_i) / x_i$	Sensitivity coefficient, $ s_i $		
			0.05 MW	0.65 MW	2.70 MW
$X_{CO}, [-]$					
$V_{CO}, [V]$ (variable)	-0.01014	0.04726 (A)	0.066	0.004	0.001
$V_{CO,Zero}, [V]$ (constant)	-0.00320	0.14629 (A)	0.000	0.000	0.000
$V_{CO,Span}, [V]$ (constant)	2.20140	0.00029 (A)	0.013	0.000	0.000
$X_{CO,Zero}, [-]$ (constant)	0.0000	0.0001 (B)	-	-	-
absolute					
$X_{CO,Span}, [-]$ (constant)	0.09080	0.00500 (B)	0.013	0.000	0.000
$RF_{CO}, [-]$ (variable)	0.62	0.00000 (B)	0.066	0.004	0.001
$RF_{CO,Zero}, [-]$ (constant)	0.62	0.00000 (B)	0.054	0.004	0.001
$RF_{CO,Span}, [-]$ (constant)	6.069	0.00000 (B)	0.013	0.000	0.000
$X_{H_2O}^o, [-]$					
$RH, [\%]$ (variable)	45	0.04038 (B)	0.020	0.020	0.021
$P_{amb}, [torr]$ (variable)	754.10	0.00266 (B)	0.020	0.020	0.021
$T_{amb}, [^{\circ}C]$ (variable)	30.0	0.05095 (A)	0.035	0.035	0.036
$U_{bdp,avg}, [m/s], T_{bdp,avg}, [K], \dot{m}_e, [kg/s]$					
$C_{bdp}, [m^3/K\text{-kg}]$ (constant)	0.0698	0.05014 (B)	1.00	1.00	1.00
$b_i, [torr/V]$ (constant)	0.10	0.00000 (B)	0.083	0.083	0.083
$V_{bdp,i}, [V]$ (variable)	1.80721	0.06231 (A)	0.082	0.082	0.082
$V_{bdp,i,Zero}, [V]$ (constant)	-0.014417	0.79906 (A)	0.000	0.000	0.000
$T_{bdp,i}, [K]$ (variable)	343.0	0.00466 (A)	0.010	0.010	0.010
$\rho_{air,ref}, [kg/m^3]$ (constant)	1.1767	0.00000 (B)	1.000	1.000	1.000
$T_{ref}, [K]$ (constant)	300	0.00000 (B)	1.000	1.000	1.000
$D, [m]$ (constant)	1.52	0.00661 (B)	2.007	2.007	2.007
Constants					
$(\Delta H_c)_{Mass_O_2}^{HC}, [MJ/kg]$ $O_2]$ (constant)	12.55	0.00159 (B)	0.981	1.000	1.000
$(\Delta H_c)_{Mass_O_2}^{CO}, [MJ/kg]$ $O_2]$, (constant)	17.60	0.00057 (B)	0.019	0.000	0.000
$\alpha, [-]$ (constant)	1.10	0.04364 (A)	0.003	0.019	0.079
$MW_{O_2}, [kg/mole]$ (constant)	32.00	0.00000 (B)	1.000	1.000	1.000
$MW_{air}, [kg/mole]$ (constant)	28.967	0.00000 (B)	1.000	1.000	1.000

Values expected to contribute significantly to the total uncertainty are in **bold**.

Table 6 Continued – Corrected heat release rate relative uncertainty

Parameter/measurement [units] (type)	Nominal value	Relative standard uncertainty, $u(x_i) / x_i$	Sensitivity coefficient, $ s_i $		
			0.05 MW	0.65 MW	2.70 MW
$V_{O_2,drift}$, [V]					
$m_{V_{O_2}}$, [V/s] (constant)	-2.43×10^{-7}	0.00344 (A)	0.269	0.002	0.002
$j_{V_{O_2}}$, [V] (constant)	0.832475	0.00000 (A)	1115	81.99	18.10
$V_{CO_2,drift}$, [V]					
$m_{V_{CO_2}}$, [V/s] (constant)	9.09×10^{-7}	0.14630 (A)	0.000	0.000	0.000
$j_{V_{CO_2}}$, [V] (constant)	0.034387	0.00403 (A)	0.414	0.031	0.007
$V_{CO,drift}$, [V]					
$m_{V_{CO}}$, [V/s] (constant)	-7.95×10^{-7}	0.71062 (A)	0.002	0.000	0.000
$j_{V_{CO}}$, [V] (constant)	-0.00536	0.02411 (A)	0.051	0.004	0.001
t_s , [s] (variable)		0.00000 (B)	0.217	0.002	0.003
		u_t / \dot{q}_{crctd}	0.075	0.053	0.053

Values expected to contribute significantly to the total uncertainty are in **bold**.

At first glance, parameters with sensitivity coefficients much greater than unity are expected to be the largest contributors to the combined uncertainty. However these parameters (the oxygen analyzer voltage, V_{O_2} , and the intercept for oxygen analyzer voltage drift measurement, $j_{V_{O_2}}$) have very small relative uncertainty. Their contribution is most significant at very low heat release rate, as evidenced by the increase in the magnitude of the sensitivity coefficient. The parameters with sensitivity coefficients near unity and standard relative uncertainty greater than 0.01 are the significant contributors across the entire range of heat release rate. Such parameters are the bi-directional probe flow constant, $C_{bdp,i}$, and the exhaust duct diameter, D (and the heat release rate of the fuel, $(\Delta_c H)_{Mass_O_2}^{HC}$, for fuels of unknown composition). The relative uncertainty contribution from these two parameters combined is a little more than ± 0.050 and essentially sets the lower limit of uncertainty of the system. In the most practical case, the fuel will be of unknown composition and the uncertainty of $(\Delta_c H)_{Mass_O_2}^{HC}$ will increase from ± 0.002 to ± 0.027 , therefore increasing the lower limit of uncertainty to ± 0.058 . The probe constant, $C_{bdp,i}$, and the duct diameter are employed in the mass flow rate measurement. Improvement in the uncertainty of both of these variables or an independent measurement of the mass flow rate measurement with a standard relative uncertainty less than ± 0.050 is recommended. It is important to realize that the oxygen depletion for large fires is actually quite small due to the need to capture the plume in the

exhaust duct and dilute it so that complete combustion will occur. The 3MWHRRF is designed for large fires. The lowest dilution rates are not optimum for small fires and therefore the uncertainty will be greater for the smaller fires, as evidenced by the increasingly large sensitivity coefficient for the oxygen sensor voltage, V_{O_2} .

It is recommended to apply the most comprehensive baseline correction, Method II, to data used for uncertainty analysis. This method of baseline correction reduces the co-dependency of variables that violate the rules of the uncertainty propagation as previously discussed. The baseline correction and associated uncertainty is a fourth innovation of this uncertainty analysis.²⁵

Table 7 50 kW fire uncertainty comparison for the two methods of corrected HRR

Baseline HRR, MW	u_t / \dot{q}_{cricd}	
	Method I correction	Method II correction
0.010	0.103	0.070
0.052	0.135	0.075

For large fires, 500 kW and above, the combined relative standard uncertainty computed for the Method I correction agrees with that of the Method II correction to within 0.005 (therefore these results are omitted for clarity). The fact that the two methods give similar results means that the simpler Method I correction can be applied to routine test runs and the uncertainty computed. The uncertainty results are compared in Table 7 for very small fires and demonstrate a lesser degree of agreement. The two examples considered suggest that as the magnitude of the baseline drift increases the discrepancy between the uncertainty results increases. The combined uncertainty is larger for the Method I correction due to the co-variance between the correction and the measurement. This co-variance has a negligible effect for larger fires.

4.4 Repeatability, Expanded Uncertainty, and Confirmation Comparison

Repeatability

The last component of the uncertainty analysis is the repeatability of the measurement system. The Large Fire Research Facility employs a natural gas burner to produce a known value of heat release rate. The burner operation and uncertainty are presented in Sec. 3.3 and Sec. 4.3.1, respectively. One cannot have a validated calorimeter without a high quality burner. The two facilities go hand in hand.

²⁵ When applying either the Method I or the Method II correction, the data should be centered about the mean time as discussed in Sec. 4.1 and 4.3.1.

Table 8 Burner and calorimetry repeatability

Burner HRR, MW	Calorimetry HRR, MW	Exhaust flow rate, m ³ /min
0.045	0.039	622.7
0.047	0.049	641.3
0.048	0.040	615.3
0.043	0.045	829.2
0.050	0.053	844.3
0.050	0.052	805.2
0.047 ± 0.003 (Avg ± σ)	0.046 ± 0.006	
0.619	0.623	673.9
0.620	0.603	701.5
0.621	0.620	689.6
0.622	0.627	880.3
0.625	0.605	895.2
0.618	0.617	862.0
0.621 ± 0.003 (Avg ± σ)	0.616 ± 0.010	
2.610	2.706	870.9
2.642	2.645	894.5
2.624	2.656	874.1
2.620	2.673	1038.3
2.657	2.649	1056.9
2.641	2.675	1035.9
2.633 ± 0.017 (Avg ± σ)	2.667 ± 0.023	

Tests were conducted to quantify the repeatability of the measurement facility. The burner was run at three set points for heat release rate over two hood exhaust flow conditions, resulting in six separate conditions. Three repeat measurements were conducted at each condition over a period of two days. The conditions were ordered by first randomly choosing one of the two exhaust flow conditions to begin a series of tests for the three randomly ordered heat release rate settings and then repeating the process for the second exhaust flow condition. The two-step randomization was necessary in order to remain at an exhaust flow setting for a series of tests due to the difficulty of reproducing the exhaust flow conditions. However, the acquired data did not indicate that the exhaust flow rate has a measurable effect on the results; therefore the two sets of three repeats were combined.

The standard deviation of the repeat measurements was used to compute the repeatability relative standard uncertainty, u_r . The results of the repeat measurements together with their estimated uncertainties are given in Table 8. The results in the table were arrived at with the following analysis: 1) each heat release rate measurement in time was corrected for the baseline drift by algebraic subtraction, 2) the average heat release rate was

computed from 300 measurements conducted at steady conditions, 3) the mean and standard deviation about the mean were computed for the HRR for the 6 measurements.

Expanded Relative Uncertainty

The combined uncertainty, u_c , is computed by adding in quadrature the total uncertainty from the uncertainty propagation with the repeatability uncertainty:

$$u_c = \sqrt{u_t^2 + u_r^2} \quad (41)$$

Finally, the relative expanded uncertainty, U_e , is computed as $2u_c$. The results for the calibration burner and the heat release rate calorimeter are presented in Table 9. Ideally the repeatability (standard deviation) is an estimate of the total uncertainty, therefore the uncertainty as computed in Eq. (41) is a conservative estimate due to some level of double counting the uncertainty. The uncertainty computed from the equation modeling the heat release rate fails to account for sources of uncertainty not included in the model such as operator error, certain environmental conditions, or undetected equipment failures. The combined uncertainty is computed in this manner in order to address these possible sources of uncertainty.

Table 9 Expanded relative uncertainty results

Nominal HRR, MW	U_e / \dot{q}_{crctd}	
	Burner	Calorimeter
0.05	0.115	0.273
0.65	0.025	0.110
2.70	0.027	0.107

The calorimeter results of Table 9 are for a natural gas fire, which is a fire from a well characterized fuel where the uncertainty of the heat of combustion term is small. In the case that the fuel is not well characterized, the uncertainty of the heat of combustion term will increase and the increase in the expanded relative uncertainty (calorimeter output) is estimated to increase by 0.01 due to the addition in quadrature.

Comparison of Calorimeter and Burner Output

The results of the oxygen calorimetry should closely agree with the burner output. A comparison factor, C_{HRR} , is determined from the ratio of the oxygen calorimetry and burner heat release rates. It is used as a validation and quality control factor for the calorimetry. When C_{HRR} is observed to fall outside predetermined bounds, it is time to troubleshoot the systems, calorimetry and calibration burner.

$$C_{HRR} = \frac{\dot{q}_{crctd}}{\dot{q}_{burner}} \quad (42)$$

The results for C_{HRR} versus burner output are plotted in Figure 20 and were arrived at with the following analysis: 1) each heat release rate measurement in time was corrected for the baseline drift by algebraic subtraction, 2) the mean heat release rate was computed from 300 measurements conducted at steady conditions, 3) the comparison factor was computed from the mean values.

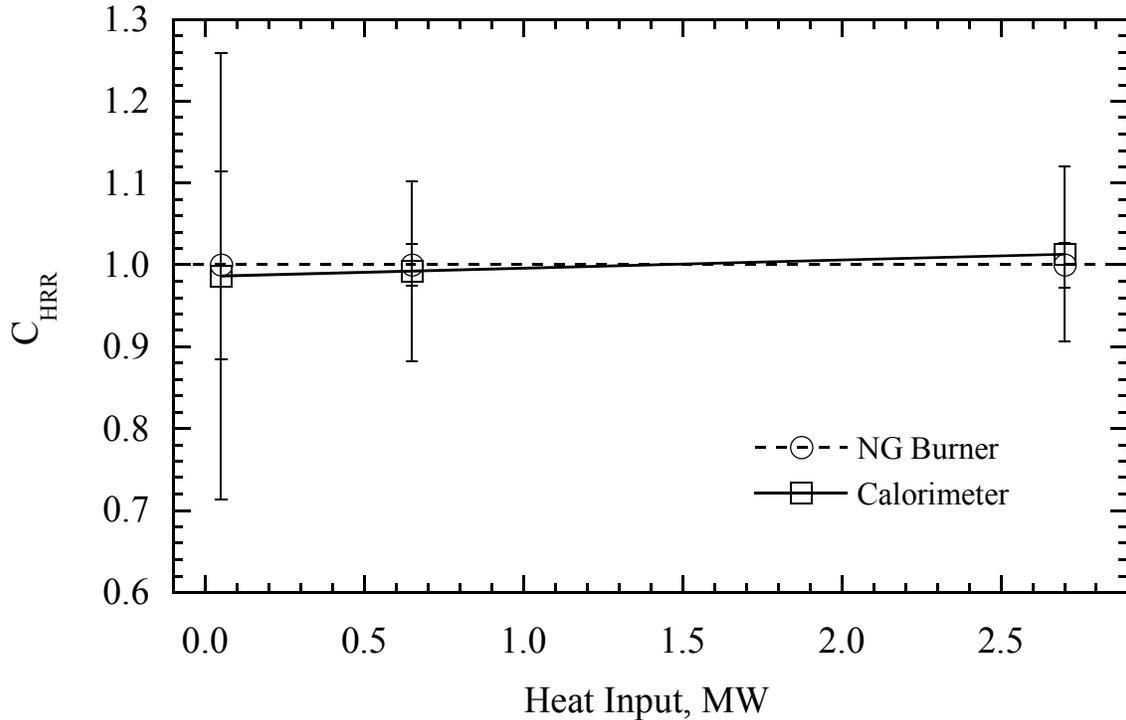


Figure 20 Burner and calorimeter comparison with respect to heat release rate.

The relative agreement between the oxygen calorimetry and the burner output is better than 0.98 for the entire range of heat release rates considered (0.05 to 2.70 MW). The bars represent the expanded relative uncertainty from Table 9. The uncertainty of the calorimetry is greater than the uncertainty of the burner heat release rate measurement and greater than the discrepancy between the calorimetry and the burner measurements.

5 Internal Quality Control Procedures

5.1 Certified Operator

The custodial operator of the system should be adequately trained on all components of the system through thorough review of instrument manuals and consultation with the manufacturer's technical representatives. The operator should be capable of training additional operators. The custodial operator is responsible for all Quality Control Procedures and scheduled maintenance. The operator should maintain a log book of all scheduled and unscheduled maintenance and facility modifications and upgrades.

5.2 Calibration of Instruments

The oxygen, carbon dioxide, and carbon monoxide meters must be calibrated with a zero gas and span gas prior to running a fire test. Because the results of the calibration are inputs to the data acquisition program the calibrations are performed using the data acquisition program.

Oxygen Meter:

The oxygen meter should be zeroed with nitrogen gas of 99.998 % purity (zero gas). (If zero gas is unavailable, 99.95 % purity will suffice.) The meter should be spanned with a gas mixture similar to ambient air. The oxygen content of the mixture must be 20.95 % and the balance must be nitrogen. Certification tickets should accompany the gas bottles and each minor component concentration should be certified accurate to ± 1 % (from expanded uncertainty) of the concentration. The meter must be zeroed and spanned prior to each fire test where HRR is measured. The oxygen meter must be constantly powered up in order to establish a thermal equilibrium in the paramagnetic cell. If constant power to the meter is not an option, then it must be powered up at least 24 hours prior to use.

Carbon Dioxide Meter:

The carbon dioxide meter should be zeroed with nitrogen gas of 99.998 % purity (zero gas). (If zero gas is unavailable, 99.95 % purity will suffice.) The meter should be spanned with a gas mixture of carbon dioxide, carbon monoxide, and nitrogen. The concentrations should be 2 % carbon dioxide, 0.1 % carbon monoxide with nitrogen making up the remainder. Certification tickets should accompany the gas bottles and each minor component concentration should be certified accurate to ± 1 % (from expanded uncertainty) of the concentration. The meter must be zeroed and spanned prior to each fire test where HRR is measured. The carbon dioxide meter must be constantly powered up in order to establish a thermal equilibrium in the instrument. If constant power to the meter is not an option, then it must be powered up at least 24 h prior to use.

Carbon Monoxide Meter:

The meter is identical to the carbon dioxide meter and the same requirements as listed above apply.

Relative Humidity Meter:

The humidity meter should be set for 1 day readings of relative humidity (see THDX manual) and the temperature output should be in units of Celsius. The instrument should be calibrated every 12 months. It is recommended to return it to the factory for calibration for the greatest accuracy. The instrument may be calibrated in house with salt capsules and a controlled environment. (see THDX manual)

Natural Gas Calorimeter:

The natural gas calorimeter should be run continuously during facility operating hours (five day week). Upon startup at the beginning of the each week, the instrument should be calibrated. Either a single point or double point calibration may be performed (see COSA CW95 manual). Calibration gases should be traceable to NIST primary standards for either gas composition or specific calorific value. Such gases are Ultra High Purity

Methane (99.99 %), Specific BTU Methane (1010 BTU), and a certified mixture of methane (91 %) and ethane (9 %). Certification tickets should accompany the gas bottles and each component concentration should be certified accurate to ± 1 % (from expanded uncertainty) of the concentration. At least once per month, a random weekly gas chromatograph report should be acquired from the local natural gas supplier to compare the two independent measurements of calorific values.

Natural Gas Flowmeter:

The natural gas flowmeter, Instromet IRMA 15M-125, should be calibrated at the NIST Fluid Flow Facility every five years or more frequently if deemed necessary.

Bi-Directional Probes and Pressure Transducers:

The bi-directional probes should be blown out with high-pressure air at the end of each day of testing. The high-pressure air should be applied for a minimum of 15 seconds. This procedure is very important when sooty fuels are burned. The pressure transducers should be calibrated annually. The calibration can be conducted in-house using a Dwyer Model 1430 point gage manometer. This device allows accurate imposition of the very low pressures.

5.3 Calibration Records

A record of all calibration certificates/reports for each instrument and calibration standards associated with the heat release rate measurement should be compiled in a single notebook and kept in the control room. An archived copy of this notebook should be kept by the facility supervisor.

The following list is an example of such records:

- Carbon Dioxide and Carbon Monoxide span gas mixture certificate of analysis
- Oxygen span gas certificate of analysis
- Nitrogen zero gas certificate of analysis
- Natural gas calorimeter calibration gases certificate of analysis
- Natural gas calorimeter calibration curves
- Natural gas flowmeter calibration report
- Heat release rate comparison curves for the natural gas burner and calorimeter measured outputs
- Pressure transducer calibrations
- Oxygen analyzer calibration report
- Carbon Dioxide analyzer calibration report
- Carbon Monoxide analyzer calibration report

5.4 Traps and Filters

A new dry ice trap should be installed prior to each fire test. The traps must be cleaned and allowed to dry for at least 24 hours before use.

The desiccant trap must be emptied and re-filled with dry desiccant (Drierite) if one quarter of the column appears to have changed color due to water. A desiccant trap may last for several fire tests.

The particle filters upstream of the control room sampling pumps should be checked daily or prior to each fire test. If they are a grayish color, not bright white, then they should be replaced.

The particle filter for the roof sampling pump should be checked monthly. It is important to keep a clean filter at this position so as to not increase the load on the sampling pump.

5.5 Data Acquisition

There should be a single version of the data acquisition program with a default configuration for basic heat release rate calorimetry. The input signals required for computing heat release rate should have permanent input channels that are not modified in any way. A list of these channels along with the description of the input and the channel settings should be readily visible to the data acquisition operator. In the event that modifications or replacement of instruments occur, the associated modifications to the data acquisition program must be documented in the log book.

5.6 Data Archiving

The data acquisition computer hard disk should be backed-up daily by NIST Central Computing. Fire test data should be archived on permanent media such as CD or DVD and properly filed for convenient retrieval. A copy of the archived data should reside outside of the Large Fire Research Facility.

5.7 Confirmation of HRR Facility

Confirmation of the complete facility using the natural gas calibration burner should be performed at the start and finish of a test series. For test series lasting multiple weeks intermediate confirmations should be performed at the start of each week.

An extensive confirmation check may include numerous gas flow rates but more typically a three point check is performed. The gas flow rates (heat release rates) chosen should encompass the expected peak values²⁶ for the test series of interest as well as lower levels (perhaps much lower levels, if a wide variety of HRR peak values is anticipated).

²⁶ The hood is nominally capable of measuring 3 MW fires using its highest flow rates. It has been used for brief 5 MW fires with good results. However, the upper limit depends strongly on plume entrainment rates, which can vary with the geometry of the fire and the plume's height of origin below the hood. With the calibration burner, there is little smoke to indicate any filling of the hood and/or skirt-enclosed volume, so it is very difficult to know when the plume is partially spilling out. The best clue of plume spillage comes when the data are analyzed, if the highest HRR point measured falls appreciably below the straight line formed by all of the lower HRR points.

Recommended procedures for performing the confirmation exercise are listed in Appendix B.5.

The data should be reduced by first plotting HRR vs time and noting time intervals that satisfy the requirement of near constancy of the HRR calculated from the measured gas flow of the calibration burner. Extract the data for each such interval (preferably at least three minutes long but two minutes may be satisfactory) and compute the average and standard deviation of each such data interval. For the same time intervals, compute the average and standard deviation for the HRR (corrected for baseline drift) calculated from the hood system measured parameters (oxygen level, hood flow, etc.). Plot the two results versus each other as “Actual HRR” for the natural gas calibration burner output on the x-axis and “Apparent HRR” for the oxygen consumption calorimetry calculated result on the y-axis. Perform a linear least squares fit of the data using a graphing package or spreadsheet statistics. Compare the results to previous such data for the system. The slopes typically agree within 1 % to 2 %.

6 Concluding Remarks

The 3 Megawatt Heat Release Rate Facility (3MWHRRF) developed at NIST is capable of accurately measuring heat release rates in the range of 0.10 to 3.0 MW including brief peaks as high as 5 MW. The expanded uncertainty (95 % confidence interval) is 11 % of the heat release rate for fire sizes larger than 400 kW. The 3MWHRRF is able to accurately measure peak heat release rates for peaks with full-width-half-maximum (as measured by the calorimeter) equal to 15 s or greater. The design features that permit this response are described in this report. It is expected that this response should enable the facility to satisfactorily measure the peak heat release rate for most fuel assemblies.

The heat release rate can be displayed in near real-time. Innovative programming was required to combine at least 30 signal outputs and to include corrections for sampling/instrumental delay and response times so that near real-time output could be obtained. The general design of the software is provided.

A natural gas calibration burner with an accurate heat output and the capability of generating short, repeatable pulses is essential for validating the 3MWHRRF. An accurate flow metering valve enabled the burner output to have an expanded uncertainty equal to 2.7 % of the heat release rate. By use of a fast response flow controller, it is possible to generate square-wave pulse widths varying from 5 s to 60 s. The repeatability of the corrected pulse heights for the burner was typically within 3 % for the entire range of the peak heat release rates and pulse-widths studied. The design of the burner including the special flow control and flow metering capabilities are presented.

The previously used uncertainty analyses for heat release rate do not appropriately account for the correlation effects in computing the oxygen difference relative to the background value and the effect of the drift in the gas analyzer outputs. A more appropriate approach to the uncertainty analysis has been utilized to include these effects

by basing the analysis on the voltage outputs of the instruments and the use of a straightforward numerical method for uncertainty propagation computed with an electronic spreadsheet. The results of the analysis identify the major source of uncertainty as the bi-directional probes used to compute the exhaust duct volume flow rate. The accuracy of the exhaust duct volume flow measurement could be improved by calibrating the probes in a controlled flow or by implementing a tracer gas volume flow measurement.

It is possible to fabricate a facility for making accurate heat release rate measurements by using mainly commercially available instruments. The 3MWHRRF utilizes commercially available equipment for the calorimeter, data acquisition/analysis system, and calibration burner. A general overview of the system hardware, operations and procedures was presented. Detailed information on specialized hardware, model numbers of the commercial products, and operational procedures is presented in greater detail in the accompanying Appendix. It is thought that this information will be useful for testing organizations to modify their facility or to design a new heat release rate facility for large fires.

7 Recommendations for Future Improvements

The following text should serve as a roadmap for institutionalizing the 3MWHRRF. This entire document is the first step in this roadmap, but much work remains. This facility has the potential to be the first NIST Fire Research Division facility capable of meeting ISO laboratory accreditation guidelines (ISO 17025) and the first NIST Fire Research Division facility to undergo internal and self-prescribed rigors to assure credible results.

7.1 Gas Sampling

- Establish routine, scheduled maintenance by manufacturer's technical representative (if necessary) of the system (particularly the gas analysis instruments, pumps, gas calibration system and the pollution control system).
- Create appropriate log books to document any problems (resolved and unresolved) and actions taken to correct them.
- Have an operational, fully compatible replacement set of gas analyzers, gas sampling pumps, and natural gas control valve on hand.
- Use NIST SRMs for carbon monoxide, carbon dioxide, and oxygen to check against the various span gases that are employed.
- Re-plumb the control room panel to shorten the flow paths and decrease system lag time. Perform systematic experiments to isolate the slow elements of the system which are prolonging the zeroing of the oxygen meter.
- Replace the gas sampling pump and pump housing on the roof with larger units. (The replacement pump on the roof was intended only as an emergency measure).
- Cover the pumps in the control room with a fan-vented enclosure to decrease noise and facilitate more effective communication among people in the room.

7.2 *Exhaust Flow Rate*

- Install a second set of pressure transducers in the box on the roof (parallel to the first set) to permit utilization of the full 21 m³/s (45,000 CFM) capacity of the hood.
- Install the helium leak detector (Varian Instruments 959-50 Porta-Test Leak Detector) as an independent device for checking the mass flow rate in the six meter hood duct. This measurement would require introduction of a precisely measured flow of helium into the calorimeter hood which would mix with the flow by the time it is sampled on the roof. From the input helium volume flow and the measured volume fraction in the mix with the hood flow, one can, from species conservation, infer the hood helium flow. Approximating the water concentration in the hood flow, and using the measured O₂, CO and CO₂ fractions in this flow, one can estimate the molecular weight and thus the mass flow in the duct. The result is a check on the flow rate inferred from the bi-directional probes that in no way depends on their output. (Note: This system could be more difficult to use in conjunction with natural gas fires, as in the calibration process described below, since natural gas may contain significant amounts of helium. This issue has yet to be resolved.)

7.3 *Data Acquisition*

- Improve the process of taking average values for the zeroing, spanning, and background operations.
 - Allow the operator to set the duration of the zero/span/background averaging times and have the operator initiate the action, but not have to hold down a button for the period.
 - Give the operator a choice of keeping or rejecting the zero/span/background data as each separate average is taken. This allows for rerecording whenever spikes or bad values are included in an average. This is helpful since currently, all recorded averages would need to be rerecorded if any are considered unacceptable. The zero/span/background buttons could also be designed to disappear after the user has accepted each average. This would prevent inadvertent reuse of the buttons and corruption of the averages.
- Create an additional channel for a user-defined time to be recorded. This time sequence could be initialized at the start of a background period or at the time of ignition.
- Design the user-selectable graphs to include the name of the channel as well as the appropriate axis labels, units, and ranges.
- Create a default parameter input file. Some input parameters cannot be modified at the front panel and modification within the code leads to an unstable program. A single program must be set up as an application that cannot be edited or saved as multiple versions for multiple experiment configurations. Users/Experimenters can create their own parameter input files that can be loaded into the application.

- Implement some mechanism such as an instrument parameter file or front panel instrument pull-down list which cross references instruments by serial number. There are parameters which are instrument specific, such as range factors, and need to be changed any time an instrument is exchanged for a similar instrument.
- Create an output parameter file that includes all of the necessary parameters for post processing the data, such as voltages, volume fractions, and range factors recorded at ambient O₂, CO₂, and CO measurements, ambient pressure, relative humidity, exhaust hood volume flow rate setting, oxygen consumption heat release parameter, delay times, etc. This reduces the need to perform a screen capture for the front panel and includes parameters that the screen capture doesn't contain. Basically the file should contain all constant parameters necessary to compute heat release rate from the output of the *.raw and *.adj files.
- Implement two separate DAQ systems, one for calorimetry signals and one for auxiliary signals. The DAQ system configuration for the calorimetry should not be modified from test to test. Such a practice degrades the capability for quality control and traceability of the calorimetry results. Therefore there should exist a separate DAQ system solely for calorimetry.
- Acquire and install a backup DAQ system for the calorimetry which simply logs the voltages in the case of system failure. If appropriate the system could provide a level of redundancy for non-repeatable fire test. This backup DAQ system should have the same analog-to-digital resolution (16 bit) as the main DAQ, and a comparable sampling rate. The minimum acceptable sampling rate should be 1 sample/per second for each channel.

7.4 Data Analysis and Uncertainty

- Create an application program to accompany the data that, with the proper inputs, can post process the data to correct for the baseline offset and compute the uncertainty of each measurement point.
- Perform an analysis that correlates the noise in the heat release rate measurement to that from each instrument.
- Assess how well the current delay time settings agree with individual instrument delay times. This assessment should be made using existing fire test data, newly designed fire test data, and cold flow data.

7.5 Calibration Burner

7.5.1 Combustion Efficiency, Flame Blow-Off, and Flame Height

- Determine the combustion efficiency at different gas flow rates and tube configurations so that optimum operating configurations can be defined and used. Based on visual observation it appears that the burner is most efficient at high gas flow rates with the minimum number of tubes open. Such a configuration yields flames whose base is predominantly blue. Unfortunately operating the burner in such a way also increases the risk of flame blow-off. With knowledge of these results, calorimetry measurements could be adjusted accordingly. In order to

accurately determine combustion efficiency, the yield of soot, CO and unburned hydrocarbons should be measured.

- Conduct experiments to determine the flow of natural gas needed for blow-off to occur. These experiments should be performed with extreme care. The burner should be operated with only bank 1 open (two tubes). The gas flow should be increased until blow-off is observed. Bank 1 only contains two primary tubes thereby minimizing the amount of unburned gas that would escape into the atmosphere. The gas flow rate could then be divided by two and we would know how much gas per tube would result in a blow-off. This information would characterize burner blow-off behavior and may be useful if the burner is operated as suggested above to determine combustion efficiency.
- Conduct experiments to develop an empirical relation for observed flame height with respect to heat release rate or natural gas flow. The experiments should be designed to address issues concerning the transition from buoyant to momentum domination, and flame merging.

7.5.2 Pulse Counting

- Implement an improved pulse counting scheme (for example through Fourier type analysis) or accurate measurement of time between pulses to significantly reduce measurement uncertainty. The Instromet rotary flow displacement meter provides output pulses that are read by the data acquisition system. The current detection scheme counts pulses for a given time duration. The ratio of these parameters yields the average volumetric flow. When the burner is used to provide a short burst of low magnitude heat release rate (i.e. low natural gas flow over a short period), the pulse count is low and the uncertainty of the burner output increases.
- Install a smaller magnitude flow meter to run in parallel to the current flow meter to increase the range of control and accuracy of the natural gas burner for low heat release rates.

7.5.3 Calibration

- Calibrate the Instromet rotary flow displacement meter across its full range of flow. The flow meter was calibrated for flows equivalent to 1.5 MW, due to operational problems associated with the NIST flow calibration facility. A copy of the calibration report is attached as Appendix E.2. Although the meter was nearly linear with pulse count, some small deviations were observed.

7.6 Control Room

- Modify the control room to be at constant temperature and positive pressure in order to provide a stable environment for the instruments and gas sampling lines and to protect the instruments from dust and moisture from the high bay area.
- Install a video display monitor and intercom system for better communication between the data acquisition officer, safety officer and researchers.

- Install a display panel which gives the status parameter (temperature) of calorimeter components located on the roof, such as the sampling pump, heated sampling line, pressure transducer housing, etc.

7.7 *Transient Fire Issues*

7.7.1 Plume Leakage

- Develop an automatic method to detect plume leakage around the hood skirt. Presently it is detected by visual observation of the plume smoke. The natural gas calibration burner does not produce significant amounts of smoke and therefore visual observation would be unreliable. Perhaps an array of thermocouples could be used to detect large scale motion of hot gas by cross correlation of their signals.

7.7.2 Plume Flow vs. Heat Release Rate

- Investigate the possible implementation of an automated exhaust flow control system. In general, the uncertainty of the heat release rate measurements is reduced as the difference between the oxygen concentration measured in the exhaust stream and the ambient value increases. While there are a number of practical problems associated with this approach, it is possible to optimize the oxygen difference by “tuning” the mass flow rate of the exhaust hood. If the exhaust is too low, then combustion products are “lost” from the hood. If the exhaust is too high, the oxygen concentration is closer to its ambient value. This would involve “matching” the hood mass flow rate with the heat release rate of the fire. In some cases, this can be anticipated and pre-programmed, while in other cases it may be useful to develop an automated flow control program. [10] Determining the maximum heat release rate for a given hood mass flow rate for which the fire plume is not affected by the hood is a possible way to set bounding limits on the exhaust flow rates. The steady state heat release rate of free burning pool fires is fairly well known, but can vary considerably depending on ambient conditions, boundary conditions, and other factors. For fires in an enclosure, the transient heat release rate is more difficult to predict. An automated exhaust flow control system would be required.

7.7.3 Capturing Transients

- Install some fast response radiometers and use their output to monitor the width of an unknown heat release rate peak. This would be an additional confirmation for fire events that are happening too rapidly for the calorimeter to resolve. Their output could also be used to monitor the relative variation of heat release rate and, combined with the calorimeter for total heat release rate, used to obtain the peak heat release rate for rapidly changing fires.

7.8 *Contribution of Smoke to Heat Release Rate*

- Review and compare approaches to estimate the effect of soot production on $(\Delta H_c)_{Mass_O_2}^{HC}$. There are two views on the significance of smoke particulate to the heat release rate. Boohez et al. [34] modified the oxygen consumption heat release equation to include soot. Calculations are carried out for a worst case, beechwood, and a best case, methane. They conclude that ignoring soot can cause a significant error. As part of the current project, preliminary work was performed to derive an equation for the fractional change in the heat of combustion /g O₂ consumed based on thermochemistry, and obtain an expression that depends on $(\Delta H_c)_{Mass_O_2}^{HC}$, the heat of formation of CO₂, the moles of soot produced per mole of fuel consumed, and the total number of moles of oxygen consumed per mole of fuel consumed. It is also assumed that all of the hydrogen reacts to form water. For toluene with a soot yield of 0.194 g soot per gram of toluene burned, it is found that the fractional change in $(\Delta H_c)_{Mass_O_2}^{HC}$ is only 1.4 %. This result suggests that smoke does not have a large effect on the heat release rate. Both of these approaches should be reviewed and compared. Estimates should be made for the effect of soot production on $(\Delta H_c)_{Mass_O_2}^{HC}$ for a range of conditions that might occur either in using the cone calorimeter or the calorimeters in the Large Fire Research Facility. Preliminary results suggest that the effect is small, but that it is larger than the effect of CO on $(\Delta H_c)_{Mass_O_2}^{HC}$.

7.9 *Education and Training*

- Establish a formal process to adequately train additional calorimeter operators other than the custodial operator of the system. These operators should be certified and periodically retrained.
- Develop an abbreviated and more general version of this document in order to effectively transfer the knowledge to technical staff at outside laboratories. For example, the document could be the centerpiece of a training workshop.

7.10 *Community Outreach*

- Conduct a workshop to gather feedback on the NIST effort and to elicit ideas and recommendations for establishing a proficiency program as recommended in NISTIR 6774. [35]

Reference List

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Appendix A Nomenclature

a	combustion products expansion factor
β	ratio of moles of combustion products to moles of oxygen consumed
ϕ	oxygen depletion factor
ρ	density, kg/m ³
b	pressure transducer calibration coefficient, torr/V
C	constant or comparison factor
D	duct diameter, m
ΔH_c	heat of combustion, kJ/kg or kJ/m ³
j	intercept of linear least squares fit
k	uncertainty coverage factor
m	slope of linear least squares fit
\dot{m}	mass loss rate or mass flow rate, kg/s
M	species molecular weight, kg/kmole
P	absolute pressure, Pa
ΔP	differential pressure, Pa
\dot{q}	heat release rate, MW
R	universal gas constant, 8.314 kg m ² /s ² K mol
RF	voltage range factor
RH	relative humidity, %
s	sensitivity coefficient
t	time, s
T	temperature, K
u	uncertainty
U	expanded uncertainty or velocity, m/s
V	instrument output voltage, V
\dot{V}	volume flow rate, m ³ /s
X	species volume fraction

Subscripts

bdp	bi-directional probe
c	combined
D	duct
e	exhaust or expanded
inc	incoming
NG	natural gas
r	repeatability
t	total

Superscripts

HC	hydrocarbon
o	ambient conditions

Appendix B Detailed Operating Procedures and Checklists

B.1 Safety

General Safety Checks

- A safety protocol for all significant fire tests is signed by Division Chief and is on file
- The area around the burner or fire zone is cleared
- The Flue Gas Cleaning System is energized and its flow checked against the planned heat release rate (to prevent hood overflow)
- The proper sized extinguishing system is ready and if necessary a trained firefighter (fully equipped) is on hand
- All personnel have respirators on hand, if necessary
- To prevent natural gas leaks to the natural gas burner the gaskets are replaced in the flexible hose every time they are reassembled
- The reassembled flexible hoses to the natural gas burner are checked for leaks prior to burner ignition
- The natural gas burner ignitor functionality is checked prior to ignition.
- A verbal warning is issued to all personnel prior to ignition of any fire
- The ignitors are energized prior to the natural gas system being energized by the DAQ operator
- All fires are constantly monitored visually
- Changes in fire size are communicated to all test personnel
- After natural gas burn completion, natural gas is purged from the flexible hose and the burner
- After fire burns to completion, or extinguishment is performed, sufficient time is allowed for fire gases to be exhausted through the hood and for the test area to reach a safe temperature
- For enclosure fire test, safe entry without protective equipment is determined by the Safety Officer from readings of carbon monoxide and temperature in the enclosure

- _____ Monitor the pressure valve after room pumps AND the Capsuhelic during test. Adjust if necessary (Use needle valve located above E to adjust Capsuhelic)
- _____ Collect data until baseline conditions return
- _____ Run N₂ zero gas and CO/CO₂ and O₂ span gases through analyzers until stable readings for each are recorded
- _____ Shut down DAQ, parse and correct data, email data
- _____ SHUT DOWN – room pumps, open valves E, B and C, dump trap, bi-directional probes off and zeroed, roof pump and fan off

B.2.2 3MWHRRF Detailed Operational Procedures

B.2.2.1 General System Preparation

Step #	Task	Comment
1	Confirm that duct system is tightly sealed from six meter hood to sampling point on roof	All bypasses closed; access hatches on roof tightly sealed
2	Confirm that pressure transducer lines have been blown clean and dry after last test.	The transducers should be shut out of the system and the zeroing valves opened before the blow back is started. With substitute pump in place on roof, gas sampling lines can only be blown out manually, from the roof. <u>There is a possibility of damage to the pressure transducers from excessive pressure if the blow back facility is used incorrectly.</u>
3	Check thermocouple readouts next to switch panel to confirm that all gas analyzers and pressure transducers are warmed-up and at steady operating temperature. Check that both sections of the heated transfer line for the gas sample are on and at a temperature setting of 90 °C (controller in roof enclosure) and 75 °C (controller on top of control room).	Bring all gas analyzers to steady operating temperature starting 24 hours in advance of testing. Start HVAC unit in pressure transducer enclosure on day before testing and send power to pressure transducers to get them to their operating temperature. See switch panel. Pressure transducer enclosure temperatures should be stable, between 24 °C (75 °F) and 29 °C (85 °F), before testing can begin (and transducers themselves should have had at least six hours to reach their steady operating temperature, otherwise they may experience zero drift).
<u>Note: Perform a drift test on warmed-up oxygen analyzer if it has shown excessive drift in previous tests. Drift test is best run by feeding the analyzer bottled air and recording output with DAQ for about 30 minutes. Determine whether apparent HRR drift behavior is acceptable for planned tests.</u>		
4	Turn all pumps off and zero the Dwyer Capsuhelic gage on the control panel.	Therefore no flow in sampling system

5	Check pump body thermocouple readout (next to switch panel) to confirm that roof pump is warmed-up. (If pump motor temp exceeds 54 °C (130 °F), the enclosure must be opened – and then closed at the end of the day)	Start gas sampling pump on roof about one hour before test to allow pump heads to heat sufficiently to prevent water condensation. (See switch panel.) All flow during this warm-up period should go out through the bypass of the flowmeter. Valve A closed, valves E, B and C open.
6	Set flow rate to 42.5 SLM (1.5 SCFM). Open access to flowmeter (two orange valves on horizontal sections) and close bypass (the other orange valve on the vertical section). Valve A closed, valves E, B and C open. Adjust the flow with the backpressure valve on the pump outlet (metering valve above Valve E).	This flow rate sets the sample line delay time. Flow rate should be a full 42.5 SLM (1.5 SCFM). If 42.5 SLM cannot be attained even with fully opened backpressure valve, the filter on roof needs replacing or the pump on roof is failing. When gas flow is properly set, switch the bypass flowmeter out of line. <u>Open the flowmeter bypass valve first then close the valves leading to the flowmeter.</u>

B.2.2.2 Immediate Test Preparation

Step #	Task	Comment
7	Install clean/dry water trap and fill dewar of cold trap with dry ice. Install clean filters and fresh Drierite, as needed.	<p>Be careful when installing glass water trap. Do not over-tighten fittings on glass tubes as the glass is easily broken. Tug on the O-ring fittings to be sure the O-rings are in their proper position. (If the tube slides out when tugged, the O-rings are not in proper position.)</p> <p>Check the Drierite in tube. The trap should never be more than half used up during the course of a test. Make sure that trap O-rings are clean, lightly greased and solidly in their grooves before re-assembling the trap. Packing of Drierite must be sufficient to prevent movement of particles when gas flows through trap but not so tight as to raise the pressure drop of the trap.</p> <p>Check all four particle filter holders in control room and install clean filters as needed. Make sure that filter holder gaskets are clean before re-assembling.</p>
8	<u>Set Valve B:</u> -Turn on roof sampling pump. -Open valves B, C and E.	The roof sampling pump is already set at flowrate, everything is at steady operating temperatures, and

	<ul style="list-style-type: none"> -Valve D closed. -Open valve A. -Turn on the control room pump(s). -Adjust the two pressure gages on the outlet lines from the pump(s) so they are centered within the ranges indicated on the gage faces. -Adjust (partially close) valve B on the gas control panel to get an internal pressure in this section of 500 Pa (2 inches of water as read on Capsuhelic pressure gage). 	<p>the flowmeter is shut out of line.</p> <p>The internal pressure setting assures that flow is always going <u>out</u> the bypass line.</p>
9	Check flow rates to all three gas analyzers.	Required flow rates are listed on the front of each analyzer.
10	<ul style="list-style-type: none"> -Check system for leaks by spraying carbon dioxide gas around joints and watching for any response on the CO₂ meter (allow time for gas to reach meter). -Check pressure drop across dry ice trap and across soot filters. 	<p>Check around any joint that has been opened since last test, especially around cold trap, Drierite trap and soot filters.</p> <p>Readings should be less than or equal to the set point markers. <u>NOTE: the response time of these gages is more than one minute.</u></p>
11	<ul style="list-style-type: none"> <u>Set up the data acquisition system.</u> -Start LabVIEW and open the current program. -Select hood flow rate. -Set current barometric pressure and relative humidity. -Set the correct E value. -Start the data collection program and enter the desired filename. -Data collection will begin. 	See separate operating instructions for detailed information about this system. It is used to record the zero and span data obtained below, as well as the test data.
<p><u>Note: Hood flow rate depends on anticipated peak fire size. The maximum flow rate 21.2 m³/s (45,000 CFM) is not acceptable if it over ranges the pressure transducers on the bi-directional probes. A high flow also lessens the resolution of the heat release rate. A lower flow rate increases heat release rate resolution of small fires but the high height of the hood makes smoke spillover from the hood more likely. The experimenter has to determine the best compromise. Consult Sec. 2.4.4.</u></p>		
<p>ZEROES AND SPANS</p>		
<p><u>Note: Perform zero and span calibrations on all gas analyzers, load cell and pressure transducers. Perform the zero first. This requires feeding an excess of the known gas to the system upstream of the soot filters. The internal pressure in the hood selection section is to be the same (500 Pa or 2 inches of water) for this section as it is when a sample is being drawn from the duct on the roof. The two pressure gages on the outlet lines from the control room pump(s) are also to be within the ranges indicated on the gage faces.)</u></p>		
12	-Zero the pressure transducers using the solenoid valve control switches to shut out the probes	Leave switches in this position while zeroing the other instruments.

	(Probes Off). -Short the probe leads (Zeroing Valves On).	
13	<u>Zero/Span the gas analyzers and load cell:</u>	
13a	Load Cell Span: Make sure testing sample is set on load cell and ready.	Warn test operator not to disturb test object during zero/span.
13b	-Turn off both gas pumps. -Close valve E. -Check the zero on the Capsuhelic pressure gage and reset to zero if needed. -Close Valve C. -Open Valve D for zero and span gas. -Turn control room pump(s) on. -Slightly open valve on Dwyer zero/span gas bypass flowmeter (or leave at previous acceptable opening)	
13c	-Slowly & carefully initiate flow of zero(Nitrogen)/span(CO/CO₂, dry air) gas until Capsuhelic gage reads 500 Pa (2 inches of water) and the flow out through the Dwyer zero/span gas bypass flowmeter is 3.3 to 3.8 SLM (7 to 8 SCFH). -Check that outlet pressures of control room pump(s) are in correct ranges. Adjust the two pressure gages if necessary, and then recheck the Capsuhelic reading. -Readjust the flow of zero/span gas, if necessary, until Capsuhelic gage reads 500 Pa (2 inches of water).	Correct Capsuhelic reading is more important than exact Dwyer flowmeter reading. These may require adjusting at random times; therefore they must be watched.
13d	Close Valve A.	This blocks out the dead volume to the left of the valve.
13e	Zero/Span the analyzers themselves by entering the zero/span set point for the CO and CO₂ meters.	See manufacturers instructions for zeroing analyzers.
13f	Adjust the zero/span output voltage for the O₂ meter.	See manufacturer's instructions for zeroing analyzers. <u>Note: For the Servomex Model 540A, the instructions recommend zeroing on the 1 % scale. However all measurements during a fire test are conducted on the 25 % scale and the DAO voltage-to-volume fraction</u>

		<p><u>conversion is based on the 25 % scaling. Therefore, zeroing on the 25 % scale is appropriate until the DAQ conversion is modified.</u></p> <p><u>The Servomex Model 540A may require 20 to 30 min to stabilize at the zero and span voltages. Watch the voltage vs time plot from the DAQ program for 2-3 minutes of steady voltage readings.</u></p>
13g	<p>When each zero or span gas has thoroughly purged the system and the instrument outputs have been properly set, record 60 scans of the instrument readings with the DAQ.</p>	<p>See DAQ instructions for Zeroing/Spanning.</p> <p>It is important not to rush the thorough purging of the system with each gas.</p>
14	<p>Return the pressure transducers to active flow measuring status Turn probes On Turn Zeroing Valves Off</p>	
15	<p>-Turn off the zero/span gas.</p>	
16	<p>- CO/CO2 span gas - repeat steps 13c – 13e, 13g. - O2 (dry air) span gas - repeat steps 13c – 13d, 13f, 13g.</p>	<p><u>Note: The gases share common supply lines; shut the bottle regulator off completely for any gas not being fed to an analyzer.</u></p>

B.2.2.3 Final Set-up for Heat Release Rate Measurements

Step #	Task	Comment
17	<p>-Turn off all calibrating gases. -Open Valve A. -Open Valve C. -Open Valve E. -Close Valve D. -Turn on the roof pump. -Confirm that the pressure transducers are in their active flow measurement state and check the volumetric flow in the exhaust duct.</p>	<p>Switch system back to sampling duct flow. Follow the exact order listed.</p>
18	<p>When the system is again thoroughly purged by the new gas flow, record the ambient gas levels with the DAQ.</p>	<p>See DAQ instructions for recording ambient readings.</p>
19	<p>Allow the system to record at least 3 min of baseline heat release rate without heat input.</p>	<p>Post processing of the data requires subtracting the baseline heat release rate from the measurement of concern. Performing this step before and after a fire test produces enough data to generate a time dependent linear function that estimates the</p>

		baseline subtraction at any moment in the test.
20	Set up and perform either natural gas or liquid burner test or fire test.	
21	After fire is completely extinguished and all combustion products have been removed from the exhaust, record another 3 to 5 minutes of baseline heat release rate.	
22	Run zero (N₂) and span (CO/CO₂ and O₂) gases through analyzers until stable readings are achieved and record	“After”-confirmation of proper operation of analyzers by checking their outputs with known inputs. The “before”-confirmation was the zero and span steps.
23	SHUT DOWN room pumps, bi-directional probes off and zeroed, roof pump off, valve E, B and C remain open.	

B.2.2.4 Special Instructions:

- 1) Start heater and circulating fan for gas sampling pump enclosure if outside temperature is less than (lab dew point + 20°C, TENTATIVE)
- 2) Start gas sampling pump head heaters and gas sampling line heaters at least one hour before test time.
- 3) Sampling pump enclosure and valve 3 body temperature must be stable and above lab dew point (+ 20°C, TENTATIVE, with pump on) before calibration or testing can begin. Pump head temperature should be at its steady temperature before testing or calibration begins.
- 4) Check sample flow splitting between bypass dump and cold trap; bypass flow should be 42.5 SLM (1.5 SCFM) and instruments should all be at their nominal gas flow rates in order for measured time delays to apply.

Note that it is possible, if the roof pump is delivering an inadequate flow and the control room pump is on, to get a zero flow indication at the large flowmeter. This can mean that flow is actually being sucked in from the exhaust line (as well as from the roof). In such circumstances, the gas sample is being diluted with air and system sensitivity is being substantially reduced. The normal system calibration does not apply. The gas sampling lines or gas sampler holes may need cleaning or the gas sampling pump on the roof should be overhauled to restore normal flow.

Do not leave bypass flowmeter in exhaust line routinely since soot will contaminate it; use the shunt path.

B.3 Data Acquisition System

Procedural lists for general calorimetry measurements and for the DAQ role in operation of the natural gas burner follow. At the DAQ screen on the computer, entering a number and having it recognized by the program requires placing the cursor on the control, typing the number, and either hitting return or right clicking anywhere on the control panel.

B.3.1 3MWHRRF DAQ Detailed Operating Procedures

Step #	Task	Comment
1	Turn on the chassis	The power switch is at the front bottom left.
2	Turn on the computer	
3	Open MAX	Open MAX (Measurement and Automation) from the desktop. Change settings (if needed). This is needed if any hardware settings or channels have been changed. MAX is used to tell Labview what hardware configuration including gains it should use.
4	Open Labview	Open Labview from the desktop.
5	Open the appropriate LFRFDAQxxx.vi program	Open the appropriate version of the program (also called a VI) LFRFDAQxxx.vi The “front panel” will come up. Maximize the window and center the panel so the controls are on the left side and first 2 graphs are on the right side. If metered natural gas is to be used, shift the panel to the left to reveal the burner controls.
6	Change the channel scan list	This is on the upper left of the front panel. Do this if you have added or subtracted instruments or changed channel number assignments. .
7	Change the delays (only if necessary)	There are sets of delays called Zero for no delays, 5.7 m ³ /s, 9.4 m ³ /s, and 14.2 m ³ /s (12000 CFM, 20000 CFM, and 30000 CFM). Also, if delays have been recalculated for the particular test or series, the array entries will need to be changed using Delay Arrays A, B, C, and D. Find the correct index number by looking for the channel description on the channel hook-up sheet and seeing what index number corresponds to it in the Array Index column.
8	Change the span values (only if necessary)	If any span values (such as a span gas concentration) have changed, adjust them in the Span Value Array. If a load cell is employed remember to put the amount of the span weight for the load cell in the array. Again, find the correct index in the Array Index column of the channel hook-up sheet. <u>To retain these values for future testing, select Operate>Make current values default and then File>Save. Make a note on the system log about the date/time of the span bottle changes.</u>
9	Adjust calorimetry	At the beginning of a series of tests, check with the test manager about whether to change the expansion factor,

	parameters, alpha or E (if necessary)	alpha (α), or the heat of combustion per mass of O ₂ , E ($(\Delta H_c)_{Mass_O_2}^{HC}$). Anytime a fuel changes, these parameters may need adjustment.
10	Input the relative humidity	Relative humidity readings should occur only AFTER exhaust system has been turned on and the building has sufficiently equilibrated.
11	Input the ambient pressure	Record the ambient pressure adjusted for temperature. Input the adjusted value.
12	Change which user-selected channels will be displayed	The two charts displayed to the right of the controls and parameters area are user-selectable channels. Ask the test manager which two parameters to display during the test. Look up the indexes for the channels corresponding to those parameters and place them in the selection controls for the charts.
13	Change any chart histories	Chart history is the number of seconds shown on the chart before older readings scroll off the screen. Change this by right-clicking on the chart. Select “chart history” at the bottom of the menu. Change the number of points displayed.
14	Adjust the overall scan rate and number of points to be averaged	Default settings are 200 scans/s, 200 points averaged. The result of this is one data point per second.
15	Start the test	Start the test with the arrow at the top menu bar. Replace the default test name. <u>You can’t choose an existing file unless it is “log-file”.</u> Delete a bad filename in the <u>DATA folder before reusing the name.</u>
16	Zero instruments	This includes O ₂ , CO, CO ₂ , and pressure transducers.
17	Record zeroes.	First, hit an event marker. Then, immediately press and hold the Zero button for at least 60 seconds (or more if deemed necessary) and then release the button.
18	Span CO and CO₂ ➔	See Sec. B.2.2.2
19	Record CO and CO₂ spans	First, hit an event marker. Then, immediately press and hold the Span button for at least 60 seconds (or more if deemed necessary) and then release the button.
20	Span O₂ ➔	See Sec. B.2.2.2.
21	Record O₂ span	First, hit an event marker. Then, immediately press and hold the Span Oxygen button for at least 60 seconds (or more if deemed necessary) and then release the button.
22	Start sampling	Make sure all pumps and instruments are running.
23	Check that all readings are normal	Check hood flow, O ₂ , CO, CO ₂ , bi-directional probes, etc.
24	Record the ambient readings	Wait until O ₂ and CO ₂ readings are steady. When steady, first, hit an event marker. Then, immediately press and hold the Average Background button for at least 60 seconds (or more if deemed necessary) and then release the button.
25	Record pre-test baseline heat release rate	Allow the entire system to run and collect data for 3 to 5 minutes without a fire.
26	Start the ignition process *	Use an event marker for ignition. A countdown by the test manager usually occurs. If using the natural gas burner,

		follow Burner Procedures, Sec. B.3.2.
27	Update relative humidity & barometric pressure	Regularly during the course of the day, check and change the relative humidity & barometric pressure.
28	* Mark extinguishment or shut down of fire	Use a countdown and event marker. Follow Burner Procedures if using the natural gas burner, Sec. B.3.2.
29	Record post-test baseline heat release rate	After fire is completely extinguished and all combustion products have been removed from the exhaust, record another 3 to 5 minutes of baseline heat release rate.
30	Stop the test	Stop the test using the large red button on the panel. <u>NEVER</u> stop with the stop sign at the top menu bar.

- = Instructions with the Calorimeter Operating Procedure
 * = Instructions with the Natural Gas Burner Procedure

B.3.2 Natural Gas Burner DAQ Detailed Operating Procedures

Step #	Task	Comment
☞	Emergency Shut Down	The red Emergency Gas Shut-off button at top center of the Burner Controls panel closes all valves after the main Maxon valve. The physical red Emergency Gas Shut-off buttons on the walls close the main Maxon valve and burner valves. Use either/both upon a dangerous condition.
1	Set Min HRR Allowed	Adjust in control at top left of Burner Controls.
2	Set Max HRR Allowed	Adjust in control at top left of Burner Controls.
3	Set Max HRR per step or loop	Adjust in control at top left of Burner Controls. This controls how fast the burner HRR can rise.
4	Set loops for gas flow measurement	Adjust to 5 to 10 if HRR>1000 kW and 10 to 60 if HRR<1000 kW.
5	Set solenoid activation thresholds	These are located at the upper right of the Burner Controls. Default settings are 300 kW for 1 st bank, 450 kW for 2 nd , 600 kW for 3 rd , and 750 kW for the 4 th .
6	Inquire for ignition ready	Ask if panel operator of safety officer is ready for ignition.
7	Turn on gas	Hit the red Emergency Gas Shut-off button at top center of the Burner Controls panel. Gas On lights up green. (Sounds counter intuitive, but this button shuts off all valves so it must be disengaged to run the burner)
8	Set target HRR for pilot	Adjust with control at middle left of Burner Controls.
9	Turn on Pilot Solenoid	Hit the switch at top right of Burner Controls.
10	Ignite	The panel operator or test manager may want to use a countdown and an event marker to mark ignition. Tell panel operator to ignite. Panel operator opens the main valve and energizes the ignitors.
11	Input Target HRR for burner.	ONLY when pilot is proven, AND all researchers are prepared. Adjust with control at the middle left of Burner Controls.
12	Watch for red Out of Range lights.	These represent values that are not physically reasonable. They should be investigated as soon as observed and may require shutting off the burner or at least operating at pilot-only or low HRR level.
13	Controlled shut down.	The test manager may use a countdown here and want an event marker. Lower target HRR to pilot level. Turn off Pilot Solenoid switch at upper right of Burner Controls. Turn off the gas with the red Emergency Gas Shut-off button at top center of the Burner Controls.

B.4 Calibration Burner

The burner requires a minimum of two operators at all times. The operators are defined as data acquisition operator (DAQO) and safety officer (SO). The DAQO is responsible for measuring and controlling the flow of gas to the burner and all other data acquisition responsibilities. The SO is responsible for burner start-up, shutdown, and manual shut-off in emergencies. Checklists of the procedures to be followed for both the DAQO and the SO are presented below.

B.4.1 Safety Officer Checklist for START-UP

Step #	Task
1	Open manual shut-off valve on column
2	Turn “Automatic Flame Detection Operation” key <i>counterclockwise</i> to activate “Ignition and Safety Panel”
3	Push “Igniter Control” button. Have technician confirm that both spark igniters are functioning.
4	Verify that DAQO is ready and all burner solenoid valves are closed.
5	Push “Igniter Control” button and open Maxon shut-off valve by depressing “Maxon Gas Valve Control” button.
6	Instruct DAQO to open Masoneilan flow control valve and pilot solenoid valve to ignite pilots.
7	Confirm ignition of pilots.
8	Confirm that FireEye “Flame” LED is illuminated.
9	Release “Igniter Control” and “Maxon Gas Valve Control” buttons.

B.4.2 DAQ Operator Checklist for START-UP

Step #	Task
1	Wait for instruction from Safety Officer to open Masoneilan flow control valve
2	Depress the emergency Gas Shut-off button on Burner Control screen
3	Give target HRR for pilot, for example 50 kW
4	Open pilot solenoid valve as Safety Officer engages igniters
5	Wait for pilot ignition to be verified by Safety Officer
6	Observe indicators on Burner Control screen for out-of-range values and if necessary go to emergency shut-down checklist



Figure 1 Ignition of pilot tubes during start-up.

B.4.3 Safety Officer Checklist for SHUT-DOWN

Step #	Task
1	Wait for notification from DAQO that the burner is ready for shut-down. DAQO will then close the Masonilan flow control valve and all primary solenoid valves.
2	Leave pilot solenoid OPEN until flame extinguishment. FireEye will automatically close Maxon valve upon flame extinguishment. Listen for Maxon valve to close.
3	Turn off manual shut-off valve on column.
4	Open "purge" valve to purge stainless steel braided hose and burner of residual gas. Purge system until three gas changes have been made, depending upon length of hose.
5	Instruct DAQO to close pilot solenoid valve.
6	Turn "Automatic Flame Detection Operation" key clockwise to OFF position. Ignition and Safety panel is now secure.

B.4.4 DAQ Operator Checklist for SHUT-DOWN

Step #	Task
1	Inform Safety Officer that burner is ready to be shut-down
2	Close the Masonellan flow control valve and all primary (non-pilot) solenoid valves. Pilot solenoid valve remains OPEN.
3	Await instructions from Safety Officer to close pilot solenoid valve.
4	See 3MWHRRF DAQ Detailed Operating Procedures for ending test.

B.4.5 Emergency Shut-Down

In the event of an emergency the burner is to be shutdown using the following procedures. Both the Safety Officer and the DAQ Operator have the capability to initiate the Emergency Shut-Down.

B.4.5.1 Safety Officer Checklist for EMERGENCY SHUT-DOWN

Step #	Task
1	Depress closest emergency shut-off button to close Maxon shut-off valve.
2	Close manual gas shut-off valve.
3	Inform DAQO that the test has been stopped and the burner has been shut-down.
4	Instruct all personal not responsible for safety to leave the building until all systems are rendered safe.

B.4.5.2 DAQ Operator Checklist for EMERGENCY SHUT-DOWN

Step #	Task
1	Depress the closest emergency shut-off button, Gas Shut-off button on Burner Control screen or emergency shut-off button on control room wall.
2	Inform Safety Officer and technician that the burner has been shutdown. Instruct Safety Officer to depress emergency shut-off button on Igniter Panel and to close manual gas shut-off valve.

B.5 Heat Release Rate Confirmation

Step #	Task	Comment
1	Set the hood flow to the desired level. Also, the flow time delay (fire to sampling point in the duct) changes with hood flow and so the correct set of time delays must be selected in the data acquisition system.	Calibration can be done at any flow level and the results should be independent of this except insofar as it affects signal-to-noise ratio on the low end of heat release rate.
2	Move the natural gas calibration burner to the center of the hood and make sure that any other flammable materials are at least 5 m away from the burner.	
3	Proceed with the normal calorimeter operating procedures (Sec. B.2.2) through the point of obtaining a background heat release rate reading.	
4	Prepare to ignite the calibration burner.	Refer to the natural gas calibration burner operation protocol and safety procedures (Sec.s B.4.1 and B.4.2).
5	Ignite the burner and allow just the pilot flows.	This will typically give the smallest HRR value for the calibration. The burner flows tend to be variable at this low end (especially below 0.10 MW). However, data in the 0.05 to 0.10 MW range can be obtained with patience. The goal is to obtain a few minutes (3 min to 4 min) of data during which the gas flow to the burner gives an essentially constant reading. Skip this point if no fires in this range are expected in the planned test series.
6	Step the burner up to 0.20 MW. Hold this setting until 3 - 4 minutes of data are obtained in which the gas burner reading is essentially constant.	
7	Repeat Step 6 for the following order of heat release rates: 0.40 MW, 0.60 MW, 1.20 MW, and 2.60 MW.	Stepping up simulates the growth of a fire and the heating up of the entire system.
8	Perform repeat measurements by stepping the burner to each of the set points previously achieved either by orderly stepping down or by a random selection.	Stepping down simulates the decline of a fire. A random progression of set points allows heat release rate levels to be achieved under different conditions.
9	Shut the natural gas burner down by stepping first to pilot level then off.	
10	Leave the calorimeter running to record 3 – 5 minutes of background heat release rate.	This step compliments Step 3 and is essential for a background correction of the data.

Appendix C Calorimeter

C.1 Sampling System

Figure 2 is a diagram of the piping inside the roof sampling pump enclosure. It is made more complex by the need to blow out the gas sampler using a back-flow of air initiated from the laboratory floor control room. Valves 1 and 3 are normally open; valves 2 and 4 are normally closed. Thus the sampled gas normally goes in and out of the two pump heads and on to the transfer line which carries it down to the analytical instruments in the control room. When the gas sampling tee is to be blown out with 140 kPa above atmospheric pressure air, the pump is off and valves 1 and 3 are closed (activated) to prevent flow through the pump. Valve 2 is opened to cause flow to go back through the gas sampling tee in the duct and remove accumulated soot from the inlet holes. Note that the heated transfer line from the pump housing to the analytical instruments can also be blown out backwards. Air at this same pressure is introduced into the end in the control room. Valves 1 and 3 are activated to close off the pump and valve 4 is opened to allow any material in the line to go out through a vent in the side of the pump enclosure.

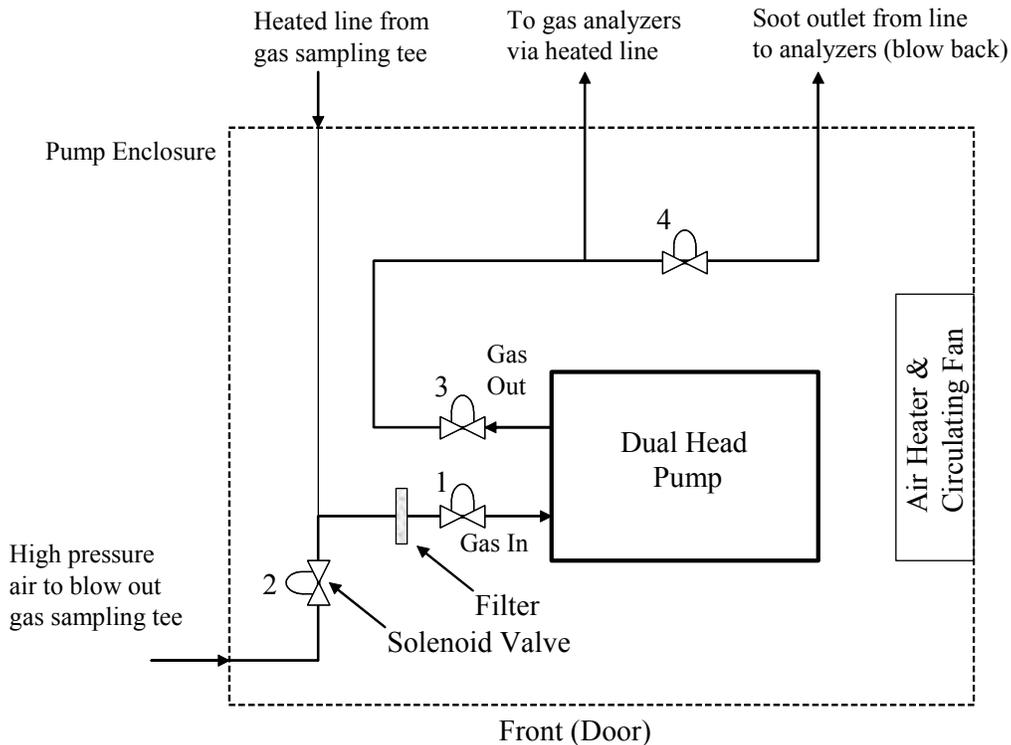


Figure 2 Diagram of plumbing inside roof sampling pump enclosure

All of the electrical switching functions are set up to be operable from the control room. Figure 3 shows a typical wiring diagram. Essentially all operations are accomplished from the control room with 24 VAC relays which are mounted in the roof enclosures.

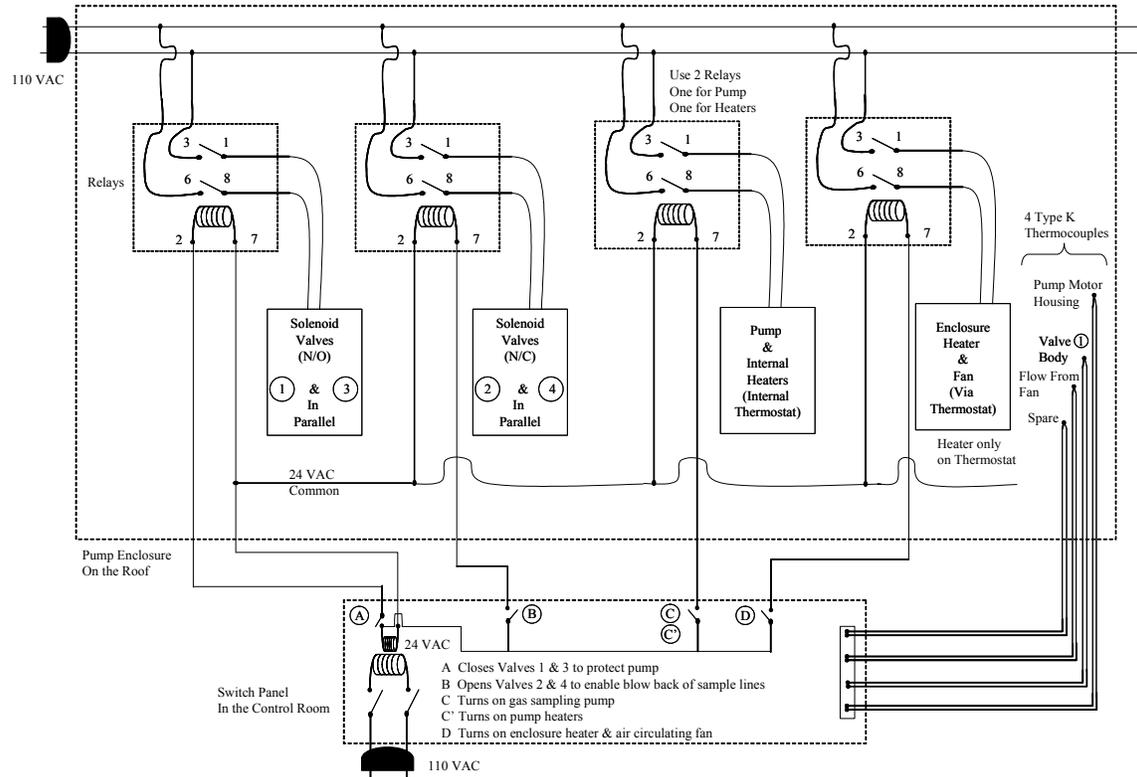


Figure 3 Electrical wiring diagram for the roof sampling pump enclosure

C.2 Bi-Directional Probes

Table 1 Positions of Bi-Directional Probes in 6 Meter Hood Duct

Designation	Lead tube orientation	Distance from duct wall, cm
E	Vertical	4.83*
D	Horizontal	20.4*
C	Horizontal	48.4*
B	Horizontal	48.4#
A	Horizontal	20.4#
F	Vertical	4.83#

* distance above the bottom of the duct

distance below the top of the duct

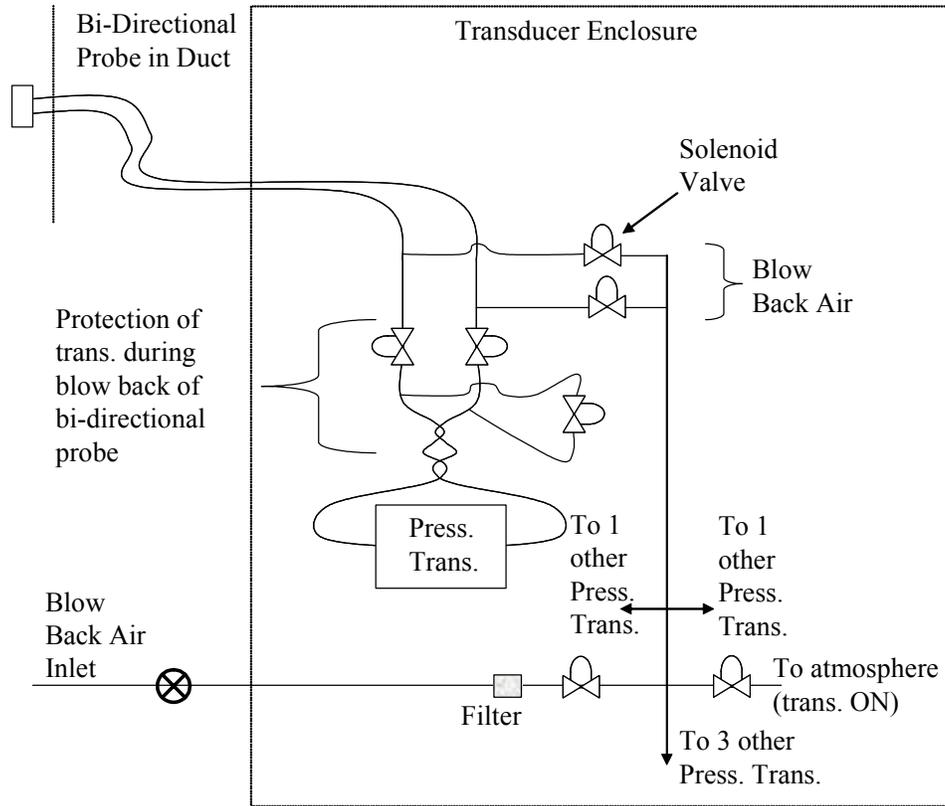


Figure 4 Pressure transducer enclosure plumbing

Table 2. Coefficients of Straight Line Fits to Pressure Transducer Output

Serial Number	a [torr]	b [torr / V]
217880 (C)	0.0050085	0.099475
217474 (D)	0.0054898	0.099214
217468 (E)	0.0030260	0.098603
217473 (B)	0.0035489	0.098800
217854 (F)	0.0042414	0.099294
217728 (A)	0.0028156	0.100070

$$\text{Pressure Reading (torr)} = a + b (\text{Voltage Reading, VDC})$$

C.3 System Components List

Component Description	Manufacturer	Model No.	No.
Oxygen analyzer – measures the dry volume fraction of O ₂ in a sample volume	Servomex	540A	1
Carbon dioxide analyzer – measures the dry volume fraction of CO ₂ in a sample volume	Siemens	ULTRAMAT 6	1
Carbon monoxide analyzer – measures the dry volume fraction of CO in a sample volume	Siemens	ULTRAMAT 6	1
Pressure transducer – measures the pressure in the O ₂ analyzer line (Controller)	MKS Instruments	628B13TBE2B (PR 4000)	1
Humidity meter – measures the relative humidity in the LFRF	Dickson	THDX	1
Pressure transducers – measures the differential pressure at the bi-directional probes located in the exhaust duct	MKS, Instruments	220CD-00010A2B	6
Thermocouples – measures the gas temperature at each of the bi-directional probes	OMEGA	Type K	6
Sampling pump –	Air Dimensions, Inc.	R272-FV-AA1-M	1
Heated hose – (Controller)	The Conrad Company, Inc.	CWH67-08-768-T-220-1920K2 (CTC-58-K-TLOGIC-240)	2
Control room pumps – pulls a portion of exhaust gas from the main sample and pushes it to the analyzers	GAST	DOA-P109-FB	2

Web addresses for online manuals:

Siemens ULTRAMAT 6:

<https://pia.khe.siemens.com/index.asp?Nr=4758>

Dickson THDX Humidity Meter:

http://www.dicksonweb.com/product_data_details.jsp?mid=1296160102_1058289965352_563525419&id=1

Appendix D Data Acquisition

D.1 Data Acquisition Channel Assignments

The following are charts representing hardware and software settings used for conducting calorimetry experiments. “Modules” are the signal conditioning modules which receive each raw voltage and “Mod.(ule) Channel No.” is the channel number for the associated module. The channel inputs are segmented into a group of arrays which correspond to the level of computation performed on the channel input. Array A represents the raw physical channels; array B represents the new channels which combine 2 or more raw channels; arrays C, D, and E proceed to further levels of combination. The “Overall Channel No.” represents the index of the output channels written to the data files with the corresponding “Column Label”. The “Gain” represents how much the instrument output voltage is amplified. The range of each instrument’s output voltage is represented as “Output Voltage Range”. Raw voltage channels are grouped by gas analysis, duct pressures, natural gas monitoring, and temperatures of the sampling process and duct. The raw voltages are output to the “raw” file and the converted values are output to the “adj” file. In the adjusted hook up sheet there are columns for a time “Delay”. These time delays represent the amount of time a signal must be delayed in its computation relative to the actual occurrence of a fire event. The delay times will vary with respect to the hood exhaust flow rate.

D.1.1 Large Fire Research Facility Data Acquisition Hook Up Sheet – Raw Voltages

Module No.	Mod. Channel No.	Array Index	Overall Channel No.	Column Label	Description	Gain	Output Voltage Range (V)	Units for Converted Values
2	0	A0	0	O2	O ₂ volume fraction	1	0 to 1	volume fraction (dry)
2	1	A1	1	PO2	O ₂ pressure	1	0 to 10	mm Hg
2	2	A2	2	CO2	CO ₂ volume fraction	1	0 to 5	volume fraction (dry)
2	3	A3	3	CO2-R	CO ₂ range factor	1	0 to 5	V
2	4	A4	4	CO	CO volume fraction	1	0 to 5	volume fraction (dry)
2	5	A5	5	CO-R	CO range factor	1	0 to 5	V
2	6	A6	6	P1	Duct differential pressure 1	1	-10 to 10	Pa
2	7	A7	7	P2	Duct differential pressure 2	1	-10 to 10	Pa
2	8	A8	8	P3	Duct differential pressure 3	1	-10 to 10	Pa

2	9	A9	9	P4	Duct differential pressure 4	1	-10 to 10	Pa
2	10	A10	10	P5	Duct differential pressure 5	1	-10 to 10	Pa
2	11	A11	11	P6	Duct differential pressure 6	1	-10 to 10	Pa
2	14	A14	14	He	Helium	1	n/a	n/a
2	15	A15	15	Load1	load cell 1 (small)	1	0 to 10	kg
2	16	A16	16	Load2	load cell 2 (med)	1	0 to 10	kg
2	17	A17	17	Load3	load cell 3 (large)	1	0 to 10	kg
2	18	A18	18	Pgas	natural gas pressure	100	0 to 0.1	psia
2	19	A19	19	Pgas SV	natural gas pressure supply voltage	1	n/a	n/a
2	20	A20	20	HComb	heat of combustion	1	n/a	n/a
2	21	A21	21	SpGr	Specific gravity	1	n/a	n/a
3	0	A22	22	Ta	T(emp) ambient	100	0 to 0.1	°C
3	1	A23	23	The	T helium	100	0 to 0.1	°C
3	2	A24	24	Tgas	T natural gas	100	0 to 0.1	°C
3	3	A25	25	TP1	T duct @ pressure 1	100	0 to 0.1	°C
3	4	A26	26	TP2	T duct @ pressure 2	100	0 to 0.1	°C
3	5	A27	27	TP3	T duct @ pressure 3	100	0 to 0.1	°C
3	6	A28	28	TP4	T duct @ pressure 4	100	0 to 0.1	°C
3	7	A29	29	TP5	T duct @ pressure 5	100	0 to 0.1	°C
3	8	A30	30	TP6	T duct @ pressure 6	100	0 to 0.1	°C
3	11	A33	33	Tencl1	T roof enclosure 1	100	0 to 0.1	°C
3	12	A34	34	Tencl2	T roof enclosure 2	100	0 to 0.1	°C
3	13	A35	35	Thtline1	T roof enclosure 1	100	0 to 0.1	°C
3	14	A36	36	Thtline2	T roof enclosure 2	100	0 to 0.1	°C
3	15	A37	37	Te1	T exhaust duct 1	100	0 to 0.1	°C
3	16	A38	38	Te2	T exhaust duct 2	100	0 to 0.1	°C
3	17	A39	39	Te3	T exhaust duct 3	100	0 to 0.1	°C

D.1.2 Large Fire Research Facility Data Acquisition Hook Up Sheet – Adjusted Values

Array Index	Overall Channel No.	Column Label	Description	Units for Calculated Values	Delay Category	5.7 m ³ /s (12000 cfm) Delay, s	9.4 m ³ /s (20000 cfm) Delay, s	14.2 m ³ /s (30000 cfm) Delay, s
A40	40	Event1	Event1	n/a	0	0	0	0
A41	41	Event2	Event2	n/a	0	0	0	0
B0	42	O2	O ₂ volume fraction	volume fraction (dry)	O ₂	32.3	28.7	25.7
B1	43	CO2	CO ₂ volume fraction	Volume fraction (dry)	CO/CO ₂	33.1	28	26.4
B2	44	CO	CO volume fraction	Volume fraction (dry)	CO/CO ₂	33.1	28	26.4
B3	45	V1	duct velocity 1	m/s	Flow	16.5	12.5	8.7
B4	46	V2	duct velocity 2	m/s	Flow	16.5	12.5	8.7
B5	47	V3	duct velocity 3	m/s	Flow	16.5	12.5	8.7
B6	48	V4	duct velocity 4	m/s	Flow	16.5	12.5	8.7
B7	49	V5	duct velocity 5	m/s	Flow	16.5	12.5	8.7
B8	50	V6	duct velocity 6	m/s	Flow	16.5	12.5	8.7
B11	53	He	He	n/a	Flow	16.5	12.5	8.7
B12	54	mloss1	mass loss 1	kg/s	Flow	16.5	12.5	8.7
B13	55	mloss2	mass loss 2	kg/s	Flow	16.5	12.5	8.7
B14	56	mloss3	mass loss 3	kg/s	Flow	16.5	12.5	8.7
B15	57	DTMHRR	HRR from diaphragm test meter	kW	0	0	0	0
B16	58	XoH2O	ambient water vapor volume fraction	volume fraction	0	0	0	0
B17	59	TPave	average duct temperature @ pressure transducers	°C	Flow	16.5	12.5	8.7
B18	60	NGFlow	calibration burner flow	m ³ /s (actual)	0	0	0	0
B19	61	NGPcorr	corrected natural gas pressure	psia	0	0	0	0
C0	62	Vave	average duct velocity	m/s	Flow	16.5	12.5	8.7
C1	63	Phi	Phi		CO/CO ₂	33.1	28	26.4
C2	64	HRRBurn	calibration burner HRR	kW	0	0	0	0
D0	65	mdote	exhaust duct mass flow rate	kg/s	Flow	16.5	12.5	8.7
D1	66	Qe	exhaust duct volume flow	ft ³ /min (actual)	Flow	16.5	12.5	8.7

E0	67	calHRR	calorimeter HRR	kW	CO/CO ₂	33.1	28	26.4
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D.2 Heat Release Rate Data Acquisition Example Data Output Filest

“raw” data file

6/11/2002	4:15 PM										
Time	O2	PO2	CO2	CO2-R	CO	CO-R	P1	P2	P3	P4	P5
0	0.81	-7.39	-0.002	1.00	-0.003	1.00	-0.030	-0.037	-0.056	-0.032	-0.043
1	0.81	-7.39	-0.002	1.00	-0.003	1.00	-0.029	-0.038	-0.056	-0.032	-0.043
P6	P7	P8	He	Load1	Load2	Load3	Pgas	PgasSV	HComb	SpGr	Ta
-0.054	-2.66	10.00	10.00	-10.00	-0.003	-2.77	0.016	-10.00	10.00	-4.12	24.06
-0.054	-2.66	10.00	10.00	-10.00	-0.003	-2.77	0.016	-10.00	10.00	-4.12	24.07
The	Tgas	TP1	TP2	TP3	TP4	TP5	TP6	TP7	TP8	Tenc11	Tenc12
25.00	26.74	32.94	33.17	33.68	34.40	34.80	33.03	24.54	24.30	24.22	3.E+03
25.01	26.74	32.95	33.17	33.67	34.41	34.80	33.02	24.55	24.29	24.22	3.E+03
Thline1	Thline2	Te1	Te2	Te3	Event1	Event2	Valve mA				
-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03	0	0	0				
-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03	0	0	0				

“adj” data file

6/11/2002	4:15 PM										
Time	O2	PO2	CO2	CO2-R	CO	CO-R	P1	P2	P3	P4	P5
0	0.203	0.99	-0.002	1.04	-0.003	0.62	-0.40	-0.48	-0.74	-0.42	-0.56
1	0.203	0.99	-0.002	1.04	-0.003	0.62	-0.39	-0.50	-0.75	-0.43	-0.57
P6	P7	P8	He	Load1	Load2	Load3	Pgas	PgasSV	HComb	SpGr	Ta
-0.71	-35.27	133.33	10.00	-60.00	-0.003	-62.86	27.81	1.00	10.00	-4.12	24.06
-0.72	-35.26	133.33	10.00	-60.00	-0.003	-62.86	27.81	1.00	10.00	-4.12	24.07
The	Tgas	TP1	TP2	TP3	TP4	TP5	TP6	TP7	TP8	Tenc11	Tenc12
25.00	26.74	32.94	33.17	33.68	34.40	34.80	33.03	24.54	24.30	24.22	3.E+03
25.01	26.74	32.95	33.17	33.67	34.41	34.80	33.02	24.55	24.29	24.22	3.E+03
Thline1	Thline2	Te1	Te2	Te3	Event1	Event2	O2	CO2	CO	V1	V2
-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03	0.00	0.00	0.21	0.00	0.00	-0.77	-0.85
-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03	0.00	0.00	0.21	0.00	0.00	-0.76	-0.86
V3	V4	V5	V6	V7	V8	He	mloss1	mloss2	mloss3	DTMHRR	XoH2O

-1.05	-0.79	-0.92	-1.03	-7.15	13.90	250.00	-60.00	0.00	-62.86	NaN	0.01
-1.06	-0.80	-0.92	-1.03	-7.15	13.90	250.14	-60.00	0.00	-62.86	NaN	0.01
TPAve	NGFlow	NGPcorr	Vave	Phi	HRRburn	mdote	Qe	calHRR			
33.67	0.18	27.81	0.90	0.029	0.01	1.87	3439.07	166.80			
33.67	0.18	27.81	0.91	0.029	0.01	1.88	3454.07	167.34			

“zs” data file

10/23/2002	3:40 PM										
Time	O2	PO2	CO2	CO2-R	CO	CO-R	P1	P2	P3	P4	P5
Zero	-0.003	-7.559	-0.005	1.005	-0.005	1.005	-0.016	-0.027	-0.058	-0.019	-0.039
Span	-0.028	-7.560	1.459	3.029	0.182	2.015	1.092	1.372	1.999	2.006	1.306
Span Val	0.2095	1	0.0909	1	0.0405	1	1	1	1	1	1
	P6	P7	P8	He	Load1	Load2	Load3	Pgas	PgasSV	HComb	SpGr
	-0.040	-9.399	10.001	10.001	0.043	10.001	-10.003	0.016	-10.002	10.004	-10.004
	0.894	-9.411	10.001	10.001	0.075	10.001	-10.003	0.016	-10.002	10.004	-10.004
	1	1	1	1	5	1	22.6796	1	1	1	1
	Ta	THe	Tgas	TP1	TP2	TP3	TP4	TP5	TP6	TP7	TP8
	21.778	22.043	25.907	19.816	19.888	19.901	20.031	20.057	20.012	-4.E+12	-4.E+12
	21.996	22.012	25.893	19.829	19.901	19.925	20.052	20.060	20.007	-4.E+12	-4.E+12
	1	1	1	1	1	1	1	1	1	1	1
	Tenc1	Tenc2	Thtline1	Thtline2	Te1	Te2	Te3	Event1	Event2	Valve mA	
	3.E+03	3.E+03	-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03				
	3.E+03	3.E+03	-4.E+12	-4.E+12	-4.E+12	3.E+03	3.E+03				
	1	1	1	1	1	1	1				

D.3 Calorimetry Algorithm Description

The data acquisition program consists of three main sections: initialization, main data loop, and process termination. The algorithm flow chart was presented in Sec. 2.2.3, Figure 8. The first section deals with setting up which channels on which hardware devices are to be scanned, initializing arrays, naming and opening of files, setting headings of the file columns, initializing the burner gas pulse counting process, providing data rate and averaging parameters, and determining the delay history required for the particular hood flow regime.

The second section is the main data loop that is active for all but the first and last few seconds of a particular program run. The normal settings are for the main loop to run once every second and take 200 scans per loop which generates an average reading per channel per loop (or per second). These settings can be changed for particular

applications. All data conversion and calculations on a new set of scanned data occur within the same loop. The first frame, or step, of the main loop scans every channel and also averages periods of data if the user activates the zero, span, or background controls. Raw voltage values as well as new converted values are stored. The second frame takes the data and copies it into a history array that holds on to fast data (from fast responding or short delay sensors) until slower data (from slower responding or delayed response sensors) can “catch up”. By storing a period of history of the data, channel outputs that represent the same event, but are generated by sensors with different response and delay times, can be combined as if the sensors responded simultaneously. Additional frames conduct second and third order calculations on previously converted data, sometimes using data from the history array. A frame responsible for burner control also is placed in the midst of these frames. Finally after all calculations, including the calorimeter heat release rate, are complete, the program writes the data to various files and displays standard output plots (heat release rate, duct velocity) as well as plots of data from user-selected channels. The loop starts again at the first step unless directed to stop.

If by the decision point at the end of the main loop a “stop” input from the computer panel has occurred during the loop, then the third section of the program begins. The third section terminates processes, writes the file containing zeroes and spans, and closes files.

D.4 Calibration Burner HRR Algorithm

The components of the data acquisition program that control and monitor the natural gas burner are primarily contained within the main data loop. A flow chart of the natural gas burner control and monitoring algorithm is presented in Sec. D.4.1. The only burner-related function that occurs prior to the main loop is the initiation of continuous counting of pulses. The digital counter is configured and armed in the initialization stage of the program even though pulses may not occur and be counted for some time or at all. Within the main loop, burner-related inputs, calculations, output display and recording, and control functions are nested or combined with the other calorimetry-related steps.

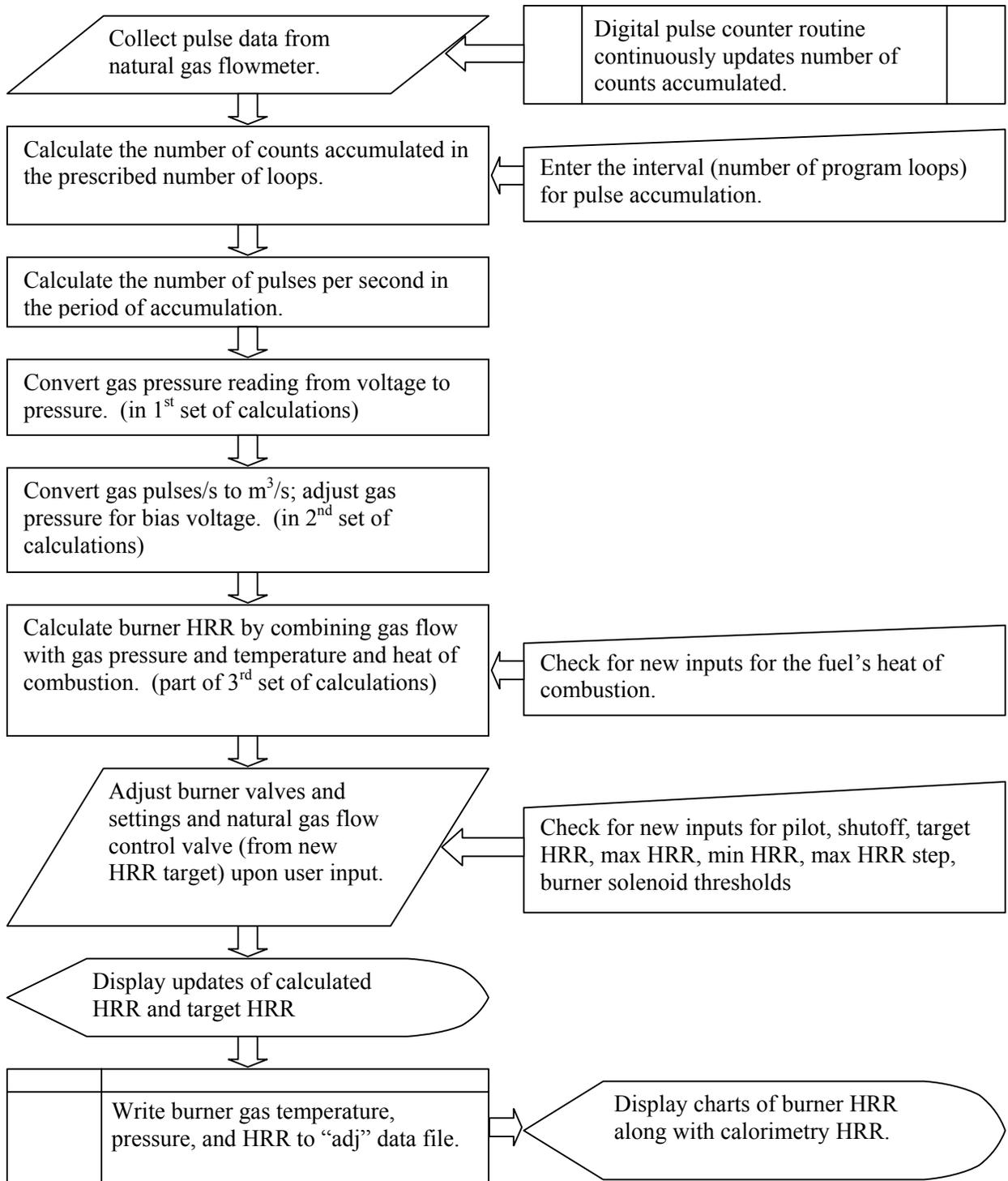
The program produces current and voltage that control various burner valves. Five volt signals are sent to relays to activate the pilot valve and 4 solenoid valves that open banks of burner tubes. The DAQ operator has on/off control to these valves and can set thresholds of heat release rate to prescribe at what level each of the 4 tube banks should open. An emergency shutoff button on the control panel is used as a safety interlock and is required to be engaged for any of the valves to be opened.

A 4 mA to 20 mA current is sent to the natural gas flow control valve to modulate it to the flow corresponding to a target heat release rate. The equation relating heat release rate to control valve current was generated through an initial calibration exercise. Before igniting the burner, the user enters the minimum and maximum heat release rate and maximum heat release rate step. These parameters prevent accidental dangerous behavior due to faulty or unreasonable inputs. During use, these safety limits can still be changed, but generally the target heat release rate is the main burner control used during

operation. User inputs are also available to adjust the heat of combustion of the gas and the specific gravity. Automatic input from online analysis is planned to replace these manual inputs. Other safety related aspects of the burner include forcing out-of-range user inputs into acceptable ranges, forcing out-of-range operation into acceptable ranges, warning alarm lights for out-of-range parameters, and a warning to exhibit extra care for fires over 3 MW. Displayed operating parameters include valve status, calculated heat release rate (plot and value), gas temperature, gas pressure, average pulses per second, and gas flow.

The user selects the number of loops over which the pulses are accumulated, averaged, and used to record/display the burner heat release rate. Normally, pulses are accumulated over brief periods of time such as (1 to 5) s during transition, but the number of loops used is increased for achieving averages over periods of steady heat release rate. Generally, the pulse frequency is used to calculate how many seconds (or loops) are necessary to achieve some prescribed number of pulses (typically 200) to achieve an acceptable level of uncertainty due to the digital jitter caused by the gaining and losing of pulse edges at adjacent accumulation periods.

D.4.1 Natural Gas Burner Control and Monitoring Algorithm



D.5 System Components List

Component Description	Manufacturer	Model No.	No.
16 channel data acquisition board for PCI bus computer interface having: 16 bit resolution, 333 kSamples/second sampling rate, 8 digital I/O channels, two 24-bit counter/timers	National Instruments	PCI 6052E	1
2 meter shielded cable with extra shielding for 68 pin devices to connect to terminal block of data acquisition board	National Instruments	SH6868-EP	1
Feed-through panel for PCI 6052E to SCXI 1001	National Instruments	SCXI 1180	1
Cable assembly for PCI 6052E, SCXI 1001, and BNC 2090	National Instruments	100-2X50POS	1
Adapter	National Instruments	68F-50M	1
Shielded rack mountable terminal block adapter for 68 pin devices with 22 BNC connectors and 28 spring terminals for analog outputs and digital I/O	National Instruments	BNC 2090	1
Chassis box to hold, protect, and power up to 12 SCXI modules	National Instruments	SCXI 1001	1
2 m cable assembly for SCXI 1001	National Instruments	SCXI 1349	1
Rack mounting kit for SCXI 1001	National Instruments	SCXI 1370	1
Signal conditioner and multiplexer for 32 differential channels consisting of thermocouples, millivolt, or 10 V signals having: 333 kHz scanning rate, 200 Hz lowpass filter, and 100X gain amplifiers for each channel	National Instruments	SCXI 1102B	6
Shielded, rack-mountable thermocouple terminal block with 32 subminiature thermocouple connectors and cold junction compensation circuitry	National Instruments	TC 2095	8
96 pin 1 meter shielded cable to connect TC 2095 and BNC 2095 to SCXI 1001	National Instruments	SH 96-96	7
Signal conditioner and multiplexer for 32 differential channels consisting of signals up to 42 V having: 333 kHz scanning rate, 10 kHz lowpass filter, and amplifiers for each channel	National Instruments	SCXI 1104C	1
Terminal block for SCXI 1104C with 32 BNC connectors	National Instruments	BNC 2095	3
Analog source board for PCI computer bus interface having: 16 bit resolution, 16 zero to +-10 V voltage channels, 16 zero to 20 mA current channels, and 8 digital I/O channels	National Instruments	NI 6704	1
68 pin 2 meter shielded cable to connect NI 6704 to SCB-68 terminal block	National Instruments	SH68-68-D1	1

Shielded terminal block with 68 pin connection for NI 6704 with onboard temperature sensor for cold junction compensation	National Instruments	SCB-68	1
Full development system for Windows 95/98/NT/2000 for running data acquisition system	National Instruments	Labview license	1

Web Addresses for online manuals:

PCI6052 DAQ Board:

<http://www.ni.com/pdf/manuals/370477c.pdf>

SCXI1001 Chassis:

<http://www.ni.com/pdf/manuals/320423f.pdf>

SCXI1349 Shielded Cable Adaptor:

<http://www.ni.com/pdf/manuals/320791c.pdf>

SCXI1102 Amplifier Module:

<http://www.ni.com/pdf/manuals/320975b.pdf>

BNC/TC2095 Terminal Block:

<http://www.ni.com/pdf/manuals/321731a.pdf>

PCI6704 Analog Output Module:

<http://www.ni.com/pdf/manuals/322110b.pdf>

SCB68 Connector Block:

<http://www.ni.com/pdf/manuals/320745b.pdf>

Labview v.7:

<http://www.ni.com/pdf/manuals/320999e.pdf>

Appendix E Natural Gas Burner

E.1 System Components List

Component Description	Manufacturer	Model No.	No.
Safety shut-off valve – closes natural gas flow in the event of an emergency and power failure either automatically or manually using DAQ	Maxon Corp.	3” Series 5000	1
Control valve with digital positioner - controls the amount of natural gas to the burner, max flow is 165 liter/s	Masoneilan	Camflex (valve) SVI (positioner)	1
Volumetric gas flow rotary meter with high frequency output, flow range: 0.79 liter/s to 118 liters/s	Instromet	IRMA 15M-125	1
Pressure transducer – measures the pressure in the body of the gas flowmeter, pressure range 0 kPa to 350 kPa above ambient	OmegaDyne Inc.	PX01C1-050AV	1
Thermocouple – measures the temperature of the gas in the body of the flowmeter	Omega	Type K	1
Modular automatic ignition and continuous flame monitoring system – safety mechanism to allow natural gas flow only when flame is present	Fireye	M-Series II (module) UV1A (flame scanner) MEP100 (Programmer) MEUV4 (amplifier)	1

Web addresses for online manuals:

Masoneilan Smart Valve Interface:

<http://www.dresser.com/internet/businessunits/measurement/subunits/masoneilan/products/instruments/ew2000.pdf>

Masoneilan SVI Pushbutton Guide:

<http://www.dresser.com/internet/businessunits/measurement/subunits/masoneilan/products/instruments/svi-button-guide.pdf>

Masoneilan CamFlex Control Valve Specs:

<http://www.dresser.com/internet/businessunits/measurement/subunits/masoneilan/products/rotary/cf5000.pdf>

Masoneilan CamFlex Control Valve Instructions:

<http://www.dresser.com/internet/businessunits/measurement/subunits/masoneilan/products/rotary/ef5000e.pdf>

E.2 Volumetric Flow Meter Calibration Reports

REPORT OF CALIBRATION

FOR

A POSITIVE DISPLACEMENT FLOW METER

February 14, 2002

Manufacturer: Instromet
Serial No.: 319396
Capacity: 0.8 – 118 liters/sec

submitted by

National Institute of Standards and Technology
Building and Fire Research Laboratory
Fire Research Division (866)
Gaithersburg, Maryland

(Reference: NIST Requisition No. 864-0247)

The positive displacement flow meter was calibrated by flowing filtered dry air at a constant rate through the meter and then into a volumetric prover. The prover measures volumetric flow by collecting gas in a known volume over a measured period of time. The meter was run at seven flow set points and five (or more) flow determinations were gathered on two different days and used to produce averages at each of these flows. As a result, the tabulated data points for these runs are averages of ten or more individual calibration measurements.

Photographs showing the arrangement of piping and sensors for the test are shown in Figures 1. The flow meter was connected to an existing length of pipe 130 cm long upstream, which was provided by the customer. An additional length of 188 cm piping and a Zanker flow diffuser (see Figure 2) were added for the upstream run. A 90 cm length of pipe was installed downstream of the meter. A NIST sensor for measuring pressure was installed at the existing tap on the meter body (Paroscientific SN 73965).¹ A temperature sensor was installed upstream of the meter, next to the existing temperature sensor on the meter body (Instrulab SN 30032, thermistor #9). Two Agilent Universal Counters (SN SG40004486 and SN SG40004417) were used to acquire the frequency output by the meter under test over the same intervals that gas was collected by the prover system.

¹ The instrument make and model is stated for completeness of the calibration record and to establish the chain of calibration traceability and is not an endorsement of the product.

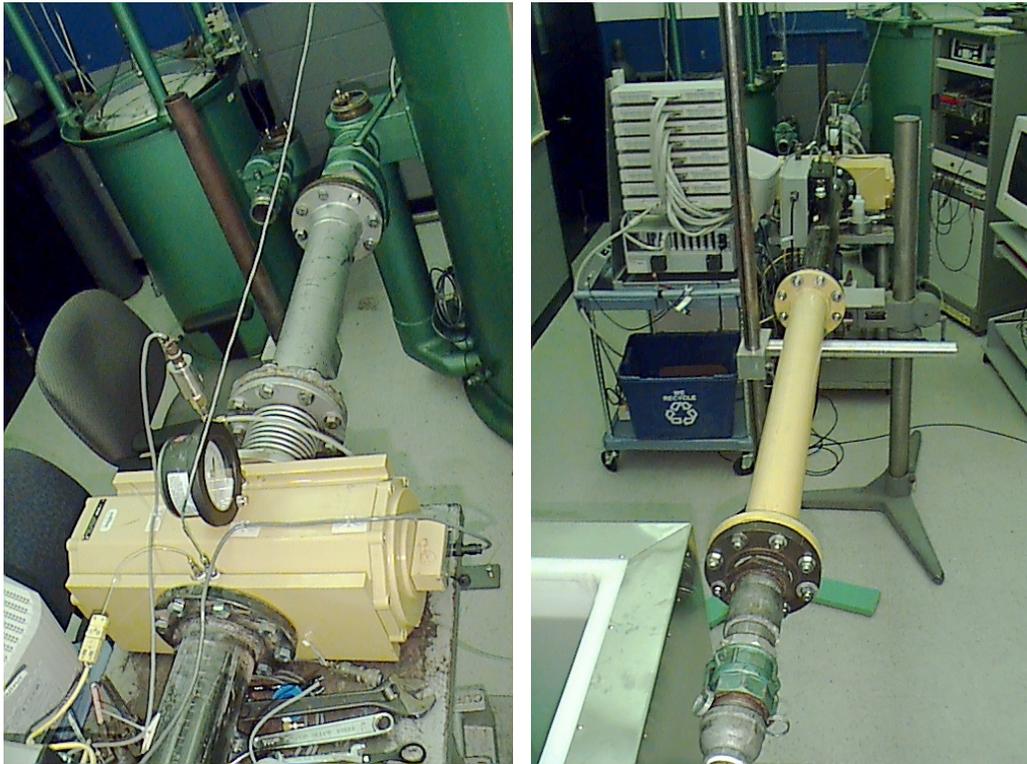


Figure 1. Meter under test and associated piping arrangement.

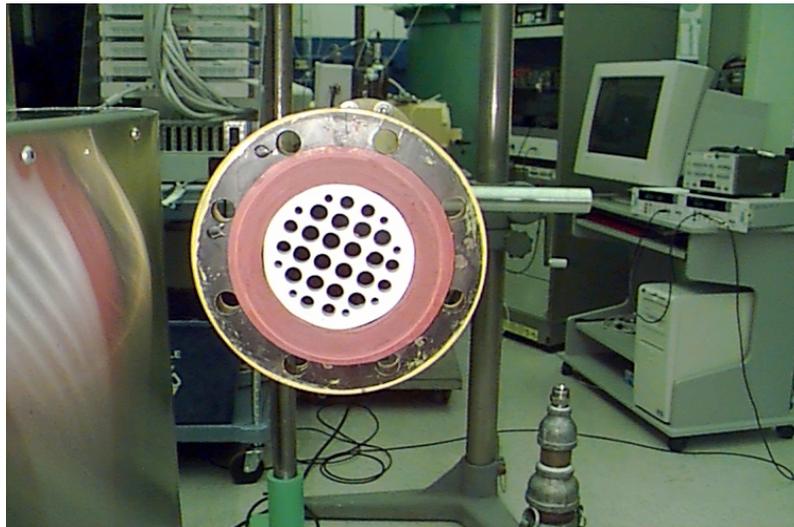


Figure 2. Zanker Flow Diffuser.

Calibration results will be presented in the form of a meter factor versus a viscosity parameter.

The meter factor was calculated from the expression:

$$K = \frac{f}{\dot{V}} \quad (1)$$

where \dot{V} is the actual volumetric flow at the meter under test and f is the frequency output by the meter. The viscosity parameter was calculated from the expression:

$$N = \frac{f \cdot \rho}{\mu} \quad (2)$$

where ρ and μ are the dry air density and viscosity, calculated with the following equations:²

$$\rho = \frac{1}{1.23838 + 287.04 \cdot \frac{T}{P} - 3012.2 \cdot T^{-1.334} - 7.3049 \cdot 10^{-4} \cdot \frac{P}{T} + 2.5304 \cdot 10^{-2} \cdot \frac{P}{T^{1.25}}} \quad (3)$$

and,

$$\mu = \left(\frac{145.8 \cdot T^{1.5}}{110.4 + T} \right) \cdot 10^{-7} \quad (4)$$

where P is in kPa, T is in K, ρ is in g/cm³, and μ has units g / (cm s). Note that if the positive displacement meter were to be utilized at temperatures significantly different from the calibration temperature, a flow calculation approach, which accounted for thermal expansion should be used to obtain optimum results.³

The calibration results are presented in the following table and figures.

² Hilsenrath, J., Beckett, C. W., Benedict, W. S., Fano, L., Hoge, H. J., Masi, J. F., Nuttall, R. L., Touloukian, Y. S., and Woolley, H. W., *Tables of Thermal Properties of Gases*, NBS Circular 564, 1955.

³ Mattingly, G. E., *The Characterization of a Piston Displacement Type Flowmeter Calibration Facility and the Calibration and Use of Pulsed Output Type Flowmeters*, J. Res. Natl. Inst. Std. Tech., 97, pp. 509, 1992.

Table 1. Calibration results for the positive displacement meter SN 319396 (nominal pressure of 200 kPa data only).

T [K]	P [kPa]	\dot{V} [cm ³ /s]	f [Hz]	N [1/cm ²]	$K \cdot 10^4$ [cm ³]	U_e [%]
296.74	206.27	578.4	0.2916	3.858	5.041	0.19
296.60	206.77	881.3	0.4453	5.914	5.052	0.19
295.85	204.95	1152	0.5827	7.704	5.058	0.23
295.70	205.84	2331	1.184	15.74	5.079	0.19
294.69	204.57	4767	2.435	32.36	5.109	0.19
294.22	205.66	11818	6.033	80.84	5.105	0.22
293.47	196.72	22094	11.236	144.6	5.086	0.22

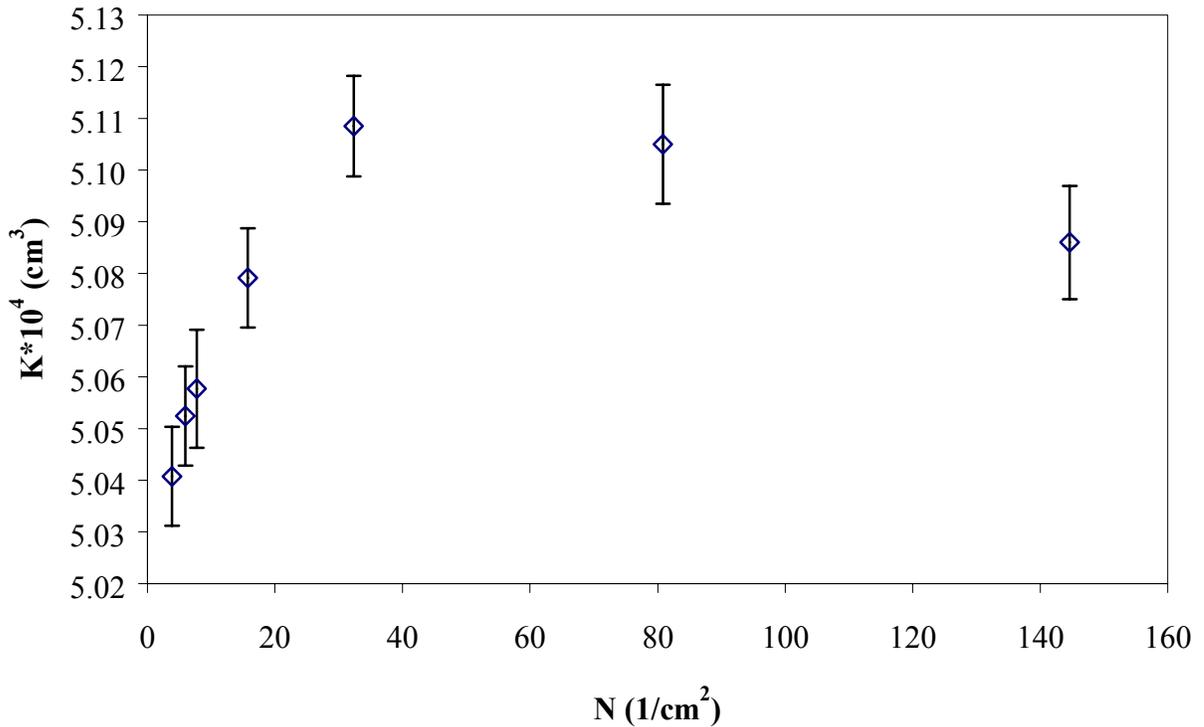


Figure 2. Calibration results for the positive displacement meter SN 319396. The diamonds represent averages of ten or more individual calibration measurements (200 kPa data only).

At a flow of $N = 15$, data were collected at three pressures of 100, 150, and 200 kPa. The results obtained are shown in Figure 3. These data demonstrates the utility of the meter factor and viscosity parameter to compensate for varying operating conditions.

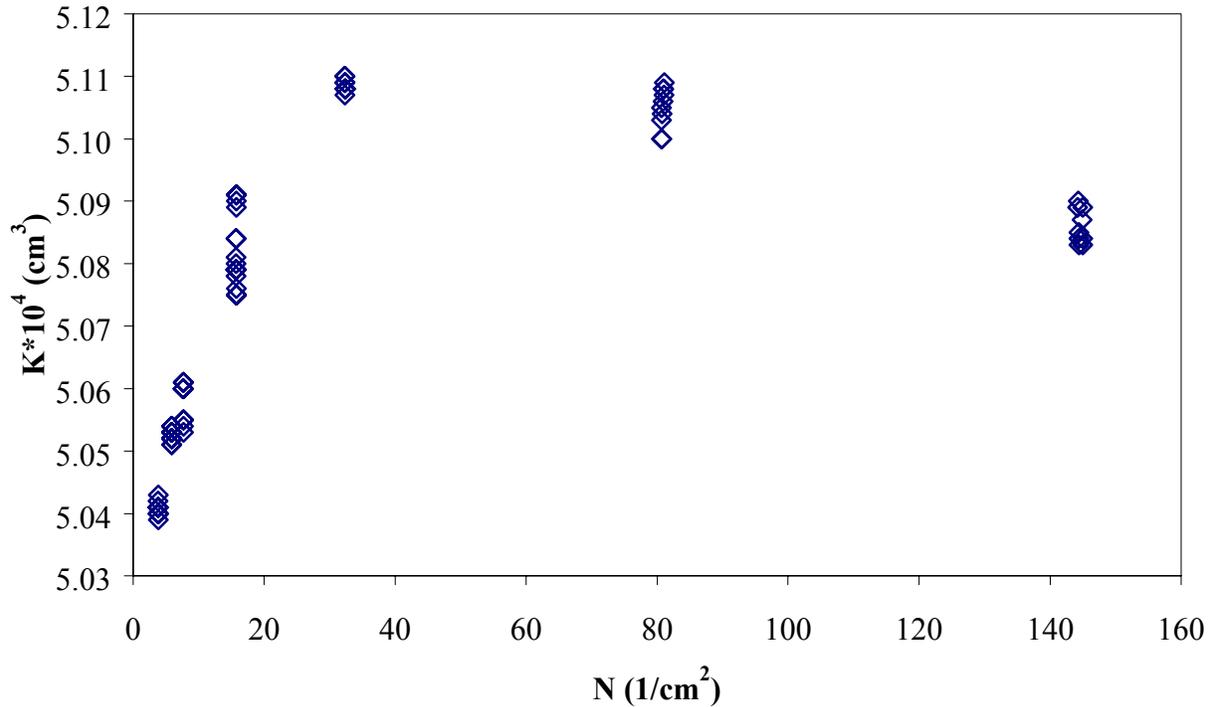


Figure 3. Calibration results for the positive displacement meter SN 319396. The diamonds represent individual calibration measurements. Also included are individual calibration measurements made at three different pressures.

An analysis was performed to assess the uncertainty of the results obtained from the meter under test.^{4, 5, 6} The process involves identifying the equations involved in calculating the calibration result (measurand) so that the sensitivity of the result to uncertainties in the input quantities can be evaluated. The 67% confidence level uncertainty of each of the input quantities is determined, weighted by its sensitivity, and combined with the other uncertainty components by root-sum-square to arrive at a combined uncertainty (U_c). The combined uncertainty is multiplied by a coverage factor of 2 to arrive at an expanded uncertainty (U_e) of the measurand with a 95% confidence level.

⁴ International Organization for Standardization, *Guide to the Expression of Uncertainty in Measurement*, Switzerland, 1996 edition.

⁵ Taylor, B. N. and Kuyatt, C. E., *Guidelines for Evaluating and Expressing the Uncertainty of NIST Measurement Results*, NIST TN 1297, 1994 edition.

⁶ Coleman, H. W. and Steele, W. G., *Experimentation and Uncertainty Analysis for Engineers*, John Wiley and Sons, 2nd ed., 1999.

As described in the references, if one considers a generic basis equation for the measurement process, which has an output, y , based on N input quantities, x_i ,

$$y = y(x_1, x_2, \dots, x_N) \quad (5)$$

and all uncertainty components are uncorrelated, the normalized expanded uncertainty is given by,

$$\frac{U_e(y)}{y} = k \frac{U_c(y)}{y} = k \sqrt{\sum_{i=1}^N s_i^2 \left(\frac{u(x_i)}{x_i} \right)^2} \quad (6)$$

In the normalized expanded uncertainty equation, the $u(x_i)$'s are the standard uncertainties of each inputs, and s_i 's are their associated sensitivity coefficients, given by,

$$s_i = \frac{\partial y}{\partial x_i} \frac{x_i}{y} \quad (7)$$

The normalized expanded uncertainty equation is convenient since it permits the usage of relative uncertainties (in fractional or percentage forms) and of dimensionless sensitivity coefficients. The dimensionless sensitivity coefficients can often be obtained by inspection since for a linear function they have a magnitude of unity.

In this case, the uncertainty of the meter factor, K , has components due to the measurement of the actual volumetric flow at the meter under test, $u(\dot{V})$, the measurement of the frequency output of the meter under test, $u(f)$, and the reproducibility of the test, $u(R)$, all of which have sensitivity coefficients of 1. The uncertainty of the actual volumetric flow has uncertainty components from the mass flow measurement by the primary standard, $u(\dot{m}) = 0.09\%$,⁷ as well as the pressure, $u(P) = 0.02\%$, and temperature, $u(T) = 0.03\%$, used to convert the mass flows to actual volumetric flows at the meter under test, all of which have sensitivity coefficients of 1. The RSS of these components gives the combined uncertainty for the actual volumetric flow of 0.09%.

To measure the reproducibility⁸ of the test, the standard deviation of the calibration results was

⁷ Wright, J. D. and Mattingly, G. E., *NIST Calibration Services for Gas Flow Meters: Piston Prover and Bell Prover Gas Flow Facilities*, NIST Special Publication 250-49, August, 1998.

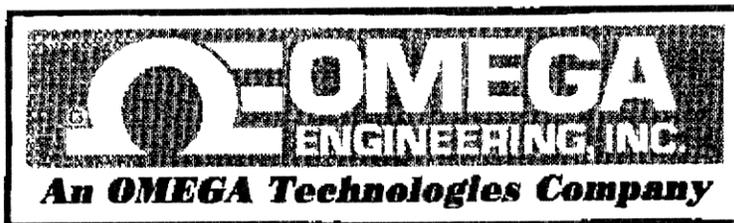
⁸ Reproducibility is herein defined as the closeness of the agreement between measurements with the flow changed and then returned to the same nominal value.

used to calculate the relative standard uncertainty (the standard deviation divided by the mean and expressed as a percentage) at each of the nominal flow set points. Using the values given above results in the expanded uncertainties for the calibration results listed in the data table and shown as error bars in the figure.

For the Director,
National Institute of Standards and Technology

Dr. Pedro I. Espina
Leader, Fluid Flow Group
Process Measurements Division
Chemical Science and Technology Laboratory

E.3 Pressure Gauge Calibration Report



Certificate of Calibration

for

NIST

100 BUREAU DRIVE

STOP 8663

GAITHERBURG MD 208998663

Cust. P.O. #: HAMINS Model #: PX01C1-050AV

OMEGA W.O. #: 208990462 S/N #: 132830

CAL-2

OMEGA Engineering, Inc. certifies that the above instrumentation has been calibrated and tested to meet or exceed the published specifications. This calibration and testing was performed using instrumentation and standards that are traceable to the United States National Institute of Standards and Technology.

Quality Assurance Inspector

11/07/02

Date

Omega Engineering, Inc., One Omega Drive, Box 4047, Stamford, CT 06907
Telephone: (203) 359-1660 · FAX: (203) 359-7811
Internet Address: <http://www.omega.com> E-Mail: info@omega.com

OMEGADYNE INC.

PRESSURE TRANSDUCER
FINAL CALIBRATION

0 - 50.00 PSIA
Excitation 10.000 Vdc

Job: Serial: 132830
Model: PX01C1-050AV Tested By: AEB
Date: 2/21/2002 Temperature Range: 60 to 160 F
Calibrated: 0.00 - 50.00 PSIA Specfile: Px01-mV.spf

Pressure PSIA	Unit Data mVdc
0.00	0.000
25.00	14.944
50.00	29.934
25.00	14.952
0.00	0.000

Balance - 0.101 mVdc
Sensitivity 29.934 mVdc
In Resist 350.80 Ohms
Out Resist 351.20 Ohms
Shunt: 14.345 mVdc

ELECTRICAL LEAKAGE: PASS
PRESSURE CONNECTION/FITTING: 1/4-18 NPT MALE
ELECTRICAL WIRING/CONNECTOR: PIN A +OUTPUT
PIN B -OUTPUT
PIN C -INPUT
PIN D +INPUT
PINS E&F SHUNT

This Calibration was performed using Instruments and Standards that are traceable to the United States National Institute of Standards Technology.

S/N	Description	Range	Reference	Cal Cert
1598/94-3	30/150 PSI DRUCK STD	0 - 150 lbs	C-2502	C-2502
3146A20557	HP 34401A	Unit Under Test	C-2405	C-2405

Q.A. Representative : *Rick Swisher* Date: 2/21/02

This transducer is tested to & meets published specifications. After final calibration our products are stored in a controlled stock room & considered in bonded storage. Depending on environment & severity of use factory calibration is recommended every one to three years after initial service installation date

Omegadyne, Inc., 149 Stelzer Court, Sunbury, OH 43074 (740) 965-9340
http://www.omegadyne.com email: info@omegadyne.com (800) USA-DYNE

Appendix F Uncertainty Comparison Example

F.1 Uncertainty in the Difference of Correlated Measurement Quantities

The uncertainty in the volume fraction measurement of a gas is assumed to have two components, one a result of the uncertainty in the calibration gas, u_{cal} , and the second arising from the electronic noise of the instrument, u_n . Two measurements of volume fraction are conducted, X_1 and X_2 , with the same instrument, after a single calibration and at separate times. The algebraic difference of the measurements, ΔX , is the quantity of interest. Figure 5 is a graphical representation of the measurement example. The volume fraction of the calibration gas is X_S and its standard uncertainty, u_{cal} , is represented by error bars. Likewise, the standard uncertainty due to the noise is shown with error bars at measurements 1 and 2. Using propagation of uncertainty (i.e. “root-sum-of-squares”), one obtains the following expression for the uncertainty for X_1 :

$$u(X_1) = (u_{cal}^2 + u_n^2)^{1/2}. \quad (B1)$$

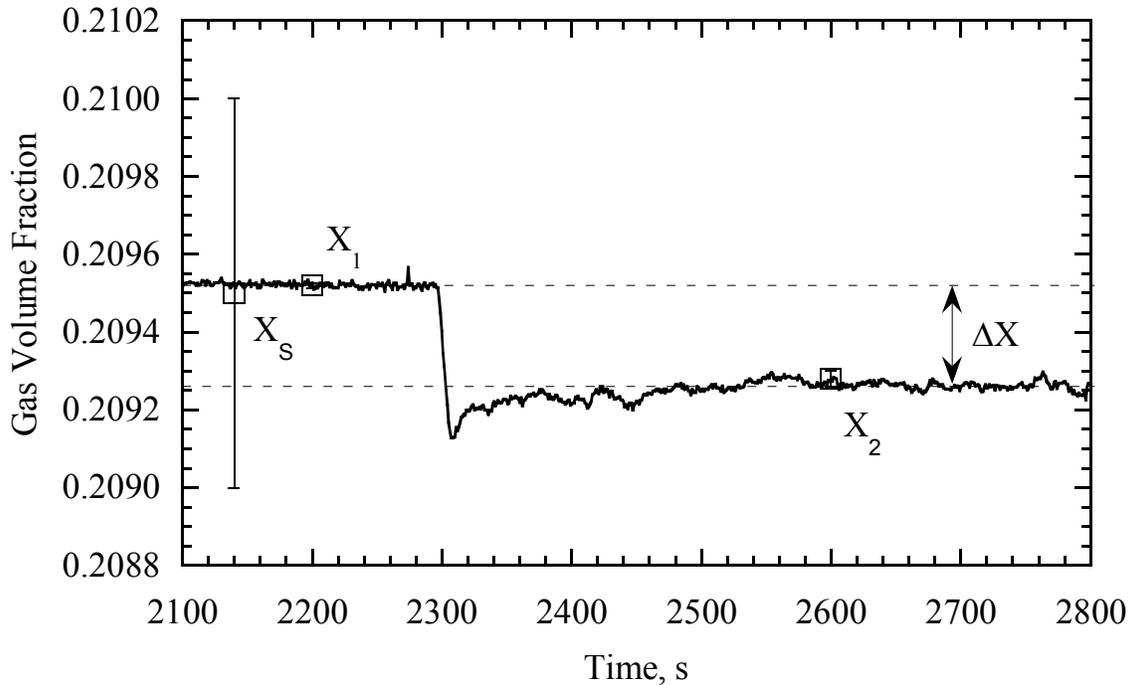


Figure 5 Example of co-dependent difference measurement.

A similar expression is obtained for the uncertainty for $u(X_2)$. Treating the two quantities as independent, one obtains an uncertainty in the difference in the oxygen volume fractions equal to $\sqrt{2}$ times the expression in Eq. (B1). For the oxygen measurement, u_{cal} is typically a factor of 20 greater than u_n . This leads $u(\Delta X)$ being approximately equal to $\sqrt{2}u_{cal}$. Using this standard approach, one obtains an overestimate of the uncertainty by

about a factor of 20. The actual uncertainty is more nearly equal to u_n than u_{cal} . The basic reason for the overestimate is that, in the case of oxygen the two gas measurements are not independent because they share the same calibration. Therefore, if the calibration gas is low by 1 % of the specified value, it will be low for both measurements.

To account for this lack of independence, the volume fraction measurements are expressed in terms of the calibration gas volume fraction, X_S , the voltage of the analyzer corresponding to the calibration gas, V_S , and the voltage corresponding to the gas volume fraction at measurement 1, V_1 , and to the voltage corresponding to the volume fraction at measurement 2, V_2 . In this case, the difference in the volume fractions is expressed as:

$$\Delta X = X_1 - X_2 = \frac{X_S}{V_S}(V_1 - V_2) \quad (B2)$$

Carrying out the uncertainty propagation based on X_S , V_S , V_1 , and V_2 , which are all independent measurements, one obtains the following expression for the uncertainty:

$$\frac{u(\Delta X)}{\Delta X} = \left(\left(\frac{u(X_S)}{X_S} \right)^2 + \left(-\frac{u(V_S)}{V_S} \right)^2 + \left(\frac{V_1}{V_1 - V_2} \frac{u(V_1)}{V_1} \right)^2 + \left(\frac{-V_2}{V_1 - V_2} \frac{u(V_2)}{V_2} \right)^2 \right)^{1/2} \quad (B3)$$

It is seen from Eq. (B3) that the uncertainty of the calibration, the first term, is only counted once. The remaining three terms account for the uncertainty of the noise. It is important to recognize that the last two terms are more heavily weighted when the difference in voltage (i.e. volume fraction) is small. To further illustrate the example, it is assumed that $X_S=0.21$, $V_S=V_1=1.0$ V, $V_2=0.995$ V, $u(X_S)=u_{cal}$, and $u(V_S)=u(V_1)=u(V_2)=u_n$, $u_{cal}=20u_n$, from which $\Delta X=0.00105$. Computing the uncertainty using Eq. (B3):

$$\frac{u(\Delta X)}{\Delta X} = \left(\left(\frac{u_{cal}}{0.21} \right)^2 + (-u_n)^2 + \left(\frac{1}{0.005} u_n \right)^2 + \left(\frac{-1}{0.005} u_n \right)^2 \right)^{1/2}$$

$$\frac{u(\Delta X)}{\Delta X} = \left((4.76u_{cal})^2 + u_n^2(2 \times 200^2 + 1^2) \right)^{1/2} \approx \left((4.76(20u_n))^2 + u_n^2(2 \times 200^2) \right)^{1/2} = 298u_n$$

Recall that in the first example $u(\Delta X)$ was equal to $\sqrt{2}u_{cal}=20\sqrt{2}u_n$. Compared to the second example where $u(\Delta X)=\Delta X 298u_n = 0.31u_n$, it is clear that the uncertainty was overestimated¹ when the co-dependency of the variables was ignored. This example shows the importance of properly accounting for co-dependent variables and is one of the new aspects of this uncertainty assessment.

¹ Although in this case failing to account for the correlation in the volume fractions lead to an overestimate of the uncertainty in their difference, in other cases an underestimate might occur.

It is apparent from the above example that a straightforward application of Eq. (22) to the heat release rate equation (Eq. (13)) such as illustrated in the first example will not account for the co-dependent effects. To account for these effects, the procedure in the second example is followed to express the variables in terms of the most basic measurement inputs of instrument voltages, thermocouple temperatures, and constant parameters (universal, empirical and calibration). In this process, both the effect of the instrument span gas and zero gas is considered whereas in the example above only the span gas was considered. The relations for each instrument or combination of instruments for converting the basic measurement inputs to scientific units are presented in the main text.

Appendix G Troubleshooting

The following problems have occurred since the system has been in operation. This list should be expanded as new problems (and their solutions) arise.

- 1) Slow response from a bi-directional probe. The reading from probe E rose much more slowly than that from the other five velocity probes when the hood fan was turned on (requiring many seconds to reach a plausible reading). A plug of water in the probe lead tubes was suspected. Normal behavior was eventually restored by disconnecting and blowing out all of the lead tubes (from probe to pressure transducer) though no water was ever confirmed.

- 2) Inability to get expected air flow rate from hood. Problem was traced to several inches of water in the blower housing after a heavy rain.

- 3) Inability to get expected gas flow through the control room sampling pumps and to the analysis instruments. Problem was traced to excessively tight packing of the Drierite in its tube. Packing must be tight enough to assure no flow paths form a bypass around the bulk of the Drierite but not as tight as possible. A few light taps of the housing on the bench before adding the last few grams is sufficient.

- 4) Lock-up of the DAQ during zero/span operations or during a fire test. Problem traced to inadequate buffer settings for the number of channels being read.

- 5) Anomalous drift in HRR signal. This could have many causes but one which has been verified is due to a drift in the output pressure of the sampling pump(s) in the control room. The test operator needs to pay close attention to the pressure gages

on the outlets of the control room sample pump(s) and adjust the flow as needed to keep the pressures in the indicated ranges.